

# Ana G Gayubo

## List of Publications by Year in descending order

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docs citations

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times ranked

4278  
citing authors

#	ARTICLE	IF	CITATIONS
1	Role of zeolite properties in bio-oil deoxygenation and hydrocarbons production by catalytic cracking. <i>Fuel Processing Technology</i> , 2022, 227, 107130.	7.2	36
2	Streamlining the estimation of kinetic parameters using periodic reaction conditions: The methanol-to-hydrocarbon reaction as a case study. <i>Chemical Engineering Journal</i> , 2022, 435, 134800.	12.7	1
3	Spectro-kinetics of the methanol to hydrocarbons reaction combining online product analysis with UV-vis and FTIR spectroscopies throughout the space time evolution. <i>Journal of Catalysis</i> , 2022, 408, 115-127.	6.2	13
4	Unveiling the deactivation by coke of NiAl <sub>2</sub> O <sub>4</sub> spinel derived catalysts in the bio-oil steam reforming: Role of individual oxygenates. <i>Fuel</i> , 2022, 321, 124009.	6.4	17
5	Stability of a NiAl <sub>2</sub> O <sub>4</sub> Derived Catalyst in the Ethanol Steam Reforming in Reaction-Regeneration Cycles: Effect of Reduction Temperature. <i>Catalysts</i> , 2022, 12, 550.	3.5	4
6	Combined effect of bio-oil composition and temperature on the stability of Ni spinel derived catalyst for hydrogen production by steam reforming. <i>Fuel</i> , 2022, 326, 124966.	6.4	16
7	Consideration of the activity distribution using the population balance theory for designing a dual fluidized bed reactor-regenerator system. Application to the MTO process. <i>Chemical Engineering Journal</i> , 2021, 405, 126448.	12.7	16
8	Feasibility of online pre-reforming step with dolomite for improving Ni spinel catalyst stability in the steam reforming of raw bio-oil. <i>Fuel Processing Technology</i> , 2021, 215, 106769.	7.2	20
9	Insights into the Reaction Routes for H <sub>2</sub> Formation in the Ethanol Steam Reforming on a Catalyst Derived from NiAl <sub>2</sub> O <sub>4</sub> Spinel. <i>Energy &amp; Fuels</i> , 2021, 35, 17197-17211.	5.1	19
10	Global vision from the thermodynamics of the effect of the bio-oil composition and the reforming strategies in the H <sub>2</sub> production and the energy requirement. <i>Energy Conversion and Management</i> , 2021, 239, 114181.	9.2	18
11	Influence of HZSM-5-based catalyst deactivation on the performance of different reactor configurations for the conversion of bioethanol into hydrocarbons. <i>Fuel</i> , 2021, 302, 121061.	6.4	2
12	Effect of reaction conditions on the deactivation by coke of a NiAl <sub>2</sub> O <sub>4</sub> spinel derived catalyst in the steam reforming of bio-oil. <i>Applied Catalysis B: Environmental</i> , 2021, 297, 120445.	20.2	44
13	A comprehensive approach for designing different configurations of isothermal reactors with fast catalyst deactivation. <i>Chemical Engineering Journal</i> , 2020, 379, 122260.	12.7	16
14	Dual catalyst-sorbent role of dolomite in the steam reforming of raw bio-oil for producing H <sub>2</sub> -rich syngas. <i>Fuel Processing Technology</i> , 2020, 200, 106316.	7.2	28
15	Coke formation and deactivation during catalytic reforming of biomass and waste pyrolysis products: A review. <i>Renewable and Sustainable Energy Reviews</i> , 2020, 119, 109600.	16.4	278
16	Deactivation of Ni spinel derived catalyst during the oxidative steam reforming of raw bio-oil. <i>Fuel</i> , 2020, 276, 117995.	6.4	26
17	Recent research progress on bio-oil conversion into bio-fuels and raw chemicals: a review. <i>Journal of Chemical Technology and Biotechnology</i> , 2019, 94, 670-689.	3.2	124
18	Origin and Nature of Coke in Ethanol Steam Reforming and Its Role in Deactivation of Ni/La <sub>2</sub> O <sub>3</sub> -Al <sub>2</sub> O <sub>3</sub> Catalyst. <i>Industrial &amp; Engineering Chemistry Research</i> , 2019, 58, 14736-14751.	3.7	70

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19	Cost-effective upgrading of biomass pyrolysis oil using activated dolomite as a basic catalyst. Fuel Processing Technology, 2019, 195, 106142.	7.2	43
20	Aqueous-phase reforming of bio-oil aqueous fraction over nickel-based catalysts. International Journal of Hydrogen Energy, 2019, 44, 13157-13168.	7.1	43
21	Effect of phenols extraction on the behavior of Ni-spinel derived catalyst for raw bio-oil steam reforming. International Journal of Hydrogen Energy, 2019, 44, 12593-12603.	7.1	35
22	On the dynamics and reversibility of the deactivation of a Rh/CeO <sub>2</sub> ZrO <sub>2</sub> catalyst in raw bio-oil steam reforming. International Journal of Hydrogen Energy, 2019, 44, 2620-2632.	7.1	25
23	Stability of a Rh/CeO <sub>2</sub> –ZrO <sub>2</sub> Catalyst in the Oxidative Steam Reforming of Raw Bio-oil. Energy & Fuels, 2018, 32, 3588-3598.	5.1	24
24	Coking and sintering progress of a Ni supported catalyst in the steam reforming of biomass pyrolysis volatiles. Applied Catalysis B: Environmental, 2018, 233, 289-300.	20.2	134
25	Temperature Programmed Oxidation Coupled with In-situ Techniques Reveal the Nature and Location of Coke Deposited on a Ni/La <sub>2</sub> O <sub>3</sub> –Al <sub>2</sub> O <sub>3</sub> Catalyst in the Steam Reforming of Bio-oil. ChemCatChem, 2018, 10, 2311-2321.	3.7	44
26	Kinetic Model for the Conversion of Chloromethane into Hydrocarbons over a HZSM-5 Zeolite Catalyst. Industrial & Engineering Chemistry Research, 2018, 57, 908-919.	3.7	11
27	Steam reforming of raw bio-oil over Ni/La <sub>2</sub> O <sub>3</sub> –Al <sub>2</sub> O <sub>3</sub> : Influence of temperature on product yields and catalyst deactivation. Fuel, 2018, 216, 463-474.	6.4	89
28	Biomass to hydrogen-rich gas via steam reforming of raw bio-oil over Ni/La <sub>2</sub> O <sub>3</sub> –Al <sub>2</sub> O <sub>3</sub> catalyst: Effect of space-time and steam-to-carbon ratio. Fuel, 2018, 216, 445-455.	6.4	79
29	Simultaneous modeling of the kinetics for n-pentane cracking and the deactivation of a HZSM-5 based catalyst. Chemical Engineering Journal, 2018, 331, 818-830.	12.7	53
30	Kinetic model considering catalyst deactivation for the steam reforming of bio-oil over Ni/La <sub>2</sub> O <sub>3</sub> –Al <sub>2</sub> O <sub>3</sub> . Chemical Engineering Journal, 2018, 332, 192-204.	12.7	36
31	Optimum operating conditions in ethanol steam reforming over a Ni/La <sub>2</sub> O <sub>3</sub> –Al <sub>2</sub> O <sub>3</sub> catalyst in a fluidized bed reactor. Fuel Processing Technology, 2018, 169, 207-216.	7.2	58
32	Oxidative Steam Reforming of Raw Bio-Oil over Supported and Bulk Ni Catalysts for Hydrogen Production. Catalysts, 2018, 8, 322.	3.5	31
33	Regeneration of NiAl <sub>2</sub> O <sub>4</sub> spinel type catalysts used in the reforming of raw bio-oil. Applied Catalysis B: Environmental, 2018, 237, 353-365.	20.2	59
34	Deactivation dynamics of a Ni supported catalyst during the steam reforming of volatiles from waste polyethylene pyrolysis. Applied Catalysis B: Environmental, 2017, 209, 554-565.	20.2	93
35	Comparison of Ni Based and Rh Based Catalyst Performance in the Oxidative Steam Reforming of Raw Bio-Oil. Energy & Fuels, 2017, 31, 7147-7156.	5.1	19
36	SAPO-18 and SAPO-34 catalysts for propylene production from the oligomerization-cracking of ethylene or 1-butene. Applied Catalysis A: General, 2017, 547, 176-182.	4.3	20

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37	Selective dealumination of HZSM-5 zeolite boosts propylene by modifying 1-butene cracking pathway. <i>Applied Catalysis A: General</i> , 2017, 543, 1-9.	4.3	30
38	Reaction conditions effect and pathways in the oxidative steam reforming of raw bio-oil on a Rh/CeO <sub>2</sub> -ZrO <sub>2</sub> catalyst in a fluidized bed reactor. <i>International Journal of Hydrogen Energy</i> , 2017, 42, 29175-29185.	7.1	25
39	Role of oxygenates and effect of operating conditions in the deactivation of a Ni supported catalyst during the steam reforming of bio-oil. <i>Green Chemistry</i> , 2017, 19, 4315-4333.	9.0	97
40	Deactivation kinetics for the conversion of dimethyl ether to olefins over a HZSM-5 zeolite catalyst. <i>Chemical Engineering Journal</i> , 2017, 311, 367-377.	12.7	58
41	Kinetic model for the reaction of DME to olefins over a HZSM-5 zeolite catalyst. <i>Chemical Engineering Journal</i> , 2016, 302, 801-810.	12.7	88
42	Kinetics of the steam reforming of dimethyl ether over CuFe <sub>2</sub> O <sub>4</sub> / $\gamma$ -Al <sub>2</sub> O <sub>3</sub> . <i>Chemical Engineering Journal</i> , 2016, 306, 401-412.	12.7	22
43	Reproducible performance of a Ni/La <sub>2</sub> O <sub>3</sub> - $\gamma$ -Al <sub>2</sub> O <sub>3</sub> catalyst in ethanol steam reforming under reaction-regeneration cycles. <i>Fuel Processing Technology</i> , 2016, 152, 215-222.	7.2	36
44	Development of a bifunctional catalyst for dimethyl ether steam reforming with CuFe <sub>2</sub> O <sub>4</sub> spinel as the metallic function. <i>Journal of Industrial and Engineering Chemistry</i> , 2016, 36, 169-179.	5.8	17
45	Comparison of Noble Metal- and Copper-Based Catalysts for the Step of Methanol Steam Reforming in the Dimethyl Ether Steam Reforming Process. <i>Industrial &amp; Engineering Chemistry Research</i> , 2016, 55, 3546-3555.	3.7	29
46	Controlling coke deactivation and cracking selectivity of MFI zeolite by H <sub>3</sub> PO <sub>4</sub> or KOH modification. <i>Applied Catalysis A: General</i> , 2015, 505, 105-115.	4.3	45
47	Role of Shape Selectivity and Catalyst Acidity in the Transformation of Chloromethane into Light Olefins. <i>Industrial &amp; Engineering Chemistry Research</i> , 2015, 54, 7822-7832.	3.7	20
48	Effect of Operating Conditions on Dimethyl Ether Steam Reforming over a CuFe <sub>2</sub> O <sub>4</sub> / $\gamma$ -Al <sub>2</sub> O <sub>3</sub> Bifunctional Catalyst. <i>Industrial &amp; Engineering Chemistry Research</i> , 2015, 54, 9722-9732.	3.7	32
49	Monitoring NiO and coke evolution during the deactivation of a Ni/La <sub>2</sub> O <sub>3</sub> - $\gamma$ -Al <sub>2</sub> O <sub>3</sub> catalyst in ethanol steam reforming in a fluidized bed. <i>Journal of Catalysis</i> , 2015, 331, 181-192.	6.2	208
50	Thermodynamic comparison between bio-oil and ethanol steam reforming. <i>International Journal of Hydrogen Energy</i> , 2015, 40, 15963-15971.	7.1	52
51	Behavior of a CuFe <sub>2</sub> O <sub>4</sub> / $\gamma$ -Al <sub>2</sub> O <sub>3</sub> Catalyst for the Steam Reforming of Dimethyl Ether in Reaction-Regeneration Cycles. <i>Industrial &amp; Engineering Chemistry Research</i> , 2015, 54, 11285-11294.	3.7	21
52	Strategies for maximizing the bio-oil valorization by catalytic transformation. <i>Journal of Cleaner Production</i> , 2015, 88, 345-348.	9.3	11
53	Hydrogen production by steam reforming of bio-oil/bio-ethanol mixtures in a continuous thermal-catalytic process. <i>International Journal of Hydrogen Energy</i> , 2014, 39, 6889-6898.	7.1	31
54	Modified HZSM-5 zeolites for intensifying propylene production in the transformation of 1-butene. <i>Chemical Engineering Journal</i> , 2014, 251, 80-91.	12.7	89

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55	Modifications in the HZSM-5 zeolite for the selective transformation of ethylene into propylene. <i>Applied Catalysis A: General</i> , 2014, 479, 17-25.	4.3	39
56	Comparison of Ni and Co Catalysts for Ethanol Steam Reforming in a Fluidized Bed Reactor. <i>Catalysis Letters</i> , 2014, 144, 1134-1143.	2.6	29
57	Compositional Insights and Valorization Pathways for Carbonaceous Material Deposited During Bio-Oil Thermal Treatment. <i>ChemSusChem</i> , 2014, 7, 2597-2608.	6.8	41
58	Kinetic Model for the Transformation of 1-Butene on a K-Modified HZSM-5 Catalyst. <i>Industrial &amp; Engineering Chemistry Research</i> , 2014, 53, 10599-10607.	3.7	34
59	Effect of Operating Conditions on Dimethyl Ether Steam Reforming in a Fluidized Bed Reactor with a CuO-ZnO-Al <sub>2</sub> O <sub>3</sub> and Desilicated ZSM-5 Zeolite Bifunctional Catalyst. <i>Industrial &amp; Engineering Chemistry Research</i> , 2014, 53, 3462-3471.	3.7	23
60	Causes of deactivation of bifunctional catalysts made up of CuO-ZnO-Al <sub>2</sub> O <sub>3</sub> and desilicated HZSM-5 zeolite in DME steam reforming. <i>Applied Catalysis A: General</i> , 2014, 483, 76-84.	4.3	44
61	Coke deactivation of Ni and Co catalysts in ethanol steam reforming at mild temperatures in a fluidized bed reactor. <i>International Journal of Hydrogen Energy</i> , 2014, 39, 12586-12596.	7.1	175
62	Upgrading of Bio-Oil in a Continuous Process with Dolomite Catalyst. <i>Energy &amp; Fuels</i> , 2014, 28, 6419-6428.	5.1	42
63	Reaction pathway for ethanol steam reforming on a Ni/SiO <sub>2</sub> catalyst including coke formation. <i>International Journal of Hydrogen Energy</i> , 2014, 39, 18820-18834.	7.1	131
64	Effect of calcination/reduction conditions of Ni/La <sub>2</sub> O <sub>3</sub> -Al <sub>2</sub> O <sub>3</sub> catalyst on its activity and stability for hydrogen production by steam reforming of raw bio-oil/ethanol. <i>Applied Catalysis B: Environmental</i> , 2014, 147, 402-410.	20.2	111
65	Intensifying Propylene Production by 1-Butene Transformation on a K Modified HZSM-5 Zeolite-Catalyst. <i>Industrial &amp; Engineering Chemistry Research</i> , 2014, 53, 4614-4622.	3.7	32
66	Kinetic behaviour of commercial catalysts for methane reforming in ethanol steam reforming process. <i>Journal of Energy Chemistry</i> , 2014, 23, 639-644.	12.9	8
67	Differences among the deactivation pathway of HZSM-5 zeolite and SAPO-34 in the transformation of ethylene or 1-butene to propylene. <i>Microporous and Mesoporous Materials</i> , 2014, 195, 284-293.	4.4	126
68	Stability of CuZnO/Al <sub>2</sub> O <sub>3</sub> /HZSM-5 and CuFe <sub>2</sub> O <sub>4</sub> /HZSM-5 catalysts in dimethyl ether steam reforming operating in reaction-regeneration cycles. <i>Fuel Processing Technology</i> , 2014, 126, 145-154.	7.2	40
69	Spatial Distribution of Zeolite ZSM-5 within Catalyst Bodies Affects Selectivity and Stability of Methanol-to-Hydrocarbons Conversion. <i>ChemCatChem</i> , 2013, 5, 2827-2831.	3.7	38
70	Kinetic behaviour of catalysts with different CuO-ZnO-Al <sub>2</sub> O <sub>3</sub> metallic function compositions in DME steam reforming in a fluidized bed. <i>Applied Catalysis B: Environmental</i> , 2013, 142-143, 315-322.	20.2	32
71	Operating conditions for attenuating Ni/La <sub>2</sub> O <sub>3</sub> -Al <sub>2</sub> O <sub>3</sub> catalyst deactivation in the steam reforming of bio-oil aqueous fraction. <i>Fuel Processing Technology</i> , 2013, 115, 222-232.	7.2	122
72	Steam Reforming of Raw Bio-oil in a Fluidized Bed Reactor with Prior Separation of Pyrolytic Lignin. <i>Energy &amp; Fuels</i> , 2013, 27, 7549-7559.	5.1	71

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73	Effect of combining metallic and acid functions in CZA/HZSM-5 desilicated zeolite catalysts on the DME steam reforming in a fluidized bed. International Journal of Hydrogen Energy, 2013, 38, 10019-10028.	7.1	34
74	Improving the DME steam reforming catalyst by alkaline treatment of the HZSM-5 zeolite. Applied Catalysis B: Environmental, 2013, 130-131, 73-83.	20.2	59
75	Catalysts of Ni/Al <sub>2</sub> O <sub>3</sub> and Ni/La <sub>2</sub> O <sub>3</sub> -Al <sub>2</sub> O <sub>3</sub> for hydrogen production by steam reforming of bio-oil aqueous fraction with pyrolytic lignin retention. International Journal of Hydrogen Energy, 2013, 38, 1307-1318.	7.1	111
76	Steam Reforming of the Bio-Oil Aqueous Fraction in a Fluidized Bed Reactor with in Situ CO <sub>2</sub> Capture. Industrial & Engineering Chemistry Research, 2013, 52, 17087-17098.	3.7	40
77	Joint Transformation of Methanol and n-Butane into Olefins on an HZSM-5 Zeolite Catalyst in Reaction-Regeneration Cycles. Industrial & Engineering Chemistry Research, 2012, 51, 13073-13084.	3.7	7
78	Effect of operating conditions on the coke nature and HZSM-5 catalysts deactivation in the transformation of crude bio-oil into hydrocarbons. Catalysis Today, 2012, 195, 106-113.	4.4	101
79	Deactivating species in the transformation of crude bio-oil with methanol into hydrocarbons on a HZSM-5 catalyst. Journal of Catalysis, 2012, 285, 304-314.	6.2	175
80	Deactivation kinetics of a HZSM-5 zeolite catalyst treated with alkali for the transformation of bioethanol into hydrocarbons. AIChE Journal, 2012, 58, 526-537.	3.6	27
81	Effect of Cofeeding Butane with Methanol on the Deactivation by Coke of a HZSM-5 Zeolite Catalyst. Industrial & Engineering Chemistry Research, 2011, 50, 9980-9988.	3.7	67
82	Kinetic modelling for the transformation of bioethanol into olefins on a hydrothermally stable Ni-HZSM-5 catalyst considering the deactivation by coke. Chemical Engineering Journal, 2011, 167, 262-277.	12.7	73
83	Olefin production by cofeeding methanol and n-butane: Kinetic modeling considering the deactivation of HZSM-5 zeolite. AIChE Journal, 2011, 57, 2841-2853.	3.6	39
84	Hydrothermally stable HZSM-5 zeolite catalysts for the transformation of crude bio-oil into hydrocarbons. Applied Catalysis B: Environmental, 2010, 100, 318-327.	20.2	124
85	Hydrothermal stability of HZSM-5 catalysts modified with Ni for the transformation of bioethanol into hydrocarbons. Fuel, 2010, 89, 3365-3372.	6.4	96
86	Catalyst discrimination for olefin production by coupled methanol/n-butane cracking. Applied Catalysis A: General, 2010, 383, 202-210.	4.3	36
87	Selective production of olefins from bioethanol on HZSM-5 zeolite catalysts treated with NaOH. Applied Catalysis B: Environmental, 2010, 97, 299-306.	20.2	135
88	Synergies in the production of olefins by combined cracking of n-butane and methanol on a HZSM-5 zeolite catalyst. Chemical Engineering Journal, 2010, 160, 760-769.	12.7	47
89	Kinetic Modeling of n-Butane Cracking on HZSM-5 Zeolite Catalyst. Industrial & Engineering Chemistry Research, 2010, 49, 8415-8423.	3.7	40
90	Selective Production of Aromatics by Crude Bio-oil Valorization with a Nickel-Modified HZSM-5 Zeolite Catalyst. Energy & Fuels, 2010, 24, 2060-2070.	5.1	164

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91	Kinetics of Methanol Transformation into Hydrocarbons on a HZSM-5 Zeolite Catalyst at High Temperature (400-550 °C). <i>Industrial &amp; Engineering Chemistry Research</i> , 2010, 49, 12371-12378.	3.7	64
92	Olefin Production by Catalytic Transformation of Crude Bio-Oil in a Two-Step Process. <i>Industrial &amp; Engineering Chemistry Research</i> , 2010, 49, 123-131.	3.7	119
93	Kinetic Model for the Transformation of Bioethanol into Olefins over a HZSM-5 Zeolite Treated with Alkali. <i>Industrial &amp; Engineering Chemistry Research</i> , 2010, 49, 10836-10844.	3.7	52
94	Attenuation of Catalyst Deactivation by Cofeeding Methanol for Enhancing the Valorisation of Crude Bio-oil. <i>Energy &amp; Fuels</i> , 2009, 23, 4129-4136.	5.1	88
95	Kinetic modelling of methylcyclohexane ring-opening over a HZSM-5 zeolite catalyst. <i>Chemical Engineering Journal</i> , 2008, 140, 287-295.	12.7	23
96	Deactivation of a CuO-ZnO/Al <sub>2</sub> O <sub>3</sub> /Al <sub>2</sub> O <sub>3</sub> Catalyst in the Synthesis of Dimethyl Ether. <i>Industrial &amp; Engineering Chemistry Research</i> , 2008, 47, 2238-2247.	3.7	97
97	The Role of Zeolite Acidity in Coupled Toluene Hydrogenation and Ring Opening in One and Two Steps. <i>Industrial &amp; Engineering Chemistry Research</i> , 2008, 47, 665-671.	3.7	16
98	Study of Complex Reactions under Rapid Deactivation -- Improvements in the Reaction Equipment and in the Methodology for Kinetic Calculation. <i>International Journal of Chemical Reactor Engineering</i> , 2007, 5, .	1.1	0
99	Kinetic Modeling of the Methanol-to-Olefins Process on a Silicoaluminophosphate (SAPO-18) Catalyst by Considering Deactivation and the Formation of Individual Olefins. <i>Industrial &amp; Engineering Chemistry Research</i> , 2007, 46, 1981-1989.	3.7	65
100	Integration of Thermal Treatment and Catalytic Transformation for Upgrading Biomass Pyrolysis Oil. <i>International Journal of Chemical Reactor Engineering</i> , 2007, 5, .	1.1	21
101	Development of Alternative Catalysts Based on HZSM-5 Zeolite for the BTO Process. <i>International Journal of Chemical Reactor Engineering</i> , 2007, 5, .	1.1	3
102	Kinetic Study of the Simultaneous Cracking of Paraffins and Methanol on HZSM-5 Zeolite Catalysts. <i>International Journal of Chemical Reactor Engineering</i> , 2007, 5, .	1.1	2
103	Role of acidity and microporous structure in alternative catalysts for the transformation of methanol into olefins. <i>Applied Catalysis A: General</i> , 2005, 283, 197-207.	4.3	164
104	Undesired components in the transformation of biomass pyrolysis oil into hydrocarbons on an HZSM-5 zeolite catalyst. <i>Journal of Chemical Technology and Biotechnology</i> , 2005, 80, 1244-1251.	3.2	135
105	Kinetic Behavior of the SAPO-18 Catalyst in the Transformation of Methanol into Olefins. <i>Industrial &amp; Engineering Chemistry Research</i> , 2005, 44, 6605-6614.	3.7	17
106	Initiation Step and Reactive Intermediates in the Transformation of Methanol into Olefins over SAPO-18 Catalyst. <i>Industrial &amp; Engineering Chemistry Research</i> , 2005, 44, 7279-7286.	3.7	45
107	Kinetic Description of the Catalytic Pyrolysis of Biomass in a Conical Spouted Bed Reactor. <i>Energy &amp; Fuels</i> , 2005, 19, 765-774.	5.1	122
108	ROLE OF WATER IN THE KINETIC MODELING OF METHANOL TRANSFORMATION INTO HYDROCARBONS ON HZSM-5 ZEOLITE. <i>Chemical Engineering Communications</i> , 2004, 191, 944-967.	2.6	35

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109	Role of Reaction-Medium Water on the Acidity Deterioration of a HZSM-5 Zeolite. <i>Industrial &amp; Engineering Chemistry Research</i> , 2004, 43, 5042-5048.	3.7	65
110	Transformation of Oxygenate Components of Biomass Pyrolysis Oil on a HZSM-5 Zeolite. II. Aldehydes, Ketones, and Acids. <i>Industrial &amp; Engineering Chemistry Research</i> , 2004, 43, 2619-2626.	3.7	363
111	Deactivation of a HZSM-5 Zeolite Catalyst in the Transformation of the Aqueous Fraction of Biomass Pyrolysis Oil into Hydrocarbons. <i>Energy &amp; Fuels</i> , 2004, 18, 1640-1647.	5.1	161
112	Transformation of Oxygenate Components of Biomass Pyrolysis Oil on a HZSM-5 Zeolite. I. Alcohols and Phenols. <i>Industrial &amp; Engineering Chemistry Research</i> , 2004, 43, 2610-2618.	3.7	402
113	Study of the preparation and composition of the metallic function for the selective hydrogenation of CO <sub>2</sub> to gasoline over bifunctional catalysts. <i>Journal of Chemical Technology and Biotechnology</i> , 2003, 78, 161-166.	3.2	23
114	Kinetics of the irreversible deactivation of the HZSM-5 catalyst in the MTO process. <i>Chemical Engineering Science</i> , 2003, 58, 5239-5249.	3.8	108
115	Study of the regeneration stage of the MTG process in a pseudoadiabatic fixed bed reactor. <i>Chemical Engineering Journal</i> , 2003, 92, 141-150.	12.7	5
116	Coke Aging and Its Incidence on Catalyst Regeneration. <i>Industrial &amp; Engineering Chemistry Research</i> , 2003, 42, 3914-3921.	3.7	50
117	Catalyst Deactivation by Coke in the Transformation of Aqueous Ethanol into Hydrocarbons. Kinetic Modeling and Acidity Deterioration of the Catalyst. <i>Industrial &amp; Engineering Chemistry Research</i> , 2002, 41, 4216-4224.	3.7	123
118	Role of water in the kinetic modeling of catalyst deactivation in the MTG process. <i>AIChE Journal</i> , 2002, 48, 1561-1571.	3.6	87
119	Study of operating variables in the transformation of aqueous ethanol into hydrocarbons on an HZSM-5 zeolite. <i>Journal of Chemical Technology and Biotechnology</i> , 2002, 77, 211-216.	3.2	104
120	Kinetic Modelling of the Transformation of Aqueous Ethanol into Hydrocarbons on a HZSM-5 Zeolite. <i>Industrial &amp; Engineering Chemistry Research</i> , 2001, 40, 3467-3474.	3.7	67
121	MTG Process in a Fixed-Bed Reactor. Operation and Simulation of a Pseudoadiabatic Experimental Unit. <i>Industrial &amp; Engineering Chemistry Research</i> , 2001, 40, 6087-6098.	3.7	13
122	Catalyst reactivation kinetics for methanol transformation into hydrocarbons. Expressions for designing reaction-regeneration cycles in isothermal and adiabatic fixed bed reactor. <i>Chemical Engineering Science</i> , 2001, 56, 5059-5071.	3.8	26
123	Conversion of syngas to liquid hydrocarbons over a two-component (Cr <sub>2</sub> O <sub>3</sub> -ZnO and ZSM-5 zeolite) catalyst. <i>Chemical Engineering Science</i> , 2000, 55, 1845-1855.	3.8	17
124	MTG fluidized bed reactor-regenerator unit with catalyst circulation: process simulation and operation of an experimental setup. <i>Chemical Engineering Science</i> , 2000, 55, 3223-3235.	3.8	25
125	Kinetic Modeling of Methanol Transformation into Olefins on a SAPO-34 Catalyst. <i>Industrial &amp; Engineering Chemistry Research</i> , 2000, 39, 292-300.	3.7	98
126	COMPOSITION AND QUALITY OF THE GASOLINE OBTAINED FROM SYNGAS ON Cr <sub>2</sub> O <sub>3</sub> -ZnO/ZSM5 CATALYSTS. <i>Chemical Engineering Communications</i> , 1999, 174, 1-19.	2.6	10



#	ARTICLE	IF	CITATIONS
127	COKE COMBUSTION AND REACTIVATION KINETICS OF A ZSM-5 ZEOLITE BASED CATALYST USED FOR THE TRANSFORMATION OF METHANOL INTO HYDROCARBONS. Chemical Engineering Communications, 1999, 176, 43-63.	2.6	15
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138	Deposition and Characteristics of Coke over a H-ZSM5 Zeolite-Based Catalyst in the MTG Process. Industrial & Engineering Chemistry Research, 1996, 35, 3991-3998.	3.7	103
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141	Relationship between surface acidity and activity of catalysts in the transformation of methanol into hydrocarbons. Journal of Chemical Technology and Biotechnology, 1996, 65, 186-192.	3.2	75
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