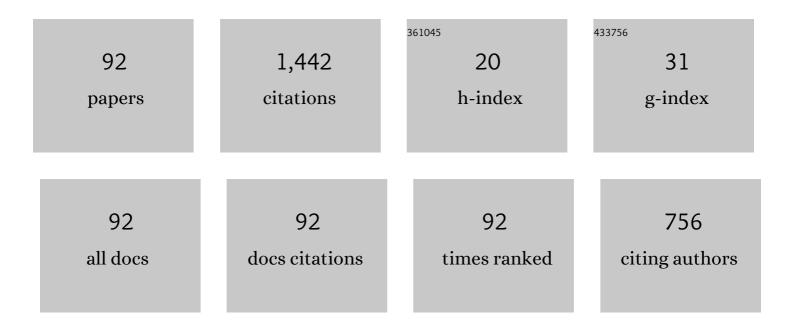
So-Jin Park

List of Publications by Year in descending order

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#	Article	IF	CITATIONS
1	lsothermal Vaporâ^'Liquid Equilibria at 333.15 K and Excess Molar Volumes at 298.15 K of Ethyltert-Butyl Ether (ETBE) + Alcoh-1-ol (C1â^'C4) Mixtures. Journal of Chemical & Engineering Data, 1998, 43, 1009-1013.	1.0	70
2	Phase Equilibrium and Physical Properties for the Purification of Propylene Carbonate (PC) and Î ³ -Butyrolactone (GBL). Journal of Chemical & Engineering Data, 2011, 56, 89-96.	1.0	62
3	Vapor–liquid equilibria and excess properties for methyl tert-butyl ether (MTBE) containing binary systems. Fluid Phase Equilibria, 2002, 200, 399-409.	1.4	58
4	Excess Molar Volumes and Viscosity Deviations for the Ternary System N,N-Dimethylformamide + N-Methylformamide + Water and the Binary Subsystems at 298.15 K. Journal of Chemical & Engineering Data, 2005, 50, 1951-1955.	1.0	46
5	Liquid–liquid equilibria for methanol + hexadecane + heterocyclic nitrogen-containing compounds at 298.15 K. Fluid Phase Equilibria, 2002, 193, 217-227.	1.4	45
6	lsothermal Vaporâ^'Liquid Equilibria of 2-Methoxy-2-methylbutane (TAME) +n-Alcohol (C1â^'C4) Mixtures at 323.15 and 333.15 K. Journal of Chemical & Engineering Data, 1997, 42, 517-522.	1.0	42
7	Isothermal vapor–liquid equilibria and excess molar volumes for 2-methyl pyrazine (2MP) containing binary mixtures. Fluid Phase Equilibria, 2001, 180, 361-373.	1.4	42
8	Isothermal Vaporâ^'Liquid Equilibrium Data at <i>T</i> = 333.15 K and Excess Molar Volumes and Refractive Indices at <i>T</i> = 298.15 K for the Dimethyl Carbonate + Methanol and Isopropanol + Water with Ionic Liquids. Journal of Chemical & Engineering Data, 2010, 55, 2474-2481.	1.0	40
9	Liquid–liquid equilibria for the binary system of di-isopropyl ether (DIPE)+water in between 288.15 and 323.15K and the ternary systems of DIPE+water+C1–C4 alcohols at 298.15K. Fluid Phase Equilibria, 2008, 269, 1-5.	1.4	37
10	Liquid–liquid equilibria for ternary systems of dimethyl carbonate+C1–C4 alcohols+water at 298.15K and atmospheric pressure. Journal of Industrial and Engineering Chemistry, 2012, 18, 499-503.	2.9	36
11	Vaporâ^'Liquid Equilibria andHEfor Binary Systems of Dimethyl Ether (DME) with C1â^'C4Alkan-1-ols at 323.15 K and Liquidâ^'Liquid Equilibria for Ternary System of DME + Methanol + Water at 313.15 K. Journal of Chemical & Engineering Data, 2007, 52, 230-234.	1.0	28
12	lsothermal Vaporâ^'Liquid Equilibrium at 333.15 K, Density, and Refractive Index at 298.15 K for the Ternary Mixture of Dibutyl Ether + Ethanol + Benzene and Binary Subsystems. Journal of Chemical & Engineering Data, 2007, 52, 1018-1024.	1.0	28
13	Excess molar volumes and deviations of refractive indices at 298.15K for binary and ternary mixtures with pyridine or aniline or quinoline. Journal of Industrial and Engineering Chemistry, 2010, 16, 200-206.	2.9	28
14	Isothermal Phase Equilibria and Excess Molar Enthalpies for Binary Systems with Dimethyl Ether at 323.15 K. Journal of Chemical & Engineering Data, 2007, 52, 1814-1818.	1.0	27
15	Densities and Viscosities for the Ternary Systems of Methyltert-Butyl Ether + Methanol + Benzene and Methyltert-Butyl Ether + Methanol + Toluene and Their Sub-binary Systems at 298.15 K. Journal of Chemical & Engineering Data, 2006, 51, 1339-1344.	1.0	26
16	lsothermal vapor–liquid equilibrium at 333.15K and excess volumes and molar refractivity deviation at 298.15K for the ternary system di-butyl ether (1)+ethanol (2)+toluene (3) and its binary subsystems. Fluid Phase Equilibria, 2007, 262, 161-168.	1.4	26
17	Liquid–liquid equilibria of ternary mixtures of dimethyl carbonate, diphenyl carbonate, phenol and water at 358.15K. Fluid Phase Equilibria, 2011, 301, 18-21.	1.4	25
18	Binary Liquidâ^'Liquid Equilibrium (LLE) for <i>N</i> -Methylformamide (NMF) + Hexadecane between (288.15 and 318.15) K and Ternary LLE for Systems of NMF + Heterocyclic Nitrogen Compounds + Hexadecane at 298.15 K. Journal of Chemical & Engineering Data, 2009, 54, 78-82.	1.0	23

#	Article	IF	CITATIONS
19	Isothermal VLE and VE at 303.15 K for the Binary and Ternary Mixtures of Di-isopropyl Ether (DIPE) + 1-Propanol + 2,2,4-Trimethylpentane. Journal of Chemical & Engineering Data, 2007, 52, 2503-2508.	1.0	21
20	lsothermal vapor–liquid equilibrium at 333.15K and excess molar volumes and refractive indices at 298.15K for the mixtures of di-methyl carbonate, ethanol and 2,2,4-trimethylpentane. Fluid Phase Equilibria, 2009, 276, 142-149.	1.4	21
21	Liquid–Liquid Equilibria for Ternary Mixtures of Methylphenyl Carbonate, Dimethyl Carbonate, Diphenyl Carbonate, Anisole, Methanol, Phenol, and Water at Several Temperatures. Journal of Chemical & Engineering Data, 2014, 59, 323-328.	1.0	21
22	Liquid–liquid equilibria for ternary mixtures of methyl tert-butyl ether, ethyl tert-butyl ether, water and imidazolium-based ionic liquids at 298.15 K. Journal of Industrial and Engineering Chemistry, 2014, 20, 3292-3296.	2.9	21
23	Excess molar volumes and refractive indices at 298.15K for the binary and ternary mixtures of diisopropyl ether+ethanol+2,2,4-trimethylpentane. Journal of Industrial and Engineering Chemistry, 2008, 14, 377-381.	2.9	20
24	Binary Liquidâ^'Liquid Equilibrium (LLE) for Dibutyl Ether (DBE) + Water from (288.15 to 318.15) K and Ternary LLE for Systems of DBE + C1 â^¼ C4 Alcohols + Water at 298.15 K. Journal of Chemical & Engineering Data, 2008, 53, 2089-2094.	1.0	20
25	(Liquid + Liquid) Equilibrium for (<i>N</i> , <i>N-</i> Dimethylformamide (DMF) + Hexadecane) at Temperatures between (293.15 and 313.15) K and Ternary Mixtures of (DMF + Hexadecane) with Either Quinoline, or Pyridine, or Pyrrole, or Aniline, or Indole at <i>T</i> = 298.15 K. Journal of Chemical & amp: Engineering Data, 2010, 55, 1266-1270.	1.0	20
26	Solid–liquid equilibria and the physical properties of binary systems of diphenyl carbonate, dimethyl carbonate, anisole, methanol and phenol. Fluid Phase Equilibria, 2014, 376, 105-110.	1.4	20
27	Vapor-liquid equilibria and excess molar properties of MTBE + methanol and + ethanol mixtures. Korean Journal of Chemical Engineering, 1995, 12, 110-114.	1.2	19
28	Vapor–liquid equilibria for the ternary systems of methyl tert-butyl ether + methanol + benzene and methyl tert-butyl ether + methanol + toluene and constituent binary systems at 313.15 K. Fluid Phase Equilibria, 2003, 209, 215-228.	1.4	19
29	Measurement and Correlation of Vaporâ`'Liquid Equilibria atT= 333.15 K and Excess Molar Volumes atT= 298.15 K for Ethanol + Dimethyl Carbonate (DMC), DMC + 1-Propanol, and DMC + 1-Butanol. Journal of Chemical & Engineering Data, 2006, 51, 1852-1855.	1.0	19
30	Solidâ^'Liquid Equilibria, Excess Molar Volumes, and Molar Refractivity Deviations for Extractive Solvents of Molybdenum. Journal of Chemical & Engineering Data, 2010, 55, 1179-1185.	1.0	18
31	Excess Molar Volumes at 298.15 K and Isothermal Vaporâ^'Liquid Equilibria at 333.15 K for the Binary Mixtures of Dimethyl Carbonate with Benzene, Toluene,n-Heptane, and Isooctane. Journal of Chemical & Engineering Data, 2006, 51, 1868-1872.	1.0	17
32	lsothermal vapor–liquid equilibrium at 333.15K, excess molar volumes and refractive indices at 298.15K for mixtures of tert-amyl methyl ether+ethanol+2,2,4-trimethylpentane. Fluid Phase Equilibria, 2009, 281, 5-11.	1.4	17
33	Isothermal Vaporâ^'Liquid Equilibrium at 333.15 K and Excess Molar Volumes, Refractive Indices, and Excess Molar Enthalpies at 303.15 K for the Binary and Ternary Mixtures of Di-isopropyl Ether, Ethanol, and 2,2,4-Trimethylpentane. Journal of Chemical & Engineering Data, 2009, 54, 3051-3058.	1.0	17
34	Liquidâ^'Liquid Equilibria for Binary System of Ethanol + Hexadecane at Elevated Temperature and the Ternary Systems of Ethanol + Heterocyclic Nitrogen Compounds + Hexadecane at 298.15 K. Journal of Chemical & Engineering Data, 2007, 52, 1919-1924.	1.0	16
35	Isothermal Binary and Ternary VLE for the Mixtures of Propyl Vinyl Ether + Ethanol + Isooctane at 323.15 K andVEat 293.15 K. Journal of Chemical & Engineering Data, 2007, 52, 1118-1122.	1.0	15
36	lsothermal vapor–liquid equilibrium at 303.15K and excess molar volumes at 298.15K for the ternary system of propyl vinyl ether+1-propanol+2,2,4-trimethyl-pentane and its binary sub-systems. Fluid Phase Equilibria, 2007, 259, 146-152.	1.4	15

IF # ARTICLE CITATIONS Thermo-physical properties, excess and deviation properties for a mixture of \hat{I}^3 -butyrolactone with 1.2 diethyl carbonate or propylene carbonate. Korean Journal of Chemical Engineering, 2018, 35, 222-233. Volumetric, enthalpic and VLE studies of binary mixtures of isomers of butyl chloride with 38 2.3 15 cyclohexane at 298.15†K. Journal of Molecular Liquids, 2020, 298, 111946. Density and viscosity studies of mixtures of oxygenate with n-alkanes (C9-C12) at (298.15, 308.15 and) Tj ETQq1 1 0.784314 rgBT /C 2.3 Molecular Liquids, 2020, 306, 112859. Isothermal vaporâ€"liquid equilibrium at 323.15K and excess molar volumes and refractive indices at 298.15K for the ternary system propyl vinyl ether+1-propanol+benzene and its binary sub-systems. Fluid 40 1.4 14 Phase Equilibria, 2008, 274, 73-79. Isothermal vaporâ \in 'liquid equilibrium at T=333.15K and excess volumes and molar refractivity deviation at T=298.15K for the ternary mixtures {di-methyl carbonate (DMC)+ethanol+benzene} and {DMC+ethanol+toluene}. Fluid Phase Equilibria, 2011, 303, 150-156. 1.4 14 Azeotrope breaking for the system ethyl tert-butyl ether (ETBE)+ethanol at 313.15K and excess 42 properties at 298.15K for mixtures of ETBE and ethanol with phosphonium-based ionic liquids. Fluid 1.4 14 Phase Equilibria, 2013, 344, 32-37. Liquid–liquid equilibria, excess molar volume and deviations of the refractive indices at 298.15K for mixtures of solvents used in the molybdenum extraction process. Fluid Phase Equilibria, 2013, 354, 1.4 59-65. Vaporâ[^]Liquid Equilibria for the Ternary Systems of Methyltert-Butyl Ether + Methanol + Methylcyclohexane and Methyltert-Butyl Éther + Methanól +n-Heptane and Constituent Binary 44 1.0 12 Systems at 313.15 K. Journal of Chemical & amp; Engineering Data, 2005, 50, 1564-1569. Liquid–liquid equilibrium for binary and ternary systems containing di-isopropyl ether (DIPE) and an 1.4 imidazolium-based ionic liquid at different temperatures. Fluid Phase Equilibria, 2010, 299, 294-299. Liquid–liquid equilibria at 298.15K for ternary mixtures of methyl tert-butyl ether+methanol (or) Tj ETQq0 0 0 rgBT /Overlock 10 Tf 50 46 1.4 12 82-87. Vapor–liquid equilibrium, densities and viscosities for the binary system exo- and endo-tetrahydrodicyclopentadiene and pure component vapor pressures. Fluid Phase Equilibria, 2006, 1.4 249, 187-191. Binary LLE for Propyl Vinyl Ether (PVE) + Water, Ternary LLE for PVE + Methanol or Ethanol + Water at 298.15 K, and <i>V</i>^E and Î"<i>R</i> at 293.15 K for the Mixture of PVE + Ethanol + 48 1.0 11

	2,2,4-Trimethylpentane. Journal of Chemical & Engineering Data, 2007, 52, 2395-2399.		
49	Density, refractive index, excess molar volumes and deviations in molar refraction at 298.15 K for binary and ternary mixtures of DIPE (OR TAME) + 1â€methanol (or) Tj ETQq1 1 0.784314 rgBT /Overlock	10 Tf 50 2	262 Td (18
	of Chemical Engineering, 2012, 90, 396-402.		
50	Hydrothermal Desorption of Cs with Oxalic Acid from Hydrobiotite and Wastewater Treatment by Chemical Precipitation. Energies, 2020, 13, 3284.	1.6	11
51	Isothermal vapor–liquid equilibria and excess molar volumes for the ternary mixtures containing 2-methyl pyrazine. Fluid Phase Equilibria, 2002, 193, 109-121.	1.4	10
52	SLE and LLE for tri-butylphosphate or tri-octylamine contained systems; extractive solvents of Molybdenum. Fluid Phase Equilibria, 2010, 295, 172-176.	1.4	10
53	Liquidâ^'Liquid Equilibrium, Solidâ^'Liquid Equilibrium, Densities, and Refractivity of a Water, Chloroform, and Acetylacetone Mixture. Journal of Chemical & Engineering Data, 2011, 56, 1798-1803.	1.0	10
54	Liquid–liquid equilibria for aqueous sulfuric acid solutions with undecane, dodecane, or 1-dodecanol, trioctylamine or tributyl phosphate and excess and deviation properties for sub-binary systems at 298.15K. Fluid Phase Equilibria, 2013, 343, 36-42.	1.4	10

#	Article	IF	CITATIONS
55	Volumetric, acoustic and optical studies of ternary mixture of diisopropyl ether, n-heptane and n-octane. Journal of Molecular Liquids, 2020, 306, 112605.	2.3	10
56	Fractionation of Aromatic Heavy Oil by Dynamic Supercritical Fluid Extraction. Industrial & Engineering Chemistry Research, 2000, 39, 4897-4900.	1.8	9
57	Excess molar enthalpies for the binary and ternary mixtures of ether compounds (di-isopropyl ether,) Tj ETQq1 1 C Engineering, 2008, 25, 1160-1164.).784314 r 1.2	rgBT /Overlo 9
58	Liquid–liquid equilibria in the ternary systems {hexadecane+BTX aromatics+2-methoxyethanol or acetonitrile} at 298.15K. Fluid Phase Equilibria, 2015, 389, 9-15.	1.4	9
59	The selectivity of imidazolium-based ionic liquids with different anions to BTX aromatics in hexane at 298.15 K and atmospheric pressure. Korean Journal of Chemical Engineering, 2016, 33, 2982-2989.	1.2	9
60	Density, refractive index and kinematic viscosity of MIPK, MEK and phosphonium-based ionic liquids and the excess and deviation properties of their binary systems. Korean Journal of Chemical Engineering, 2017, 34, 214-224.	1.2	9
61	Cs desorption behavior during hydrothermal treatment of illite with oxalic acid. Environmental Science and Pollution Research, 2020, 27, 35580-35590.	2.7	9
62	Binary Liquidâ [~] Liquid Equilibrium (LLE) for Methyl <i>tert</i> Amyl Ether (TAME) + Water from (288.15) Tj ETQqC 298.15 K. Journal of Chemical & Engineering Data, 2008, 53, 2878-2883.	0 0 rgBT 1.0	Overlock 10 8
63	The liquid–liquid equilibria for low pH aqueous acid solution+tri-octylamine (or) Tj ETQq1 1 0.784314 rgBT /Ove refractive indices. Fluid Phase Equilibria, 2012, 314, 7-12.	erlock 10 T 1.4	f 50 427 Td 8
64	The solid–liquid equilibrium, excess molar volume and refractive deviation properties of binary systems containing dimethyl carbonate, anisole and phenol. Fluid Phase Equilibria, 2014, 383, 21-26.	1.4	8
65	Solid–Liquid Equilibria, Excess Molar Volumes, and Deviations in the Molar Refractivity for the Binary Systems of Alamine 304-1 + Decane, Dodecane, or Dodecanol. Journal of Chemical & Engineering Data, 2014, 59, 289-294.	1.0	8
66	Colorimetric Method for Detection of Hydrazine Decomposition in Chemical Decontamination Process. Energies, 2019, 12, 3967.	1.6	8
67	Measurement and modelling of solid-liquid equilibria, density and viscosity of fatty acid methyl or ethyl esters. Journal of Molecular Liquids, 2020, 314, 113628.	2.3	8
68	Ternary liquid–liquid equilibria and binary excess and deviation properties at constant temperature for mixtures of dimethyl carbonate, anisole, methanol, phenol and water. Fluid Phase Equilibria, 2014, 378, 93-101.	1.4	7
69	Isothermal vapor-liquid equilibria, excess molar volume and the deviation of refractive indices for binary mixtures of 1-butanol, 1-hexanol, 3-methyl-1-butanol and butyl acetate. Fluid Phase Equilibria, 2017, 436, 47-54.	1.4	7
70	Liquid–Liquid Equilibrium for Ternary Systems of Propyl Vinyl Ether + C ₃ or C ₄ Alcohols + Water at 298.15 K and Excess Molar Enthalpies for Ternary and Constituent Binary Systems of Propyl Vinyl Ether + Ethanol + Isooctane at 303.15 K. Journal of Chemical & Engineering Data, 2008, 53, 475-480.	1.0	6
71	Binary and Ternary Vaporâ^`Liquid Equilibrium at 323.15 K and Excess Molar Volumes at 298.15 K for the Mixtures of Propyl Vinyl Ether + 1-Propanol + Toluene. Journal of Chemical & Engineering Data, 2009, 54, 1041-1045.	1.0	6
72	Isothermal Vaporâ^'Liquid Equilibrium at 333.15 K and Excess Volumes and Molar Refractivity Deviation at 298.15 K for Binary System Dibutyl Ether (DBE) + 2,2,4-Trimethylpentane and for Ternary System DBE + Ethanol + 2,2,4-Trimethylpentane. Journal of Chemical & Engineering Data, 2010, 55, 864-870.	1.0	6

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73	Vapor–liquid equilibria at 333.15K and excess molar volumes and deviations in molar refractivity at 298.15K for mixtures of diisopropyl ether, ethanol and ionic liquids. Fluid Phase Equilibria, 2011, 309, 145-145.	1.4	6
74	Solid–liquid equilibrium and mixture properties for the binary systems of Alamine 336 with decane, dodecane, and 1-dodecanol. Fluid Phase Equilibria, 2014, 361, 130-134.	1.4	6
75	Isothermal vapor–liquid equilibrium at 333.15K and excess molar volumes at 298.15K for the ternary system di-isopropyl ether+n-propyl alcohol+toluene and its binary subsystems. Fluid Phase Equilibria, 2008, 270, 103-108.	1.4	5
76	Solid–liquid equilibrium, excess molar volume, and deviations in the molar refractivity for the binary and ternary mixtures of Alamine 304-1 with 1-octanol, 2-octanol, and 1-decanol. Fluid Phase Equilibria, 2012, 324, 44-49.	1.4	5
77	Measurement and modeling of transport properties of binary liquid mixtures containing oxygenates and n-alkanes. Korean Journal of Chemical Engineering, 2019, 36, 1922-1931.	1.2	5
78	Measurement and correlation of thermodynamic properties of ternary mixtures of oxygenated fuel. Korean Journal of Chemical Engineering, 2020, 37, 1181-1194.	1.2	5
79	Excess molar volumes at the 308.15 K for constituent binaries of n-decane, n-dodecane, 1-decanol and 1-dodecanol. Korean Journal of Chemical Engineering, 1995, 12, 152-155.	1.2	4
80	Isobaric vapor–liquid equilibrium at 101.3 kPa and excess properties at 298.15 K for binary mixtures of methyl phenyl carbonate with methanol or dimethyl carbonate. Fluid Phase Equilibria, 2013, 360, 260-264.	1.4	4
81	Tracking the distribution of organic compounds using fugacity model. Korean Journal of Chemical Engineering, 2000, 17, 12-16.	1.2	2
82	Liquid–liquid equilibria for the pseudo-ternary system {aqueous sulfuric acid solution+methyl ethyl ketone or methyl isopropyl ketone+phosphonium-based ionic liquids} at 298.15K and atmospheric pressure. Fluid Phase Equilibria, 2013, 358, 1-6.	1.4	2
83	Solid-liquid phase equilibria, excess molar volume, and molar refraction deviation for the mixtures of ethanoic acid with propanoic, butanoic, and pentanoic acid. Korean Journal of Chemical Engineering, 2018, 35, 1710-1715.	1.2	2
84	Pattern formation using polystyrene benzaldimine selfâ€assembled monolayer by soft Xâ€ray. Surface and Interface Analysis, 2019, 51, 408-412.	0.8	2
85	Excess molar volumes for titanium butoxide contained binary and ternary systems at 298.15K. Journal of Industrial and Engineering Chemistry, 2008, 14, 243-246.	2.9	1
86	Numerical analysis of flow distribution for combined weapon system in environmental tester. Journal of Mechanical Science and Technology, 2012, 26, 3339-3345.	0.7	1
87	Homeotropic alignment of liquid crystals on ITO surface using LBL assembly. Journal of the Society for Information Display, 2018, 26, 413-418.	0.8	1
88	Solid-liquid equilibria and thermo-physical properties of liquid electrolyte systems for lithium ion batteries. Fluid Phase Equilibria, 2018, 473, 138-144.	1.4	1
89	Solid-liquid phase equilibria, excess volume and molar refraction deviation for carbonate ester systems with γ-Butyrolactone (GBL). Journal of Molecular Liquids, 2020, 314, 113627.	2.3	1
90	Solubility of Organic Systems Containing 1,4-Dioxan-2-one. Journal of Chemical & Engineering Data, 2006, 51, 1182-1184.	1.0	0

#	Article	IF	CITATIONS
91	Determination and correlation of phase behavior and physical properties for benign synthetic process of diphenylcarbonate. , 2013, , .		Ο
92	Solid-liquid equilibrium and kinematic viscosity of binary mixture of fatty acid alkyl esters. Korean Journal of Chemical Engineering, 2021, 38, 1006-1013.	1.2	0