William L Luyben

List of Publications by Citations

176 papers	5,645 citations	43 h-index	68 g-index
178 ext. papers	6,198 ext. citations	4 avg, IF	6.83 L-index

#	Paper	IF	Citations
176	Use of Hammerstein models in identification of nonlinear systems. *AICHE Journal*, **1991**, 37, 255-268	3.6	351
175	Tuning PI controllers for integrator/dead time processes. *Industrial & Engineering Chemistry Research*, **1992**, 31, 2625-2628	3.9	274
174	Comparison of Extractive Distillation and Pressure-Swing Distillation for Acetone/Methanol Separation. *Industrial & Engineering Chemistry Research*, **2008**, 47, 2696-2707	3.9	163
173	Comparison of extractive distillation and pressure-swing distillation for acetone/chloroform separation. *Computers and Chemical Engineering*, **2013**, 50, 1-7	4	154
172	Snowball effects in reactor/separator processes with recycle. *Industrial & Engineering Chemistry Research*, **1994**, 33, 299-305	3.9	150
171	Plantwide control design procedure. *AICHE Journal*, **1997**, 43, 3161-3174	3.6	149
170	New Control Structure for Divided-Wall Columns. *Industrial & Engineering Chemistry Research*, **2009**, 48, 6034-6049	3.9	143
169	**2006**,		131
168	Comparison of Alternative Control Structures for an Ideal Two-Product Reactive Distillation Column. *Industrial & Engineering Chemistry Research*, **2000**, 39, 3298-3307	3.9	122
167	Evaluation of criteria for selecting temperature control trays in distillation columns. *Journal of Process Control*, **2006**, 16, 115-134	3.9	117
166	Temperature Control of the BTX Divided-Wall Column. *Industrial & Engineering Chemistry Research*, **2010**, 49, 189-203	3.9	106
165	Control of the Heterogeneous Azeotropic n-Butanol/Water Distillation System. *Energy & Fuels*, **2008**, 22, 4249-4258	4.1	100
164	Tuning Proportional/Integral/Derivative Controllers for Integrator/Deadtime Processes. *Industrial & Engineering Chemistry Research*, **1996**, 35, 3480-3483	3.9	98
163	Design and Control of a Methanol Reactor/Column Process. *Industrial & Engineering Chemistry Research*, **2010**, 49, 6150-6163	3.9	91
162	Design and Control of a Fully Heat-Integrated Pressure-Swing Azeotropic Distillation System. *Industrial & Engineering Chemistry Research*, **2008**, 47, 2681-2695	3.9	87
161	Comparative control study of ideal and methyl acetate reactive distillation. *Chemical Engineering Science*, **2002**, 57, 5039-5050	4.4	83
160	Plantwide Dynamic Simulators in Chemical Processing and Control		76

159	Control of a multiunit heterogeneous azeotropic distillation process. *AICHE Journal*, **2006**, 52, 623-637	3.6	74
158	Getting More Information from Relay-Feedback Tests. *Industrial & Engineering Chemistry Research*, **2001**, 40, 4391-4402	3.9	74
157	Methane Conversion to Syngas for Gas-to-Liquids (GTL): Is Sustainable CO2 Reuse via Dry Methane Reforming (DMR) Cost Competitive with SMR and ATR Processes?. *ACS Sustainable Chemistry and Engineering*, **2015**, 3, 2100-2111	8.3	64
156	Design and control of a two-column azeotropic distillation system. *Industrial & Engineering Chemistry Process Design and Development*, **1985**, 24, 132-140		64
155	Plantwide control for TAME production using reactive distillation. *AICHE Journal*, **2004**, 50, 1462-1473	3.6	62
154	Control comparison of conventional and thermally coupled ternary extractive distillation processes. *Chemical Engineering Research and Design*, **2016**, 106, 253-262	5.5	59
153	Simple Dynamic Gasifier Model That Runs in Aspen Dynamics. *Industrial & Engineering Chemistry Research*, **2008**, 47, 7784-7792	3.9	59
152	Effect of Solvent on Controllability in Extractive Distillation. *Industrial & Engineering Chemistry Research*, **2008**, 47, 4425-4439	3.9	58
151	Quantitative Comparison of Reactive Distillation with Conventional Multiunit Reactor/Column/Recycle Systems for Different Chemical Equilibrium Constants. *Industrial & Engineering Chemistry Research*, **2004**, 43, 2493-2507	3.9	57
150	Distillation column pressure selection. *Separation and Purification Technology*, **2016**, 168, 62-67	8.3	56
149	Comparison of Pressure-Swing and Extractive-Distillation Methods for Methanol-Recovery Systems in the TAME Reactive-Distillation Process. *Industrial & Engineering Chemistry Research*, **2005**, 44, 5715-5725	3.9	55
148	Economic and Dynamic Impact of the Use of Excess Reactant in Reactive Distillation Systems. *Industrial & Engineering Chemistry Research*, **2000**, 39, 2935-2946	3.9	55
147	Comparison of Two Types of Two-Temperature Control Structures for Reactive Distillation Columns. *Industrial & Engineering Chemistry Research*, **2005**, 44, 4625-4640	3.9	54
146	Steady-State Energy Conservation Aspects of Distillation Column Control System Design. *Industrial & Engineering Chemistry Fundamentals*, **1975**, 14, 321-325		54
145	Plantwide control of an isopropyl alcohol dehydration process. *AICHE Journal*, **2006**, 52, 2290-2296	3.6	53
144	Nonlinear dynamic matrix control for high-purity distillation columns. *AICHE Journal*, **1988**, 34, 1287-1298	3.6	53
143	Design and Control of a Complex Process Involving Two Reaction Steps, Three Distillation Columns, and Two Recycle Streams. *Industrial & Engineering Chemistry Research*, **1995**, 34, 3885-3898	3.9	50
142	Design and Control of the Dry Methane Reforming Process. *Industrial & Engineering Chemistry Research*, **2014**, 53, 14423-14439	3.9	48

141	Design and Control of Conventional and Reactive Distillation Processes for the Production of Butyl Acetate. *Industrial & Engineering Chemistry Research*, **2004**, 43, 8014-8025	3.9	48
140	Control Study of Ethyl tert-Butyl Ether Reactive Distillation. *Industrial & Engineering Chemistry Research*, **2002**, 41, 3784-3796	3.9	48
139	Methanol/Trimethoxysilane Azeotrope Separation Using Pressure-Swing Distillation. *Industrial & Engineering Chemistry Research*, **2014**, 53, 5590-5597	3.9	47
138	Design and control of an olefin metathesis reactive distillation column. *Chemical Engineering Science*, **2002**, 57, 715-733	4.4	47
137	Control of a Column/Pervaporation Process for Separating the Ethanol/Water Azeotrope. *Industrial & Engineering Chemistry Research*, **2009**, 48, 3484-3495	3.9	46
136	Effect of Derivative Algorithm and Tuning Selection on the PID Control of Dead-Time Processes. *Industrial & Engineering Chemistry Research*, **2001**, 40, 3605-3611	3.9	46
135	Integrated Gasification Combined Cycle Dynamic Model: H2S Absorption/Stripping, Water Gas Shift Reactors, and CO2 Absorption/Stripping. *Industrial & Engineering Chemistry Research*, **2010**, 49, 4766-4781	3.9	44
134	Design and Control of the Cumene Process. *Industrial & Engineering Chemistry Research*, **2010**, 49, 719-734	3.9	43
133	Evaluation of a two-temperature control structure for a two-reactant/two-product type of reactive distillation column. *Chemical Engineering Science*, **2006**, 61, 4432-4450	4.4	42
132	Control of a Heat-Integrated Pressure-Swing Distillation Process for the Separation of a Maximum-Boiling Azeotrope. *Industrial & Engineering Chemistry Research*, **2014**, 53, 18042-18053	3.9	41
131	Control of ethylene glycol reactive distillation column. *AICHE Journal*, **2002**, 48, 905-908	3.6	41
130	Control of a triple-column pressure-swing distillation process. *Separation and Purification Technology*, **2017**, 174, 232-244	8.3	39
129	Tuning Proportional Integral Controllers for Processes with Both Inverse Response and Deadtime. *Industrial & Engineering Chemistry Research*, **2000**, 39, 973-976	3.9	39
128	Evaluation of Plant-Wide Control Structures by Steady-State Disturbance Sensitivity Analysis. *Industrial & Engineering Chemistry Research*, **1995**, 34, 2393-2405	3.9	36
127	Design and Control Degrees of Freedom. *Industrial & Engineering Chemistry Research*, **1996**, 35, 2204-2214	3.9	35
126	Design and control of a pressure-swing distillation process with vapor recompression. *Chemical Engineering and Processing: Process Intensification*, **2018**, 123, 174-184	3.7	34
125	Design and control of the ethyl benzene process. *AICHE Journal*, **2011**, 57, 655-670	3.6	34
124	Control of the Maximum-Boiling Acetone/Chloroform Azeotropic Distillation System. *Industrial & Engineering Chemistry Research*, **2008**, 47, 6140-6149	3.9	34

123	Dynamic Disadvantages of Intensification in Inherently Safer Process Design. *Industrial & Engineering Chemistry Research*, **2004**, 43, 384-396	3.9	34
122	Effect of Relative Volatility on the Quantitative Comparison of Reactive Distillation and Conventional Multi-unit Systems. *Industrial & Engineering Chemistry Research*, **2004**, 43, 3151-3162	3.9	33
121	Aspen Dynamics simulation of a middle-vessel batch distillation process. *Journal of Process Control*, **2015**, 33, 49-59	3.9	32
120	Control of an azeotropic DWC with vapor recompression. *Chemical Engineering and Processing: Process Intensification*, **2016**, 109, 114-124	3.7	31
119	Economic Optimum Design of the Heterogeneous Azeotropic Dehydration of Ethanol. *Industrial & Engineering Chemistry Research*, **2012**, 51, 16427-16432	3.9	30
118	Control of parallel dry methane and steam methane reforming processes for Fischer□Tropsch syngas. *Journal of Process Control*, **2016**, 39, 77-87	3.9	29
117	Economic Incentive for Intermittent Operation of Air Separation Plants with Variable Power Costs. *Industrial & Engineering Chemistry Research*, **2008**, 47, 1132-1139	3.9	29
116	Control of heat-integrated extractive distillation processes. *Computers and Chemical Engineering*, **2018**, 111, 267-277	4	28
115	Design and control of coupled reactor/column systems□Part 1. A binary coupled reactor/rectifier system. *Computers and Chemical Engineering*, **1997**, 21, 25-46	4	28
114	Steady-State and Dynamic Effects of Design Alternatives in Heat-Exchanger/Furnace/Reactor Processes. *Industrial & Engineering Chemistry Research*, **2000**, 39, 3335-3346	3.9	28
113	Control of vapor recompression distillation columns. *Industrial & Engineering Chemistry Research*, **1990**, 29, 59-71	3.9	28
112	Use of dynamic simulation for reactor safety analysis. *Computers and Chemical Engineering*, **2012**, 40, 97-109	4	27
111	Optimum Economic Design and Control of a Gas Permeation Membrane Coupled with the Hydrodealkylation (HDA) Process. *Industrial & Engineering Chemistry Research*, **2008**, 47, 1221-1237	3.9	27
110	Extensions of the Simultaneous Design of Gas-Phase Adiabatic Tubular Reactor Systems with Gas Recycle. *Industrial & Engineering Chemistry Research*, **2001**, 40, 635-647	3.9	26
109	Control of an Extractive Distillation System for the Separation of CO2 and Ethane in Enhanced Oil Recovery Processes. *Industrial & Engineering Chemistry Research*, **2013**, 52, 10780-10787	3.9	25
108	Design and Control of the Styrene Process. *Industrial & Engineering Chemistry Research*, **2011**, 50, 1231-1246	3.9	25
107	Capacity-Based Economic Approach for the Quantitative Assessment of Process Controllability during the Conceptual Design Stage. *Industrial & Engineering Chemistry Research*, **1995**, 34, 3907-3915	3.9	25
106	Analysis of Control Structures for Reaction/Separation/Recycle Processes with Second-Order Reactions. *Industrial & Engineering Chemistry Research*, **1996**, 35, 758-771	3.9	25

105	Improved plantwide control structure for extractive divided-wall columns with vapor recompression. *Chemical Engineering Research and Design*, **2017**, 123, 152-164	5.5	24
104	Vapor split manipulation in extractive divided-wall distillation columns. *Chemical Engineering and Processing: Process Intensification*, **2018**, 126, 132-140	3.7	23
103	Simple Regulatory Control of the Eastman Process. *Industrial & Engineering Chemistry Research*, **1996**, 35, 3280-3289	3.9	23
102	Estimating refrigeration costs at cryogenic temperatures. *Computers and Chemical Engineering*, **2017**, 103, 144-150	4	22
101	Plantwide Control of a Hybrid Integrated Gasification Combined Cycle/Methanol Plant. *Industrial & Engineering Chemistry Research*, **2011**, 50, 4579-4594	3.9	22
100	External versus Internal Open-Loop Unstable Processes. *Industrial & Engineering Chemistry Research*, **1998**, 37, 2713-2720	3.9	22
99	Design and Control of Gas-Phase Reactor/Recycle Processes with Reversible Exothermic Reactions. *Industrial & Engineering Chemistry Research*, **2000**, 39, 1529-1538	3.9	22
98	Quantitative Assessment of Controllability during the Design of a Ternary System with Two Recycle Streams. *Industrial & Engineering Chemistry Research*, **1996**, 35, 3470-3479	3.9	22
97	Comparison of flowsheets for THF/water separation using pressure-swing distillation. *Computers and Chemical Engineering*, **2018**, 115, 407-411	4	21
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94	Sensitivity of distillation relative gain arrays to steady-state gains. *Industrial & Engineering Chemistry Research*, **1987**, 26, 2076-2078	3.9	21
93	Two-Stripper/Decanter Flowsheet for Methanol Recovery in the TAME Reactive-Distillation Process. *Industrial & Engineering Chemistry Research*, **2009**, 48, 10532-10540	3.9	20
92	Optimum Design of a Column/Side Reactor Process. *Industrial & Engineering Chemistry Research*, **2007**, 46, 5175-5185	3.9	20
91	Design and Control of the Butyl Acetate Process*Industrial & Engineering Chemistry Research*, **2011**, 50, 1247-1263	3.9	19
90	Quantitative comparison of dynamic controllability between a reactive distillation column and a conventional multi-unit process. *Computers and Chemical Engineering*, **2008**, 32, 1456-1470	4	19
89	NGL Demethanizer Control. *Industrial & Engineering Chemistry Research*, **2013**, 52, 11626-11638	3.9	18
88	Series versus parallel reboilers in distillation columns. *Chemical Engineering Research and Design*, **2018**, 133, 294-302	5.5	17

87	Design and Control Comparison of Alternative Separation Methods for n-Heptane/Isobutanol. *Chemical Engineering and Technology*, **2017**, 40, 1895-1906	2	17
86	Design and Control of the Acetone Process via Dehydrogenation of 2-Propanol. *Industrial & Engineering Chemistry Research*, **2011**, 50, 1206-1218	3.9	17
85	Design and Control of a Methyl Acetate Process Using Carbonylation of Dimethyl Ether. *Industrial & Engineering Chemistry Research*, **2010**, 49, 12224-12241	3.9	16
84	Effect of the Chemical Equilibrium Constant on the Design of Reactive Distillation Columns. *Industrial & Engineering Chemistry Research*, **2004**, 43, 3666-3671	3.9	16
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82	Design and control of coupled reactor/column systemsPart 2. More complex coupled reactor/column systems. *Computers and Chemical Engineering*, **1997**, 21, 47-67	4	15
81	Effect of Feed Composition on the Selection of Control Structures for High-Purity Binary Distillation. *Industrial & Engineering Chemistry Research*, **2005**, 44, 7800-7813	3.9	15
80	Effect of Kinetic, Design, and Operating Parameters on Reactor Gain. *Industrial & Engineering Chemistry Research*, **2000**, 39, 2384-2391	3.9	15
79	New Control Structure for Feed-Effluent Heat Exchanger/Reactor Systems. *Industrial & Engineering Chemistry Research*, **2012**, 51, 8566-8574	3.9	14
78	Compressor Heuristics for Conceptual Process Design. *Industrial & Engineering Chemistry Research*, **2011**, 50, 13984-13989	3.9	14
77	Design and Control of Distillation Columns with Intermediate Reboilers. *Industrial & Engineering Chemistry Research*, **2004**, 43, 8244-8250	3.9	14
76	Design and Control of a Gas-Phase Adiabatic Tubular Reactor Process with Liquid Recycle. *Industrial & Engineering Chemistry Research*, **2001**, 40, 3762-3774	3.9	14
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74	Design and control of a cryogenic multi-stage compression refrigeration process. *Chemical Engineering Research and Design*, **2017**, 121, 360-367	5.5	13
73	Control of a Train of Distillation Columns for the Separation of Natural Gas Liquid. *Industrial & Engineering Chemistry Research*, **2013**, 52, 10741-10753	3.9	13
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68	Inherent Dynamic Problems with On-Demand Control Structures. *Industrial & Engineering Chemistry Research*, **1999**, 38, 2315-2329	3.9	12
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65	Design and Control of an Autorefrigerated Alkylation Process. *Industrial & Engineering Chemistry Research*, **2009**, 48, 11081-11093	3.9	10
64	Design and Control of a Modified Vinyl Acetate Monomer Process. *Industrial & Engineering Chemistry Research*, **2011**, 50, 10136-10147	3.9	9
63	Guides for the Selection of Control Structures for Ternary Distillation Columns. *Industrial & Engineering Chemistry Research*, **2005**, 44, 7113-7119	3.9	9
62	Dynamic Modeling and Control of a Hot-Gas Desulfurization Process with a Transport Desulfurizer. *Industrial & Engineering Chemistry Research*, **2001**, 40, 1157-1167	3.9	9
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60	Dynamic Model and Control Structures for a Hot-Gas Desulfurization Fluidized Process. *Industrial & Engineering Chemistry Research*, **1999**, 38, 4290-4298	3.9	9
59	Method for Assessing the Effect of Design Parameters on Controllability. *Industrial & Engineering Chemistry Research*, **1996**, 35, 3484-3497	3.9	9
58	Economic trade-offs in acrylic acid reactor design. *Computers and Chemical Engineering*, **2016**, 93, 118-127	4	8
57	Design of a Petroleum Preflash Column. *Energy & Fuels*, **2012**, 26, 1268-1274	4.1	8
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14	Heuristics for Plantwide Control **2012**, 97-119		1
13	Rebuttal to the Comments of Thomas J. McAvoy on Simple Regulatory Control of the Eastman Process *Industrial & Engineering Chemistry Research*, **1997**, 36, 1954-1954	3.9	1
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8	Simplified plantwide control structure for the diethyl oxalate process. *Computers and Chemical Engineering*, **2019**, 126, 451-464	4	0
7	Effect of Peak Temperature Limitations on the Design of Processes with Cooled Tubular Reactors. *International Journal of Chemical Reactor Engineering*, **2014**, 12, 191-203	1.2	0
6	Optimum vacuum distillation pressure. *Chemical Engineering and Processing: Process Intensification*, **2021**, 171, 108630	3.7	0
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1	Control structures for process piping systems. *Chemical Engineering Research and Design*, **2020**, 162, 28-37	3.9	