

# Victoria Eugenia Santos

## List of Publications by Year in descending order

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79  
papers

3,540  
citations

172457

29  
h-index

138484

58  
g-index

84  
all docs

84  
docs citations

84  
times ranked

3341  
citing authors

#	ARTICLE	IF	CITATIONS
1	Xanthan gum: production, recovery, and properties. <i>Biotechnology Advances</i> , 2000, 18, 549-579.	11.7	1,166
2	Oxygen uptake rate in microbial processes: An overview. <i>Biochemical Engineering Journal</i> , 2010, 49, 289-307.	3.6	344
3	Oxygen transfer and uptake rates during xanthan gum production. <i>Enzyme and Microbial Technology</i> , 2000, 27, 680-690.	3.2	151
4	Xanthan gum production under several operational conditions: molecular structure and rheological properties. <i>Enzyme and Microbial Technology</i> , 2000, 26, 282-291.	3.2	148
5	Production of a <i>Rhodococcus erythropolis</i> IGTS8 biocatalyst for DBT biodesulfurization: influence of operational conditions. <i>Biochemical Engineering Journal</i> , 2005, 22, 229-237.	3.6	67
6	Utilisation/upgrading of orange peel waste from a biological biorefinery perspective. <i>Applied Microbiology and Biotechnology</i> , 2019, 103, 5975-5991.	3.6	64
7	Metabolic and process engineering for biodesulfurization in Gram-negative bacteria. <i>Journal of Biotechnology</i> , 2017, 262, 47-55.	3.8	58
8	Production of a Biocatalyst of <i>Pseudomonas putida</i> CECT5279 for Dibenzothiophene (DBT) Biodesulfurization for Different Media Compositions. <i>Energy &amp; Fuels</i> , 2004, 18, 851-857.	5.1	55
9	Modeling the production of a <i>Rhodococcus erythropolis</i> IGTS8 biocatalyst for DBT biodesulfurization: Influence of media composition. <i>Enzyme and Microbial Technology</i> , 2005, 37, 157-166.	3.2	55
10	Fumaric Acid Production: A Biorefinery Perspective. <i>Fermentation</i> , 2018, 4, 33.	3.0	53
11	Production of a Biocatalyst of <i>Pseudomonas putida</i> CECT5279 for DBT Biodesulfurization: Influence of the Operational Conditions. <i>Energy &amp; Fuels</i> , 2005, 19, 775-782.	5.1	52
12	Kinetic Model for Anaerobic Digestion of Livestock Manure. <i>Enzyme and Microbial Technology</i> , 1999, 25, 55-60.	3.2	50
13	Orange peel waste upstream integrated processing to terpenes, phenolics, pectin and monosaccharides: Optimization approaches. <i>Industrial Crops and Products</i> , 2019, 134, 370-381.	5.2	49
14	Xanthan gum production: An unstructured kinetic model. <i>Enzyme and Microbial Technology</i> , 1995, 17, 206-217.	3.2	48
15	Nutritional study of <i>Xanthomonas campestris</i> in xanthan gum production by factorial design of experiments. <i>Enzyme and Microbial Technology</i> , 1992, 14, 991-996.	3.2	47
16	Oxygen-Uptake and Mass-Transfer Rates on the Growth of <i>Pseudomonas putida</i> CECT5279: Influence on Biodesulfurization (BDS) Capability. <i>Energy &amp; Fuels</i> , 2006, 20, 1565-1571.	5.1	47
17	Production of d-lactic acid by <i>Lactobacillus delbrueckii</i> ssp. <i>delbrueckii</i> from orange peel waste: techno-economical assessment of nitrogen sources. <i>Applied Microbiology and Biotechnology</i> , 2018, 102, 10511-10521.	3.6	44
18	On the use of resting <i>L. delbrueckii</i> spp. <i>delbrueckii</i> cells for D-lactic acid production from orange peel wastes hydrolysates. <i>Biochemical Engineering Journal</i> , 2019, 145, 162-169.	3.6	43

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19	Enhancement of the biodesulfurization capacity of <i>Pseudomonas putida</i> CECT5279 by co-substrate addition. <i>Process Biochemistry</i> , 2015, 50, 119-124.	3.7	42
20	Production of Oligosaccharides from Agrofood Wastes. <i>Fermentation</i> , 2020, 6, 31.	3.0	42
21	Biodesulfurisation of DBT with <i>Pseudomonas putida</i> CECT5279 by resting cells: Influence of cell growth time on reducing equivalent concentration and HpaC activity. <i>Biochemical Engineering Journal</i> , 2005, 26, 168-175.	3.6	40
22	The effect of hydrodynamic stress on the growth of <i>Xanthomonas campestris</i> cultures in a stirred and sparged tank bioreactor. <i>Bioprocess and Biosystems Engineering</i> , 2013, 36, 911-925.	3.4	39
23	Metabolic structured kinetic model for xanthan production. <i>Enzyme and Microbial Technology</i> , 1998, 23, 75-82.	3.2	37
24	Analysis of Dibenzothiophene Desulfurization in a Recombinant <i>Pseudomonas putida</i> Strain. <i>Applied and Environmental Microbiology</i> , 2009, 75, 875-877.	3.1	34
25	Oxygen transport rate on <i>Rhodococcus erythropolis</i> cultures: Effect on growth and BDS capability. <i>Chemical Engineering Science</i> , 2006, 61, 4595-4604.	3.8	33
26	1,3-Propanediol production from glycerol with a novel biocatalyst <i>Shimwellia blattae</i> ATCC 33430: Operational conditions and kinetics in batch cultivations. <i>Bioresource Technology</i> , 2016, 200, 830-837.	9.6	33
27	Biodesulfurization of Dibenzothiophene (DBT) Using <i>Pseudomonas putida</i> CECT 5279: A Biocatalyst Formulation Comparison. <i>Energy &amp; Fuels</i> , 2009, 23, 5491-5495.	5.1	32
28	Esterification of benzoic acid and glycerol to $\pm$ -monobenzoate glycerol in solventless media using an industrial free <i>Candida antarctica</i> lipase B. <i>Process Biochemistry</i> , 2012, 47, 243-250.	3.7	32
29	Study on the effects of several operational variables on the enzymatic batch saccharification of orange solid waste. <i>Bioresource Technology</i> , 2017, 245, 906-915.	9.6	32
30	Chemical structured kinetic model for xanthan production. <i>Enzyme and Microbial Technology</i> , 2004, 35, 284-292.	3.2	27
31	Mixtures of <i>Pseudomonas putida</i> CECT 5279 cells of different ages: Optimization as biodesulfurization catalyst. <i>Process Biochemistry</i> , 2011, 46, 1323-1328.	3.7	25
32	Novel biocatalysts for glycerol conversion into 2,3-butanediol. <i>Process Biochemistry</i> , 2016, 51, 740-748.	3.7	24
33	Biodesulfurization of dibenzothiophene by resting cells of <i>Pseudomonas putida</i> CECT5279: influence of the oxygen transfer rate in the scale-up from shaken flask to stirred tank reactor. <i>Journal of Chemical Technology and Biotechnology</i> , 2016, 91, 184-189.	3.2	24
34	Title is missing!. <i>World Journal of Microbiology and Biotechnology</i> , 1999, 15, 269-276.	3.6	23
35	Oxygen uptake rate measurements both by the dynamic method and during the process growth of <i>Rhodococcus erythropolis</i> IGTS8: Modelling and difference in results. <i>Biochemical Engineering Journal</i> , 2006, 32, 198-204.	3.6	22
36	Kinetic modeling of 1,3-propanediol production from raw glycerol by <i>Shimwellia blattae</i> : Influence of the initial substrate concentration. <i>Biochemical Engineering Journal</i> , 2017, 117, 57-65.	3.6	22

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37	d-lactic acid production from orange waste enzymatic hydrolysates with <i>L. delbrueckii</i> cells in growing and resting state. <i>Industrial Crops and Products</i> , 2020, 146, 112176.	5.2	22
38	Influence of oxygen transfer on <i>Pseudomonas putida</i> effects on growth rate and biodesulfurization capacity. <i>Bioprocess and Biosystems Engineering</i> , 2016, 39, 545-554.	3.4	21
39	Multi-feedstock lignocellulosic biorefineries based on biological processes: An overview. <i>Industrial Crops and Products</i> , 2021, 172, 114062.	5.2	20
40	Effect of fluid dynamic conditions on growth rate and biodesulfurization capacity of <i>Rhodococcus erythropolis</i> IGTS8. <i>Biochemical Engineering Journal</i> , 2015, 99, 138-146.	3.6	18
41	High 2,3-butanediol production from glycerol by <i>Raoultella terrigena</i> CECT 4519. <i>Bioprocess and Biosystems Engineering</i> , 2020, 43, 685-692.	3.4	18
42	Kinetic model for DBT desulfurization by resting whole cells of <i>Pseudomonas putida</i> CECT5279. <i>Biochemical Engineering Journal</i> , 2008, 39, 486-495.	3.6	17
43	1,3-Propanediol production by <i>Klebsiella oxytoca</i> NRRL-B199 from glycerol. Medium composition and operational conditions. <i>Biotechnology Reports (Amsterdam, Netherlands)</i> , 2015, 6, 100-107.	4.4	17
44	Production of D-lactic acid by <i>L. delbrueckii</i> growing on orange peel waste hydrolysates and model monosaccharide solutions: effects of pH and temperature on process kinetics. <i>Biomass Conversion and Biorefinery</i> , 2019, 9, 565-575.	4.6	17
45	Use of flow cytometry for growth structured kinetic model development. <i>Enzyme and Microbial Technology</i> , 2004, 34, 399-406.	3.2	16
46	Effect of fluid dynamic conditions on 2,3-butanediol production by <i>Raoultella terrigena</i> in SBTR: oxygen transfer and uptake rates. <i>Journal of Chemical Technology and Biotechnology</i> , 2017, 92, 1266-1275.	3.2	16
47	Fluid dynamic conditions and oxygen availability effects on microbial cultures in STBR: An overview. <i>Biochemical Engineering Journal</i> , 2020, 164, 107803.	3.6	16
48	Modulating redox metabolism to improve isobutanol production in <i>Shimwellia blattae</i> . <i>Biotechnology for Biofuels</i> , 2021, 14, 8.	6.2	15
49	Extended kinetic model for DBT desulfurization using <i>Pseudomonas Putida</i> CECT5279 in resting cells. <i>Biochemical Engineering Journal</i> , 2012, 66, 52-60.	3.6	14
50	Influence of oxygen transfer and uptake rates on dihydroxyacetone production from glycerol by <i>Gluconobacter oxydans</i> in resting cells operation. <i>Biochemical Engineering Journal</i> , 2019, 147, 20-28.	3.6	14
51	Intracellular compounds quantification by means of flow cytometry in bacteria: Application to xanthan production by <i>Xanthomonas campestris</i> . , 1998, 57, 87-94.		13
52	Simulation of xanthan gum production by a chemically structured kinetic model. <i>Mathematics and Computers in Simulation</i> , 1996, 42, 187-195.	4.4	12
53	Metabolic kinetic model for dibenzothiophene desulfurization through 4S pathway using intracellular compound concentrations. <i>Biochemical Engineering Journal</i> , 2017, 117, 89-96.	3.6	12
54	Isobutanol production by a recombinant biocatalyst <i>Shimwellia blattae</i> (p424IbPSO): Study of the operational conditions. <i>Biochemical Engineering Journal</i> , 2018, 133, 21-27.	3.6	11

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55	Dihydroxyacetone production from glycerol using <i>Gluconobacter oxydans</i> : Study of medium composition and operational conditions in shaken flasks. <i>Biotechnology Progress</i> , 2019, 35, e2803.	2.6	11
56	Kinetic Modeling of Dihydroxyacetone Production from Glycerol by <i>Gluconobacter oxydans</i> ATCC 621 Resting Cells: Effect of Fluid Dynamics Conditions. <i>Catalysts</i> , 2020, 10, 101.	3.5	11
57	Structured kinetic model for <i>Xanthomonas campestris</i> growth. <i>Enzyme and Microbial Technology</i> , 2004, 34, 583-594.	3.2	10
58	Immobilization-Stabilization of Î²-Glucosidase for Implementation of Intensified Hydrolysis of Cellobiose in Continuous Flow Reactors. <i>Catalysts</i> , 2022, 12, 80.	3.5	10
59	Optimization of the Enzymatic Saccharification Process of Milled Orange Wastes. <i>Fermentation</i> , 2017, 3, 37.	3.0	9
60	Effects of fluid-dynamic conditions in <i>Shimwellia blattae</i> (p424lbPSO) cultures in stirred tank bioreactors: Hydrodynamic stress and change of metabolic routes by oxygen availability. <i>Biochemical Engineering Journal</i> , 2019, 149, 107238.	3.6	9
61	Behavior of several <i>pseudomonas putida</i> strains growth under different agitation and oxygen supply conditions. <i>Biotechnology Progress</i> , 2018, 34, 900-909.	2.6	8
62	Resting cells isobutanol production by <i>Shimwellia blattae</i> (p424lbPSO): Influence of growth culture conditions. <i>Biotechnology Progress</i> , 2018, 34, 1073-1080.	2.6	8
63	Kinetic modelling of 2,3-butanediol production by <i>Raoultella terrigena</i> CECT 4519 resting cells: Effect of fluid dynamics conditions and initial glycerol concentration. <i>Biochemical Engineering Journal</i> , 2021, 176, 108185.	3.6	7
64	Title is missing!. <i>World Journal of Microbiology and Biotechnology</i> , 1999, 15, 309-316.	3.6	6
65	Desulfurization of dibenzothiophene using the 4S enzymatic route: Influence of operational conditions on initial reaction rates. <i>Biocatalysis and Biotransformation</i> , 2007, 25, 286-294.	2.0	6
66	Carbon flux distribution in the metabolism of <i>Shimwellia blattae</i> (p424lbPSO) for isobutanol production from glucose as function of oxygen availability. <i>Journal of Chemical Technology and Biotechnology</i> , 2019, 94, 850-858.	3.2	6
67	Production of Fumaric Acid by <i>Rhizopus arrhizus</i> NRRL 1526: A Simple Production Medium and the Kinetic Modelling of the Bioprocess. <i>Fermentation</i> , 2022, 8, 64.	3.0	6
68	Influence of fluid dynamic conditions on 1,3-ε-propanediol production from glycerol by <i>Shimwellia blattae</i> : carbon flux and cell response. <i>Journal of Chemical Technology and Biotechnology</i> , 2017, 92, 2050-2059.	3.2	5
69	Extraction of Antioxidants from Grape and Apple Pomace: Solvent Selection and Process Kinetics. <i>Applied Sciences (Switzerland)</i> , 2022, 12, 4901.	2.5	5
70	Production and Isolation of Xanthan Gum. <i>Methods in Biotechnology</i> , 1999, , 7-21.	0.2	4
71	Kinetic Modeling of the Isobutanol Production from Glucose Using <i>Shimwellia blattae</i> (p424lbPSO) Strain: Effect of Initial Substrate Concentration. <i>Industrial &amp; Engineering Chemistry Research</i> , 2019, 58, 1502-1512.	3.7	4
72	Kinetic Modelling of the Coproduction Process of Fumaric and Malic Acids by <i>Rhizopus arrhizus</i> NRRL 1526. <i>Processes</i> , 2020, 8, 188.	2.8	4

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73	On the succinic acid production from xylose by growing and resting cells of <i>Actinobacillus succinogenes</i> : a comparison. <i>Biomass Conversion and Biorefinery</i> , 2024, 14, 6533-6546.	4.6	4
74	Stirred Tank Bioreactors. , 2011, , 179-198.		3
75	Viability study of biofilm-former strains from paper industry by flow cytometry with application to kinetic models. <i>Biochemical Engineering Journal</i> , 2012, 68, 199-206.	3.6	3
76	Stirred Tank Bioreactors. , 2019, , 270-290.		1
77	Study of influence of oxygen transport conditions on oxygen uptake rate of <i>Pseudomonas putida</i> CECT5279 cultures. <i>New Biotechnology</i> , 2009, 25, S216.	4.4	0
78	Biodesulfurization of DBT using <i>Pseudomonas putida</i> CECT5279 resting cells: an improvement by using cosubstrates. <i>New Biotechnology</i> , 2009, 25, S156-S157.	4.4	0
79	The effect of ATP and NADH induced by acetic acid as co-substrate in the 4S route of DBT biodesulphurization by <i>Pseudomonas putida</i> CECT 5279 with mixture of resting whole cells with different age. <i>New Biotechnology</i> , 2012, 29, S51.	4.4	0