

# Jiri Hanika

## List of Publications by Year in descending order

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48  
papers

435  
citations

759233

12  
h-index

794594

19  
g-index

49  
all docs

49  
docs citations

49  
times ranked

361  
citing authors

#	ARTICLE	IF	CITATIONS
1	QUALITATIVE OBSERVATIONS OF HEAT AND MASS TRANSFER EFFECTS ON THE BEHAVIOUR OF A TRICKLE BED REACTOR. <i>Chemical Engineering Communications</i> , 1975, 2, 19-25.	2.6	44
2	Catalytic wet oxidation of substituted phenols in the trickle bed reactor. <i>Journal of Chemical Technology and Biotechnology</i> , 1998, 71, 262-266.	3.2	43
3	Alkylation and disproportionation of aromatic hydrocarbons over mesoporous molecular sieves. <i>Microporous and Mesoporous Materials</i> , 2001, 44-45, 499-507.	4.4	37
4	Periodic Operation of Three $\alpha$ Phase Catalytic Reactors. <i>Canadian Journal of Chemical Engineering</i> , 2004, 82, 1105-1142.	1.7	32
5	Partial wetting and forced reaction mixture transition in a model trickle-bed reactor. <i>Catalysis Today</i> , 1994, 20, 467-483.	4.4	20
6	Catalytic Effect of Active Carbon Black Chezacarb in Wet Oxidation of Phenol. <i>Collection of Czechoslovak Chemical Communications</i> , 1996, 61, 1010-1017.	1.0	19
7	Ethyl acetate synthesis by coupling of fixed-bed reactor and reactive distillation column Process integration aspects. <i>Chemical Engineering Journal</i> , 2009, 154, 236-240.	12.7	18
8	Dynamic modelling of glucose oxidation with palladium catalyst deactivation in multifunctional CSTR: Benefits of periodic operation. <i>Chemical Engineering Journal</i> , 2009, 150, 223-230.	12.7	17
9	Kinetics of hydrogenation of cyclic butadiene oligomers on palladium catalysts. Cyclooctadiene isomers. <i>Collection of Czechoslovak Chemical Communications</i> , 1981, 46, 1031-1038.	1.0	17
10	2-Methylpropylacetate synthesis in a system of equilibrium reactor and reactive distillation column. <i>Chemical Engineering Science</i> , 2001, 56, 365-370.	3.8	15
11	Relation between the distribution of platinum, its dispersion, and activity of catalysts prepared by impregnation of activated carbon with chloroplatinic acid solutions. <i>Collection of Czechoslovak Chemical Communications</i> , 1981, 46, 3270-3277.	1.0	14
12	Design, scale up and safe piloting of thymol hydrogenation and menthol racemisation. <i>Chemical Engineering Research and Design</i> , 2009, 87, 83-90.	5.6	13
13	Electrochemical Microreactor Design for Alkoxylation Reactions Experiments and Simulations. <i>Industrial &amp; Engineering Chemistry Research</i> , 2012, 51, 1515-1524.	3.7	13
14	Dynamic Behaviour of the Laboratory Trickle Bed Reactor. <i>The Chemical Engineering Journal</i> , 1981, 21, 109-114.	0.3	12
15	The effect of zeolite structure on the disproportionation of trimethylbenzenes to xylenes and tetramethylbenzenes. <i>Studies in Surface Science and Catalysis</i> , 1999, 125, 351-358.	1.5	12
16	HYDROGENATION OF 1,5-CYCLOOCTADIENE IN A TRICKLE BED REACTOR ACCOMPANIED BY PHASE TRANSITION. <i>Chemical Engineering Communications</i> , 1986, 40, 183-194.	2.6	10
17	Reactivation of a palladium catalyst during glucose oxidation by molecular oxygen. <i>Chemical Papers</i> , 2009, 63, .	2.2	9
18	Synthesis of (2E)-2-methyl-3-(4-{[4-(quinolin-2-ylmethoxy)phenyl]sulfanyl}phenyl)prop-2-enoic acid (VUFB 20609) and 2-methyl-3-(4-{[4-(quinolin-2-ylmethoxy)phenyl]sulfanyl}phenyl)propanoic acid (VUFB) Tj ETQq2.4 0 rgBT9Overlock 1		

#	ARTICLE	IF	CITATIONS
19	Purification of Phenolic Waste Waters by Catalytic Oxidation. Collection of Czechoslovak Chemical Communications, 1995, 60, 482-488.	1.0	9
20	Saturation of activated carbon with hexachloroplatinic acid. Collection of Czechoslovak Chemical Communications, 1981, 46, 1588-1593.	1.0	6
21	The effect of liquid flow distribution on catalytic hydrogenation of cyclohexene in an adiabatic trickle-bed reactor. Chemical Engineering Science, 1982, 37, 1283-1288.	3.8	6
22	Chapter 16 Application of Fixed-Bed Reactors to Liquid-Phase Hydrogenation. Studies in Surface Science and Catalysis, 1986, 27, 547-577.	1.5	6
23	Multi-functional trickle bed reactor for butylacetate synthesis. Catalysis Today, 2003, 79-80, 83-87.	4.4	6
24	The effect of preparation conditions of a platinum hydrogenation catalyst on its activity and on the dispersity of platinum crystallites. Collection of Czechoslovak Chemical Communications, 1979, 44, 2619-2623.	1.0	6
25	Dicyclopentadiene hydrogenation in trickle-bed reactor under forced periodic control. Chemical Papers, 2008, 62, .	2.2	5
26	Effect of internal diffusion on kinetics of liquid phase hydrogenation and disproportionation of the cyclohexene on palladium catalysts. Collection of Czechoslovak Chemical Communications, 1989, 54, 3003-3010.	1.0	5
27	Catalyst particle shape and dimension effects on gas oil hydrodesulphurization. Chemical Engineering Science, 1992, 47, 2739-2744.	3.8	4
28	Modelling of a trickle bed reactor with strong exothermal reaction. Catalysis Today, 1995, 24, 87-93.	4.4	4
29	Modelling of impregnation of $\gamma$ -alumina with cobalt and molybdenum salts. $\text{CoCl}_2\text{-(NH}_4\text{)}_2\text{MoO}_4\text{-}\gamma\text{-Al}_2\text{O}_3$ (aluminate type) system. Collection of Czechoslovak Chemical Communications, 1987, 52, 663-671.	1.0	4
30	Catalytic Oxidation of Substituted Phenols in a Trickle Bed Reactor. Collection of Czechoslovak Chemical Communications, 1997, 62, 866-874.	1.0	4
31	Experimentelle Untersuchungen zur periodischen Prozeßführung eines Trickle-bed-Reaktors. Chemie-Ingenieur-Technik, 1994, 66, 365-369.	0.8	3
32	A cell model of the isothermal trickle-bed reactor. Collection of Czechoslovak Chemical Communications, 1978, 43, 2111-2121.	1.0	3
33	Modelling of impregnation of $\gamma$ -alumina with cobalt and molybdenum salts. $\text{Co(NO}_3\text{)}_2\text{-(NH}_4\text{)}_2\text{MoO}_4\text{-}\gamma\text{-alumina}$ (chloride type) system. Collection of Czechoslovak Chemical Communications, 1987, 52, 672-677.	1.0	2
34	Catalyst Selection for Hydrogenation of 1,2-Dihydroacenaphthylene. Collection of Czechoslovak Chemical Communications, 1998, 63, 1945-1953.	1.0	2
35	Internal diffusion in the extruded catalyst particle with tetralobe cross section. Collection of Czechoslovak Chemical Communications, 1990, 55, 2161-2168.	1.0	1
36	Optimization of the High-Shear Wet Granulation Wetting Process Using Fuzzy Logic Modeling. Pharmaceutical Development and Technology, 2007, 12, 345-352.	2.4	1

#	ARTICLE	IF	CITATIONS
37	Relation between the conditions of preparation and the activity of supported platinum catalysts. Collection of Czechoslovak Chemical Communications, 1983, 48, 3079-3085.	1.0	1
38	Modelling of internal diffusion inside a catalyst particle with non-uniform radial activity profile for parallel reactions. Collection of Czechoslovak Chemical Communications, 1989, 54, 81-90.	1.0	1
39	Development of Cobalt-Molybdenum Hydrodesulfurization Catalysts. Collection of Czechoslovak Chemical Communications, 1992, 57, 2501-2508.	1.0	1
40	Mass Transfer Limited Wet Oxidation in Trickle-Bed Reactor. Collection of Czechoslovak Chemical Communications, 1998, 63, 1938-1944.	1.0	1
41	Mass Transfer in Catalyst Particles of Non-Traditional Shape. Collection of Czechoslovak Chemical Communications, 1996, 61, 564-573.	1.0	0
42	Effectiveness of Catalyst Extrudate of Tetralobed Cross Section Under Conditions of Influence of Internal Diffusion. Collection of Czechoslovak Chemical Communications, 1997, 62, 223-237.	1.0	0
43	Flow Interruption in Trickle Beds. , 2013, , 463-493.		0
44	New Directionsâ€”Research and Development Challenges. , 2013, , 679-689.		0
45	Partial oxidation of high-boiling hydrocarbon mixtures in the pilot unit. Chemical Papers, 2014, 68, .	2.2	0
46	Internal diffusion effect and hydrogenation selectivity of 1,5-cyclooctadiene. Collection of Czechoslovak Chemical Communications, 1980, 45, 1684-1691.	1.0	0
47	Determination of structure parameters of platinum hydrogenation catalysts and their supports. Collection of Czechoslovak Chemical Communications, 1987, 52, 2680-2686.	1.0	0
48	Preparation and Evaluation of Skeletal Cobalt-Molybdenum Hydrodesulfurization Catalysts. Collection of Czechoslovak Chemical Communications, 1995, 60, 568-575.	1.0	0