Christophe Coquelet

List of Publications by Year
in descending order

112	2,162	236612	288905
papers	citations	25 h-index	40 g-index

117	117	117	1318
all docs	docs citations	times ranked	citing authors

#	Article	IF	Citations
1	Vapourâ€“liquid equilibria in the carbon dioxideâ€“water system, measurement and modelling from 278.2 to 318.2K. Fluid Phase Equilibria, 2004, 226, 333-344.	1.4	299
2	Measurements and predictive models of high-pressure H2 solubility in brine (H2O+NaCl) for underground hydrogen storage application. International Journal of Hydrogen Energy, 2020, 45, 32206-32220.	3.8	99
3	Effect of impurities on thermophysical properties and phase behaviour of a CO2-rich system in CCS. International Journal of Greenhouse Gas Control, 2013, 19, 92-100.	2.3	77
4	Experimental measurements and correlation of vaporâ€“liquid equilibrium and critical data for the CO 2 Â+ÂR1234yf and CO 2 Â+ÂR1234ze(E) binary mixtures. International Journal of Refrigeration, 2014, 47, 141-152.	1.8	72
5	Investigation of a two stage Rankine cycle for electric power plants. Applied Energy, 2012, 100, 285-294.	5.1	63
6	Determination of critical properties of pure and multi-component mixtures using a â€œdynamicâ€“syntheticâ€•apparatus. Journal of Supercritical Fluids, 2010, 55, 545-553.	1.6	50
7	Solubility of hydrocarbons in water: Experimental measurements and modeling using a group contribution with association equation of state (GCA-EoS). Fluid Phase Equilibria, 2009, 275, 52-59.	1.4	49
8	Vaporâ^'Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa. Journal of Chemical & Engineering Data, 2003, 48, 317-323.	1.0	47
9	New Solubility Data of Hydrocarbons in Water and Modeling Concerning Vaporâ^'Liquidâ^'Liquid Binary Systems. Industrial & Engineering Chemistry Research, 2007, 46, 9257-9262.	1.8	47
10	Experimental Measurement of Vapor Pressures and Densities of Pure Hexafluoropropylene. Journal of Chemical & Engineering Data, 2010, 55, 2093-2099.	1.0	44
11	Acid gases partial pressures above a 50wt% aqueous methyldiethanolamine solution: Experimental work and modeling. Fluid Phase Equilibria, 2010, 289, 99-109.	1.4	40
12	Vapourâ€“liquid equilibrium data for the hydrogen sulphide (H2S)+carbon dioxide (CO2) system at temperatures from 258 to 313K. Fluid Phase Equilibria, 2013, 356, 223-228.	1.4	37
13	Fluid-phase-equilibrium prediction of fluorocompound-containing binary systems with the predictive E -PPR78 model. International Journal of Refrigeration, 2017, 73, 65-90.	1.8	36
14	Hydrocarbons â€“ water phase equilibria using the CPA equation of state with a group contribution method. Canadian Journal of Chemical Engineering, 2015, 93, 432-442.	0.9	35
15	Hydrate equilibrium data for the CO2Â+ÂN2 system with the use of tetra-n-butylammonium bromide (TBAB), cyclopentane (CP) and their mixture. Fluid Phase Equilibria, 2016, 408, 240-247.	1.4	33
16	Thermodynamic study of the CO2 â€“ H2O â€“ NaCl system: Measurements of CO2 solubility and modeling of phase equilibria using Soreide and Whitson, electrolyte CPA and SIT models. International Journal of Greenhouse Gas Control, 2019, 91, 102825.	2.3	32
17	Measurement of the Water Solubility in the Gas Phase of the Ethane + Water Binary System near Hydrate Forming Conditions. Journal of Chemical & Engineering Data, 2003, 48, 957-966.	1.0	31
18	Isothermal Vaporâ^'Liquid Equilibrium Data for the Hexafluoroethane (R116) + Propane System at Temperatures from (263 to 323) K. Journal of Chemical & Engineering Data, 2009, 54, 1292-1296.	1.0	30

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19	Isothermal Vaporâ"Liquid Equilibrium Data for the Perfluorobutane (R610) + Ethane System at Temperatures from (263 to 353) K. Journal of Chemical & Engineering Data, 2011, 56, 1918-1924.	1.0	29
20	Isothermal vaporâ€"liquid equilibrium data for the carbon dioxide (R744)+decafluorobutane (R610) system at temperatures from 263 to 353K. Fluid Phase Equilibria, 2011, 304, 44-51.	1.4	29
21	Isothermal vaporâ€"liquid equilibrium data for the trifluoromethane (R23)Â+ 2,3,3,3-tetrafluoroprop-1-ene (R1234yf) system at temperatures from 254 to 348ÂK. Fluid Phase Equilibria, 2016, 415, 158-165.	1.4	29
22	Thermodynamic study of binary systems containing sulphur dioxide: Measurements and molecular modelling. Fluid Phase Equilibria, 2011, 304, 21-34.	1.4	28
23	Experimental measurement and modelling of vapor-liquid equilibrium for 3,3,3- Trifluoropropene (R1243zf) and trans-1,3,3,3-Tetrafluoropropene (R1234ze(E)) binary system. International Journal of Refrigeration, 2020, 120, 137-149.	1.8	28
24	Vaporâ€"liquid equilibrium data for the hexafluoroethane+carbon dioxide system at temperatures from 253 to 297K and pressures up to 6.5MPa. Fluid Phase Equilibria, 2007, 258, 179-185.	1.4	27
25	Vaporâ€"liquid equilibrium in the n-butane+methanol system, measurement and modeling from 323.2 to 443.2K. Fluid Phase Equilibria, 2009, 277, 152-161.	1.4	26
26	Densities and derived thermophysical properties of the 0.9505ÂCO2+ 0.0495ÂH2S mixture from 273ÂK to 353ÂK and pressures up to 41ÂMPa. Fluid Phase Equilibria, 2016, 423, 156-171.	1.4	26
27	Vapourâ€"liquid equilibrium (VLE) for the systems furan+n-hexane and furan+toluene. Measurements, data treatment and modeling using molecular models. Fluid Phase Equilibria, 2013, 337, 234-245.	1.4	25
28	Liquid-liquid equilibria of waterÂ+ solutes (acetic acid/) Tj ETQq0 0 0 rgBT /Overlock 10 Tf 50 387 Td (acetol/furfural/guaiacol/methanol/p systems for pyrolysis oil fractionation. Fluid Phase Equilibria, 2018, 468, 49-57.	1.4	25
29	Vaporâ€"liquid equilibrium and molecular simulation data for carbon dioxide (CO2)â€¯+â€¯trans-1,3,3,3-tetrafluoroprop-1-ene (R-1234ze(E)) mixture at temperatures from 283.32 to 353.02â€¯K and pressures up to 7.6â€¯MPa. International Journal of Refrigeration, 2019, 98, 362-371.	1.8	25
30	Improvement of the PR-CPA equation of state for modelling of acid gases solubilities in aqueous alkanolamine solutions. Fluid Phase Equilibria, 2018, 471, 74-87.	1.4	23
31	Vaporâ€"liquid equilibrium data for the (hexafluoroethane +1,1,1,2-tetrafluoroethane) system at temperatures from 263 to 353K and pressures up to 4.16MPa. Fluid Phase Equilibria, 2008, 268, 68-73.	1.4	22
32	Experimental Measurement of Vapor Pressures and Densities at Saturation of Pure Hexafluoropropylene Oxide: Modeling Using a Crossover Equation of State. Industrial & Engineering Chemistry Research, 2011, 50, 4761-4768.	1.8	22
33	Volumetric properties of (piperidine+water) binary system: Measurements and modeling. Journal of Chemical Thermodynamics, 2008, 40, 47-53.	1.0	20
34	An equation of state for solidâ€"liquidâ€"vapor equilibrium applied to gas processing and natural gas liquefaction. Fluid Phase Equilibria, 2014, 362, 258-267.	1.4	20
35	Measurement of Henry's Law Constants and Infinite Dilution Activity Coefficients of Propyl Mercaptan, Butyl Mercaptan, and Dimethyl Sulfide in Methyldiethanolamine (1) + Water (2) with w1 = 0.50 Using a Gas Stripping Technique. Journal of Chemical & Engineering Data, 2005, 50, 2053-2057.	1.0	18
36	Prediction of thermodynamic properties of refrigerant fluids with a new three-parameter cubic equation of state. International Journal of Refrigeration, 2016, 69, 418-436.	1.8	18

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37	Volumetric Properties of Binary Mixtures of 1,2-Dichloroethane with Polyethers from (283.15 to 333.15) K and at Atmospheric Pressure. Journal of Chemical & Engineering Data, 2011, 56, 1629-1657.	1.0	17
38	A generalized Kiselev crossover approach applied to Soaveâ€“Redlichâ€“Kwong equation of state. Fluid Phase Equilibria, 2015, 401, 16-26.	1.4	17
39	Impact of impurities on CO 2 storage in saline aquifers: Modelling of gases solubility in water. International Journal of Greenhouse Gas Control, 2018, 68, 247-255.	2.3	17
40	Computational screening methodology identifies effective solvents for CO2 capture. Communications Chemistry, 2022, 5, .	2.0	17
41	Vaporâ€“Liquid Equilibrium Measurements and Modeling for the Ethane (R-170) + 1,1,2,3,3,3-Hexafluoro-1-propene (R-1216) Binary System. Journal of Chemical & Engineering Data, 2012, 57, 2947-2955.	1.0	16
42	Phase equilibrium data for the hydrogen sulphide + methane system at temperatures from 186 to 313 K and pressures up to about 14 MPa. Fluid Phase Equilibria, 2014, 383, 94-99.	1.4	16
43	Vapor pressures and vapor phase compositions of choline chloride urea and choline chloride ethylene glycol deep eutectic solvents from molecular simulation. Journal of Chemical Physics, 2021, 155, 114504.	1.2	16
44	Water Content of CO₂ -rich Mixtures: Measurements and Modeling using the Cubic-Plus-Association Equation of State. Journal of Natural Gas Engineering, 2016, 1, 85-97.	0.3	16
45	Chemoinformatics-Driven Design of New Physical Solvents for Selective CO₂ Absorption. Environmental Science & Technology, 2021, 55, 15542-15553.	4.6	16
46	Application of a new crossover treatment to a generalized cubic equation of state. Fluid Phase Equilibria, 2011, 302, 241-248.	1.4	15
47	Vapourâ€“liquid equilibrium of binary systems containing pentafluorochemicals from 363 to 413ÂK: Measurement and modelling with Pengâ€“Robinson and three SAFT-like equations of states. International Journal of Refrigeration, 2012, 35, 2297-2310.	1.8	15
48	Isothermal Vaporâ€“Liquid Equilibrium Measurements for the (R1234ze(E) + Ethane) System at Temperatures from 272.27 to 347.52 K. Journal of Chemical & Engineering Data, 2018, 63, 4185-4192.	1.0	15
49	Vapor-liquid equilibrium measurements for 5 binary mixtures involving HFO-1336mzz(E) at temperatures from 313 to 353ÂK and pressures up to 2.735ÂMPa. International Journal of Refrigeration, 2020, 114, 210-220.	1.8	15
50	High-Pressure Vaporâ€'Liquid Equilibria, Liquid Densities, and Excess Molar Volumes for the Carbon Dioxide + 2-Propanol System from (308.10 to 348.00) K. Journal of Chemical & Engineering Data, 2007, 52, 2032-2040.	1.0	14
51	Experimental determination of phase diagram and modeling: Application to refrigerant mixtures. International Journal of Refrigeration, 2009, 32, 1604-1614.	1.8	14
52	Equilibrium data and GC-PC SAFT predictions for furanic extraction. Fluid Phase Equilibria, 2016, 430, 57-66.	1.4	14
53	New Features of the Open Source Monte Carlo Software Brick-CFCMC: Thermodynamic Integration and Hybrid Trial Moves. Journal of Chemical Information and Modeling, 2021, 61, 3752-3757.	2.5	14
54	Experimental and modelling study of the densities of the hydrogen sulphideÂ+ methane mixtures at 253, 273 and 293ÂK and pressures up to 30ÂMPa. Fluid Phase Equilibria, 2016, 427, 371-383.	1.4	12

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55	Transport of CO2: Presentation of New Thermophysical Property Measurements and Phase Diagrams. Energy Procedia, 2017, 114, 6844-6859.	1.8	12
56	Hydrogen sulfide solubility in 50Âwt% and 70Âwt% aqueous methyldiethanolamine at temperatures from 283 to 393ÂK and total pressures from 500 to 10000ÂkPa. Fluid Phase Equilibria, 2020, 511, 112498.	1.4	12
57	Measurements and Modeling of High-Pressure O₂ and CO₂ Solubility in Brine (H₂O + NaCl) between 303 and 373 K and Pressures up to 36 MPa. Journal of Chemical & Engineering Data, 2021, 66, 609-620.	1.0	12
58	Vapourâ€“liquid equilibrium data for the hydrogen sulphide+n-heptane system at temperatures from 293.25 to 373.22K and pressures up to about 6.9MPa. Fluid Phase Equilibria, 2006, 249, 179-186.	1.4	11
59	Measurement through a Gas Stripping Technique of Henryâ€™s Law Constants and Infinite Dilution Activity Coefficients of Propyl Mercaptan, Butyl Mercaptan, and Dimethyl Sulfide in Methyldiethanolamine (1) + Water (2) with w₁ = 0.25 and 0.35. Journal of Chemical & Engineering Data, 2008, 53, 2540-2543.	1.0	11
60	Equilibrium Data for the Oxygen + Propane Binary System at Temperatures of (110.22, 120.13, 130.58, and) Tj ETQq0 0 0 rgBT /Overloc	1.0	11
61	Phase Equilibria of H₂S-Hydrocarbons (Propane, n-Butane, and n-Pentane) Binary Systems at Low Temperatures. Journal of Chemical & Engineering Data, 2012, 57, 1534-1543.	1.0	11
62	Isothermal Vaporâ€“Liquid Equilibrium Data and Modeling for the Ethane (R170) + Perfluoropropane (R218) System at Temperatures from (264 to 308) K. Journal of Chemical & Engineering Data, 2013, 58, 1316-1320.	1.0	11
63	Review of carbon dioxide capture and storage with relevance to the South African power sector. South African Journal of Science, 2014, 110, 12.	0.3	11
64	An improved staticâ€“analytic apparatus for vaporâ€“liquid equilibrium (PTxy) measurement using modified in-situ samplers. Fluid Phase Equilibria, 2016, 409, 425-433.	1.4	11
65	Experimental measurements and modelling of vapour-liquid equilibrium of 2,3,3,3-tetrafluoropropene (R-1234yf)â€¯+â€¯1,1,1,2,2-pentafluoropropane (R-245cb) system. International Journal of Refrigeration, 2019, 107, 315-325.	1.8	11
66	Phase Equilibria of Three Binary Mixtures: Methanethiol + Methane, Methanethiol + Nitrogen, and Methanethiol + Carbon Dioxide. Journal of Chemical & Engineering Data, 2012, 57, 896-901.	1.0	10
67	Vaporâ€“Liquidâ€“Liquid Equilibrium Measurements and Modeling of Ethanethiol + Methane + Water, 1-Propanethiol + Methane + Water and 1-Butanethiol + Methane + Water Ternary Systems at 303, 335, and 365 K and Pressure Up to 9 MPa. Industrial & Engineering Chemistry Research, 2013, 52, 14698-14705.	1.8	9
68	Effect of acid gases on the solubility of n-propylmercaptan in 50wt% methyl-diethanolamine aqueous solution. Chemical Engineering Research and Design, 2008, 86, 600-605.	2.7	8
69	Vaporâ€“Liquidâ€“Liquid Equilibrium Measurements and Modeling of the Methanethiol + Methane + Water Ternary System at 304, 334, and 364 K. Industrial & Engineering Chemistry Research, 2012, 51, 11561-11564.	1.8	8
70	Isothermal Vaporâ€“Liquid Equilibrium Data for the Hexafluoroethane (R116) + n-Butane System at Temperatures from 273 to 323 K. Journal of Chemical & Engineering Data, 2017, 62, 3483-3487.	1.0	8
71	Vaporâ€“Liquid Equilibria of the CH₄ + CO₂ + H₂S Ternary System with Two Different Global Compositions: Experiments and Modeling. Journal of Chemical & Engineering Data, 2020, 65, 1802-1813.	1.0	8
72	Critical properties and vapor-liquid equilibrium of two near-azeotropic mixtures containing HFOs. International Journal of Refrigeration, 2022, 138, 133-147.	1.8	8

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73	Measurement of Henryâ€™s Law constant and infinite dilution activity coefficient of isopropyl mercaptan and isobutyl mercaptan in (methyldiethanolamine (1) + water (2)) with w 1 = 0.25 and 0.50 at temperature of (298 to 348) K using inert gas stripping method. Journal of Chemical Thermodynamics, 2016, 93, 193-199.	1.0	7
74	Experimental determination of the critical loci for R-23+(n-propane or n-hexane) and R-116+n-propane binary mixtures. Journal of Chemical Thermodynamics, 2017, 108, 84-96.	1.0	7
75	Measurement and modelling of solid apparition temperature for the CO2 â€“ H2S â€“ CH4 ternary system. Fluid Phase Equilibria, 2020, 509, 112465.	1.4	7
76	Isothermal vaporâ€“liquid equilibrium data for the decafluorobutane (R3110)+1,1,1,3,3-pentafluorobutane (R365mfc) system at temperatures from 333K to 441K. Fluid Phase Equilibria, 2013, 354, 109-113.	1.4	6
77	Alkane solubilities in aqueous alkanolamine solutions with CPA EoS. Fluid Phase Equilibria, 2017, 434, 93-101.	1.4	6
78	Vapor Liquid Equilibrium Data for the Furanâ€“Toluene Binary System between 313.02 and 352.99 K. Journal of Chemical & Engineering Data, 2017, 62, 1168-1172.	1.0	6
79	Density and Excess Volume for Four Systems Involving Eugenol and Furan. Journal of Solution Chemistry, 2019, 48, 455-488.	0.6	6
80	Density data for carbon dioxide (CO2) +trans-1,3,3,3-tetrafluoroprop-1-ene (R-1234ze(E)) mixture at temperatures from 283.32 to 353.02K and pressures up to 10MPa. International Journal of Refrigeration, 2020, 120, 430-444.	1.8	6
81	â€œVaporâ€“liquidâ€•equilibrium measurements and modeling for the cyclohexane+cyclohexanol binary system. Fluid Phase Equilibria, 2010, 298, 33-37.	1.4	5
82	Isothermal Vaporâ€“Liquid Equilibrium (VLE) and Vaporâ€“Liquidâ€“Liquid Equilibrium (VLLE) Data for Two Binary Systems Containing Perfluorohexane with Carbon Monoxide or Hydrogen Sulfide at (293, 313,) Tj ETQq0 0 0 rgBT /Overlock 10 T	1.8	5
83	Apparent Henryâ€™s law constants of furan in different n -alkanes and alcohols at temperatures from 293 to 323 K. Journal of Environmental Chemical Engineering, 2017, 5, 1205-1209.	3.3	5
84	Simulations of the Impact of Co-injected Gases on CO2 Storage, the SIGARRR Project: Processes and Geochemical Approaches for Gas-water-Salt Interactions Modeling. Energy Procedia, 2017, 114, 3322-3334.	1.8	5
85	Density and Viscosity Measurements and Modeling of CO₂-Loaded and Unloaded Aqueous Solutions of Potassium Lysinate. Journal of Chemical & Engineering Data, 2021, 66, 4460-4475.	1.0	5
86	Experimental measurements and modelling of vapourâ^'liquid equilibria for four mixtures of 2,3,3,3â^'tetrafluoropropene (R1234yf) with 1,1,1,2â^'tetrafluoroethane (R134a) or 1,1â^'difluoroethane (R152a) or transâ^'1â^'chloroâ^'3,3,3â^'trifluoropropene (R1233zd(E)) or 2â^'chloroâ^'3,3,3â^'trifluoropropene (R1233xf). International Journal of Refrigeration, 2022, 140, 172-185.	1.8	5
87	Vaporâ€“liquid equilibrium data for the dimethyl ether (RE170)+decafluorobutane (R3-1-10) system at temperatures from 313.28 to 392.83K and pressures up to 4.9MPa. Fluid Phase Equilibria, 2012, 316, 141-146.	1.4	4
88	Prediction of methanol content in natural gas with the GC-PR-CPA model. Journal of Natural Gas Science and Engineering, 2015, 27, 745-750.	2.1	4
89	Densities and Excess Molar Volumes of the Ternary System (1,4-Dioxane + 2-Propanol +) Tj ETQq1 1 0.784314 rgBT /Overlock 10 Tf 5 Measurements and Prigogineâ€“Floryâ€“Patterson Modeling. Journal of Chemical & Engineering Data, 2019, 64, 5122-5131.	1.0	4
90	A New Semi-Empirical Model for Saturated Vapor Density of Pure Compounds. Journal of Chemical & Engineering Data, 2020, 65, 577-590.	1.0	4

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91	Volumetric Properties of Furan and 2-5-Dimethylfuran in Different Industrial Solvents at Temperatures from 278 to 343 K. Journal of Chemical & Engineering Data, 2021, 66, 2666-2680.	1.0	4
92	Experimental Density Data of Three Carbon Dioxide and Oxygen Binary Mixtures at Temperatures from 276 to 416 K and at Pressures up to 20 MPa. Journal of Chemical & Engineering Data, 2020, 65, 5313-5327.	1.0	4
93	Vaporâ€“Liquid Equilibrium (PTxy) Measurements and Modeling for the COâ€“C₂H₄ Binary System. Journal of Chemical & Engineering Data, 2012, 57, 2744-2749.	1.0	3
94	Phase Equilibrium Measurements and Modeling of 1-Propanethiol +1-Butanethiol + CH₄ in Methane Ternary System at 303, 336, and 368 K and Pressure Up to 9 MPa. Journal of Chemical & Engineering Data, 2016, 61, 41-44.	1.0	3
95	Phase Equilibrium of Three Binary Mixtures Containing NO and Components Present in Ambient Air. Journal of Chemical & Engineering Data, 2018, 63, 1021-1026.	1.0	3
96	Isothermal Vaporâ€“Liquid Equilibrium Data for Binary Mixtures of Hexafluoroethane (R116) + n-Pentane or n-Hexane at Two Temperatures, 288 and 296 K. Journal of Chemical & Engineering Data, 2018, 63, 1228-1233.	1.0	3
97	Vapour-liquid equilibria of n-butane and ethyl mercaptan: Experiments and modelling. Fluid Phase Equilibria, 2020, 504, 112335.	1.4	3
98	Experimental Determination of Thermophysical Properties of Working Fluids for ORC Applications. , 2020, , .		3
99	Vapour-Liquid Equilibria of Ethane and Ethanethiol: Experiments and Modelling. Journal of Natural Gas Engineering, 2019, 3, 96-108.	0.3	3
100	Vaporâ˜Liquid Equilibrium Measurements and Modeling for Cyclohexane + Cyclohexanone. Journal of Chemical & Engineering Data, 2010, 55, 4521-4524.	1.0	2
101	â€œVaporâ€“liquidâ€•equilibrium measurements and modeling for the cyclohexane+n-hexanoic acid binary system. Fluid Phase Equilibria, 2011, 309, 15-19.	1.4	2
102	Vaporâ€“Liquid Equilibrium Data for the Carbon Dioxide (CO2) + 1,1,1,3,3-Pentafluorobutane (R365mfc) System at Temperatures from 283.15 to 337.15 K. Journal of Chemical & Engineering Data, 2018, , .	1.0	2
103	A New Thermodynamic Correlation for Apparent Henry's Law Constants, Infinite Dilution Activity Coefficient and Solubility of Mercaptans in Pure Water. Journal of Natural Gas Engineering, 2017, 2, 148-170.	0.3	2
104	Vapour-Liquid Equilibrium Study for the Carbon Dioxide and Hydrogen Sulphide in Deionized Water and NaCl Aqueous Solution at Temperature from 373.15 to 423.15 K. , 2021, , .		1
105	Improvements for a fully consistent description of the new semi-empirical vapor density model for pure compounds. Fluid Phase Equilibria, 2022, 556, 113374.	1.4	1
106	Modelling of solubility of mercaptans in water at low concentrations. AIP Conference Proceedings, 2019, , .	0.3	0
107	Vapor Liquid Equilibrium Data for the Hydrogen Chlorideâ€“Chlorobenzene Binary System at 353.16, 403.16, and 453.25 K. Journal of Chemical & Engineering Data, 2020, 65, 3652-3657.	1.0	0
108	Hydrate Stability of Carbon Dioxide + Oxygen Binary Mixture (CO₂ + O₂) in Pure Water: Measurements and Modeling. Journal of Chemical & Engineering Data, 2021, 66, 767-779.	1.0	0

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109	Role of Computational Variables on the Performances of COSMO-SAC Model: A Combined Theoretical and Experimental Investigation. Industrial & Engineering Chemistry Research, 2021, 60, 2314-2325.	1.8	0
110	Effect of Methane, CO2, and H2S on the Solubility of Methyl and Ethyl Mercaptans in a 25 wt % Methyldiethanolamine Aqueous Solution at 333 and 365 K. Journal of Chemical & Engineering Data, 0, , .	1.0	0
111	Volumetric Properties of Binary Mixtures of 1,2-Dichloroethane with Ethers from 278.15â€“333.15 K and at Atmospheric Pressure. Journal of Chemical & Engineering Data, 2022, 67, 554-567.	1.0	0
112	Isothermal P, x, y data for the nitrogenÂ+Âcarbon monoxide system at five temperatures from 100 to 130ÂK and pressures up to 3.4ÂMPa. Fluid Phase Equilibria, 2022, 559, 113476.	1.4	0