Petri K Uusi-Kyyny

List of Publications by Year in Descending Order

110 papers	1,194 citations	19 h-index	26 g-index
118 ext. papers	1,307 ext. citations	2.9 avg, IF	4.29 L-index

#	Paper	IF	Citations
110	Application-Related Consideration of the Thermal Stability of [mTBDH][OAc] Compared to Amidine-Based Ionic Liquids in the Presence of Various Amounts of Water. *Industrial & Engineering Chemistry Research*, **2022**, 61, 259-268	3.9	2
109	Liquid–liquid equilibria in binary and ternary systems of phenol + hydrocarbons (n-dodecane or n-hexadecane) and water + phenol + hydrocarbons (n-dodecane or n-hexadecane) at temperatures between 298K and 353K. *Fluid Phase Equilibria*, **2022**, 556, 113402	2.5	0
108	A Volumetric Pitzer Model for Aqueous Solutions of Zinc Sulfate up to Near-Saturation Concentrations at Temperatures from 293.15 to 393.15 K and Pressures up to 10 MPa. *Journal of Chemical & Engineering Data*, **2021**, 66, 58-64	2.8	2
107	Vapor- liquid equilibrium for the n-dodecane + phenol and n-hexadecane + phenol systems at 523 K and 573 K. *Fluid Phase Equilibria*, **2021**, 537, 112991	2.5	3
106	Volumetric Properties of Aqueous Solutions of Zinc Sulfate at Temperatures from 298.15 to 393.15 K and Pressures up to 10 MPa. *Journal of Chemical & Engineering Data*, **2021**, 66, 45-57	2.8	2
105	Vapor–Liquid Equilibrium of Ionic Liquid 7-Methyl-1,5,7-triazabicyclo[4.4.0]dec-5-enium Acetate and Its Mixtures with Water. *Journal of Chemical & Engineering Data*, **2020**, 65, 2405-2421	2.8	7
104	Application of GaInSn Liquid Metal Alloy Replacing Mercury in a Phase Equilibrium Cell: Vapor Pressures of Toluene, Hexylbenzene, and 2-Ethylnaphthalene. *Journal of Chemical & Engineering Data*, **2020**, 65, 3270-3276	2.8	2
103	Hydrodeoxygenation Model Compounds: Heptalactone and Nonalactone: Density from 293 to 473 K and H2 Solubility from 479 to 582 K. *Journal of Chemical & Engineering Data*, **2020**, 65, 2764-2773	2.8	2
102	Hydrodeoxygenation of Propylphenols on a Niobia-Supported Platinum Catalyst: Ortho, Meta, Para Isomerism, Reaction Conditions, and Phase Equilibria. *Advanced Sustainable Systems*, **2020**, 4, 1900140	5.9	
101	Densities, Viscosities, and Thermal Conductivities of the Ionic Liquid 7-Methyl-1,5,7-triazabicyclo[4.4.0]dec-5-enium Acetate and Its Mixtures with Water. *International Journal of Thermophysics*, **2020**, 41, 1	2.1	3
100	Physical Properties of 7-Methyl-1,5,7-triazabicyclo[4.4.0]dec-5-ene (mTBD). *International Journal of Thermophysics*, **2019**, 40, 1	2.1	10
99	110th Anniversary: Critical Properties and High Temperature Vapor Pressures for Furan, 2-Methylfuran, 2-Methoxy-2-methylpropane, 2-Ethoxy-2-methylbutane, n-Hexane, and Ethanol and Bubble Points of Mixtures with a New Apparatus. *Industrial & Engineering Chemistry Research*, **2019**, 58, 22350-22362	3.9	3
98	Vapor Pressures, Densities, and PC-SAFT Parameters for 11 Bio-compounds. *International Journal of Thermophysics*, **2019**, 40, 1	2.1	19
97	Temperature and Pressure Dependence of Density of a Shale Oil and Derived Thermodynamic Properties. *Industrial & Engineering Chemistry Research*, **2018**, 57, 5128-5135	3.9	3
96	Isobaric Vapor–Liquid Equilibrium of Furfural + γ-Valerolactone at 30 kPa and Isothermal Liquid–Liquid Equilibrium of Carbon Dioxide + γ-Valerolactone + Water at 298 K. *Journal of Chemical & Engineering Data*, **2018**,	2.8	5
95	Chemical Recovery of γ-Valerolactone/Water Biorefinery. *Industrial & Engineering Chemistry Research*, **2018**, 57, 15147-15158	3.9	20
94	Hydrogen solubility in furfural and 2-propanol: Experiments and modeling. *Journal of Chemical Thermodynamics*, **2017**, 112, 1-6	2.9	19

93	Micro-scale piloting of a process for production of 2-methoxy-2,4,4-trimethylpentane. *Chemical Engineering and Processing: Process Intensification*, **2017**, 122, 143-154	3.7	2
92	Study of CO2 Absorption into Phase Change Solvents MAPA and DEEA. *Journal of Chemical & Engineering Data*, **2017**, 62, 2261-2271	2.8	2
91	Hydrogen Solubility of Shale Oil Containing Polar Phenolic Compounds. *Industrial & Engineering Chemistry Research*, **2017**, 56, 8738-8747	3.9	7
90	6. Process intensification for microdistillation using the equipment miniaturization approach **2017**, 213-240		
89	Solubility of carbon monoxide in bio-oil compounds. *Journal of Chemical Thermodynamics*, **2017**, 105, 296-311	2.9	4
88	Hydrogen solubility measurements of analyzed tall oil fractions and a solubility model. *Journal of Chemical Thermodynamics*, **2017**, 105, 15-20	2.9	6
87	Experimental and Theoretical Thermodynamic Study of Distillable Ionic Liquid 1,5-Diazabicyclo[4.3.0]non-5-enium Acetate. *Industrial & Engineering Chemistry Research*, **2016**, 55, 10445-10454	3.9	24
86	Development of a unique modular distillation column using 3D printing. *Chemical Engineering and Processing: Process Intensification*, **2016**, 109, 136-148	3.7	19
85	Prototyping a calorimeter mixing cell with direct metal laser sintering. *Chemical Engineering Research and Design*, **2016**, 108, 146-151	5.5	4
84	Dew points of pure DBN and DBU and vapor□quid equilibria of water+DBN and water+DBU systems for cellulose solvent recycling. *Fluid Phase Equilibria*, **2016**, 408, 79-87	2.5	10
83	Feasibility of thermal separation in recycling of the distillable ionic liquid [DBNH][OAc] in cellulose fiber production. *Chemical Engineering Research and Design*, **2016**, 114, 287-298	5.5	19
82	Design of Equilibrium Cells for Phase Equilibria and PVT Measurements in Large Ranges of Temperatures and Pressures. I. Vapor□liquid□liquid Equilibria. *Journal of Chemical & Engineering Data*, **2016**, 61, 2700-2711	2.8	5
81	Solubility of hydrogen in bio-oil compounds. *Journal of Chemical Thermodynamics*, **2016**, 102, 406-412	2.9	12
80	Measurements and modeling for the density of 2-methoxy-2,4,4-trimethylpentane, HE for (methanol + 2-methoxy-2,4,4-trimethylpentane), LLE for (water + 2-methoxy-2,4,4-trimethylpentane) and LLE for (water + methanol + 2-methoxy-2,4,4-trimethylpentane). *Journal of Chemical Thermodynamics*, **2015**, 91, 313-320	2.9	1
79	A comprehensive study of CO 2 solubility in aqueous 2-HEAA and MEA + 2-HEAA solutions □ Measurements and modeling. *International Journal of Greenhouse Gas Control*, **2015**, 42, 296-306	4.2	3
78	Measurement of activity coefficient at infinite dilution for some bio-oil components in water and mass transfer study of bubbles in the dilutor. *Fluid Phase Equilibria*, **2015**, 392, 1-11	2.5	5
77	Measurements and modeling of LLE and HE for (methanol + 2,4,4-trimethyl-1-pentene), and LLE for (water + methanol + 2,4,4-trimethyl-1-pentene). *Journal of Chemical Thermodynamics*, **2015**, 85, 120-128	2.9	9
76	Isothermal vapor□quid equilibrium and excess molar enthalpies of the binary mixtures furfural+methyl isobutyl ketone, +2-butanol and +2-methyl-2-butanol. *Fluid Phase Equilibria*, **2014**, 372, 85-99	2.5	9

75	Hydrogen solubility in heavy oil systems: Experiments and modeling. *Fuel*, **2014**, 137, 393-404	7.1	27
74	A modified continuous flow apparatus for gas solubility measurements at high pressure and temperature with camera system. *Fluid Phase Equilibria*, **2014**, 382, 150-157	2.5	8
73	Measurements and modeling of CO2 solubility in 1,8-diazabicyclo-[5.4.0]-undec-7-ene glycerol solutions. *Fluid Phase Equilibria*, **2014**, 374, 25-36	2.5	25
72	Comparative study: Absorption enthalpy of carbon dioxide into aqueous diisopropanolamine and monoethanolamine solutions and densities of the carbonated amine solutions. *Fluid Phase Equilibria*, **2014**, 376, 85-95	2.5	7
71	Distillable Protic Ionic Liquid 2-(Hydroxy)ethylammonium Acetate (2-HEAA): Density, Vapor Pressure, Vapor liquid Equilibrium, and Solid liquid Equilibrium. *Industrial & Engineering Chemistry Research*, **2014**, 53, 19322-19330	3.9	10
70	A comprehensive thermodynamic study of heat stable acetic acid salt of monoethanolamine. *International Journal of Greenhouse Gas Control*, **2014**, 22, 313-324	4.2	16
69	A novel continuous flow apparatus with a video camera system for high pressure phase equilibrium measurements. *Fluid Phase Equilibria*, **2013**, 356, 291-300	2.5	6
68	Measurements of H2S solubility in aqueous diisopropanolamine solutions and vapour pressure of diisopropanolamine. *Fluid Phase Equilibria*, **2013**, 338, 164-171	2.5	17
67	The use of microplants in process development Case study of etherification of 2-ethoxy-2-methylbutane. *Chemical Engineering and Processing: Process Intensification*, **2013**, 74, 75-82	3.7	5
66	Control of reflux and reboil flow rates for milli and micro distillation. *Chemical Engineering Research and Design*, **2013**, 91, 753-760	5.5	10
65	Vapor liquid equilibrium measurements of dimethylsulfide, +ethanol, +dimethylether, +methylacetate with a static total pressure method. *Fluid Phase Equilibria*, **2013**, 355, 34-39	2.5	1
64	Vapor liquid Equilibrium, Excess Molar Enthalpies, and Excess Molar Volumes of Binary Mixtures Containing 2-Ethoxy-2-methylpropane or 2-Ethoxy-2-methylbutane and Acetonitrile or Propanenitrile. *Journal of Chemical & Engineering Data*, **2013**, 58, 943-950	2.8	5
63	Vapor liquid Equilibrium at 350 K, Excess Molar Enthalpies at 298 K, and Excess Molar Volumes at 298 K of Binary Mixtures Containing Ethyl Acetate, Butyl Acetate, and 2-Butanol. *Journal of Chemical & Engineering Data*, **2013**, 58, 1011-1019	2.8	10
62	Vapor liquid Equilibrium for Methoxymethane + Thiophene, + Diethylsulfide, + 2-Methyl-2-propanethiol and 1-Hexene, + 1-Propanethiol. *Journal of Chemical & Engineering Data*, **2013**, 58, 956-963	2.8	9
61	FEASIBILITY OF LASER MATERIAL PROCESSING IN THE DESIGN AND MANUFACTURE OF SMALL SCALE DEVICES. *Mechanika*, **2013**, 19,	1.5	2
60	Vapor liquid Equilibria, Excess Enthalpy, and Excess Volume of Binary Mixtures Containing an Alcohol (1-Butanol, 2-Butanol, or 2-Methyl-2-butanol) and 2-Ethoxy-2-methylbutane. *Journal of Chemical & Engineering Data*, **2012**, 57, 3502-3509	2.8	8
59	Microscale distillation. *Russian Journal of General Chemistry*, **2012**, 82, 2079-2087	0.7	10
58	Vapor liquid Equilibrium, Excess Molar Enthalpies, and Excess Molar Volumes of Binary Mixtures Containing Methyl Isobutyl Ketone (MIBK) and 2-Butanol, tert-Pentanol, or 2-Ethyl-1-hexanol. *Journal of Chemical & Engineering Data*, **2012**, 57, 3092-3101	2.8	14

57	The Henry's law constant of N2O and CO2 in aqueous binary and ternary amine solutions (MEA, DEA, DIPA, MDEA, and AMP). *Fluid Phase Equilibria*, **2011**, 311, 59-66	2.5	51
56	Finding a suitable thermodynamic model and phase equilibria for hydrodeoxygenation reactions of methyl heptanoate. *Fuel*, **2011**, 90, 3315-3322	7.1	12
55	Application of Microreactors in the Dehydrogenation of Isobutane. *Topics in Catalysis*, **2011**, 54, 1206-1212	2.3	3
54	Isobaric vapor–liquid equilibrium for binary systems containing benzothiophene. *Fluid Phase Equilibria*, **2011**, 307, 180-184	2.5	7
53	Vapor–liquid Equilibrium for Methoxymethane + Methyl Formate, Methoxymethane + Hexane, and Methyl Formate + Methanol. *Journal of Chemical & Engineering Data*, **2011**, 56, 2634-2640	2.8	10
52	Vapor–liquid Equilibrium for Dimethyl Disulfide + Butane, + trans-But-2-ene, + 2-Methylpropane, + 2-Methylpropene, + Ethanol, and 2-Ethoxy-2-methylpropane. *Journal of Chemical & Engineering Data*, **2011**, 56, 2501-2510	2.8	6
51	Vapor–liquid Equilibrium for Thiophene + Butane, + trans-But-2-ene, + 2-Methylpropane, and + 2-Methylpropene. *Journal of Chemical & Engineering Data*, **2011**, 56, 614-621	2.8	3
50	Phase equilibria on binary systems containing diethyl sulfide. *Fluid Phase Equilibria*, **2011**, 301, 200-205	2.5	6
49	Isothermal Binary Vapor–liquid Equilibrium for 2-Methylpropane and n-Butane with 1,2-Ethanedithiol and 2-Methyl-2-propanethiol. *Journal of Chemical & Engineering Data*, **2010**, 55, 291-296	2.8	5
48	Vapor–liquid equilibrium for the binary systems tetrahydrothiophene + toluene and tetrahydrothiophene + o-xylene at 368.15 K and 383.15 K. *Fluid Phase Equilibria*, **2010**, 296, 4-8	2.5	4
47	Solubility of carbon dioxide in aqueous solutions of diisopropanolamine and methyldiethanolamine. *Fluid Phase Equilibria*, **2010**, 293, 101-109	2.5	27
46	Phase equilibrium measurements for systems containing propanenitrile with tert-butyl ethyl ether and C4-hydrocarbons. *Fluid Phase Equilibria*, **2010**, 299, 148-160	2.5	5
45	Vapour–liquid equilibrium for the systems diethyl sulphide+1-butene, +cis-2-butene, +2-methylpropane, +2-methylpropene, +n-butane, +trans-2-butene. *Fluid Phase Equilibria*, **2010**, 291, 180-187	2.5	6
44	Phase equilibria on five binary systems containing 1-butanethiol and 3-methylthiophene in hydrocarbons. *Fluid Phase Equilibria*, **2010**, 293, 157-163	2.5	7
43	Vapor–liquid equilibrium for binary system of tetrahydrothiophene+2,2,4-trimethylpentane and tetrahydrothiophene+2,4,4-trimethyl-1-pentene at 358.15 and 368.15K. *Fluid Phase Equilibria*, **2010**, 296, 159-163	2.5	
42	Thermodynamics of aqueous solutions of methyldiethanolamine and diisopropanolamine. *Fluid Phase Equilibria*, **2010**, 299, 51-59	2.5	16
41	Phase equilibria of binary systems of 3-methylthiophene with four different hydrocarbons. *Fluid Phase Equilibria*, **2010**, 288, 155-160	2.5	10
40	Reply to the letter to the editor by J. Gmehling and A. Jacob about the paper "Phase equilibria on four binary systems containing 3-methylthiophene" [Fluid Phase Equilib. 279 (2009) 81–86]. *Fluid Phase Equilibria*, **2010**, 292, 117	2.5	

39	Phase equilibria for systems containing dimethyl disulfide and diethyl disulfide with hydrocarbons at 368.15K. *Fluid Phase Equilibria*, **2010**, 293, 175-181	2.5	5
38	Infinite dilution activity coefficient and vapour liquid equilibrium measurements for dimethylsulphide and tetrahydrothiophene with hydrocarbons. *Fluid Phase Equilibria*, **2010**, 295, 17-25	2.5	3
37	Phase equilibria on four binary systems containing 3-methylthiophene. *Fluid Phase Equilibria*, **2009**, 279, 81-86	2.5	20
36	Novel micro-distillation column for process development. *Chemical Engineering Research and Design* , **2009**, 87, 705-710	5.5	32
35	Vapor–liquid Equilibrium for Tetrahydrothiophene + n-Butane, + trans-2-Butene, + 2-Methylpropane, and + 2-Methylpropene. *Journal of Chemical & Engineering Data*, **2009**, 54, 1311-1317	2.8	5
34	Vapor–liquid Equilibrium for Butane + Methanol, + Ethanol, + 2-Propanol, + 2-Butanol, and + 2-Methyl-2-Propanol (TBA) at 323 K. *Journal of Chemical & Engineering Data*, **2008**, 53, 83-88	2.8	13
33	Vapor–liquid Equilibrium for the cis-2-Butene + Methanol, + 2-Propanol, + 2-Butanol, + 2-Methyl-2-propanol Systems at 364.5 K. *Journal of Chemical & Engineering Data*, **2008**, 53, 1539-1544	2.8	5
32	Vapor–liquid Equilibrium for the Systems trans-2-Butene + Methanol, + 1-Propanol, + 2-Propanol, + 2-Butanol, and + 2-Methyl-2-propanol at 364.5 K. *Journal of Chemical & Engineering Data*, **2008**, 53, 607-612	2.8	6
31	Vapor–liquid Equilibrium for 1-Butene + Methanol, + 1-Propanol, + 2-Propanol, + 2-Butanol, and 2-Methyl-2-propanol (TBA) at 364.5 K. *Journal of Chemical & Engineering Data*, **2008**, 53, 1829-1835	2.8	6
30	Vapor–liquid Equilibrium for 1-Butanol + 1-Butene at (318.4 and 364.5) K and Vapor–liquid Equilibrium of 1-Butanol + 2-Methylpropane, + n-Butane and 1-Butene + 2-Methylpropane at 318.4 K. *Journal of Chemical & Engineering Data*, **2008**, 53, 2454-2461	2.8	2
29	Vapor–liquid Equilibrium for the Systems 2-Methylpropane + Methanol, + 2-Propanol, + 2-Butanol, and + 2-Methyl-2-propanol at 364.5 K. *Journal of Chemical & Engineering Data*, **2008**, 53, 913-918	2.8	3
28	Isothermal binary vapour–liquid equilibrium for butanes and butenes with dimethylsulphide. *Fluid Phase Equilibria*, **2008**, 266, 143-153	2.5	10
27	Vapor–liquid Equilibrium for Binary System of Diethyl Sulfide + n-Heptane and Diethyl Sulfide + 2,2,4-Trimethylpentane at (363.15 and 353.15) K. *Journal of Chemical & Engineering Data*, **2007**, 52, 192-198	2.8	12
26	Vapor–liquid Equilibrium for Binary System of Diethyl Sulfide + n-Hexane at (338.15 and 323.15) K and Diethyl Sulfide + 1-Hexene at (333.15 and 323.15) K. *Journal of Chemical & Engineering Data*, **2007**, 52, 571-576	2.8	5
25	Vapour–liquid equilibrium for the systems butane+methanol, +2-propanol, +1-butanol, +2-butanol, +2-methyl-2-propanol at 364.5K. *Fluid Phase Equilibria*, **2007**, 254, 49-59	2.5	18
24	Vapor–liquid equilibrium for binary system of diethyl sulfide+cyclohexane at 353.15 and 343.15K and diethyl sulfide+2-ethoxy-2-methylpropane at 343.15 and 333.15K. *Fluid Phase Equilibria*, **2007**, 252, 130-136	2.5	12
23	Vapor–liquid equilibrium for binary system of thiophene+2,2,4-trimethylpentane at 343.15 and 353.15K and thiophene+2-ethoxy-2-methylpropane at 333.15 and 343.15K. *Fluid Phase Equilibria*, **2007**, 261, 115-121	2.5	27
22	Practical Methodology for Distillation Design using a Miniplant. *Chemical Engineering and Technology*, **2006**, 29, 104-112	2	3

21	Isothermal Vapor Liquid Equilibrium for 2-Methylpropene + Methanol, + 1-Propanol, + 2-Propanol, + 2-Butanol, and + 2-Methyl-2-propanol Binary Systems at 364.5 K. *Journal of Chemical & Engineering Data*, **2006**, 51, 562-568	2.8	24
20	Vapor Liquid Equilibrium for Six Binary Systems of C4-Hydrocarbons + 2-Propanone. *Journal of Chemical & Engineering Data*, **2006**, 51, 554-561	2.8	15
19	Vapor–liquid Equilibrium for Binary System of 1-Propanethiol, Thiophene, and Diethyl Sulfide with Toluene at 90.03 kPa. *Journal of Chemical & Engineering Data*, **2006**, 51, 1372-1376	2.8	27
18	Vapor–liquid Equilibrium for Binary System of Thiophene + n-Hexane at (338.15 and 323.15) K and Thiophene + 1-Hexene at (333.15 and 323.15) K. *Journal of Chemical & Engineering Data*, **2006**, 51, 2203-2208	2.8	44
17	Infinite dilution activity coefficient measurements by inert gas stripping method. *Fluid Phase Equilibria*, **2006**, 243, 126-132	2.5	16
16	Vapour–liquid equilibrium for the ethyl ethanoate+1-butene, +cis-2-butene, +trans-2-butene, +2-methylpropene, +n-butane and +2-methylpropane. *Fluid Phase Equilibria*, **2005**, 230, 21-28	2.5	6
15	Vapour–liquid equilibrium for the 2-methylpropane+methanol, +ethanol, +2-propanol, +2-butanol and +2-methyl-2-propanol systems at 313.15K. *Fluid Phase Equilibria*, **2005**, 232, 90-99	2.5	16
14	Isothermal vapour–liquid equilibrium measurements for six binary systems of C4 hydrocarbons + 2-propanone. *Fluid Phase Equilibria*, **2004**, 226, 173-181	2.5	16
13	Isothermal Vapor Liquid Equilibrium for Binary 2-Methylpropene + Methanol to Butanol Systems. *Journal of Chemical & Engineering Data*, **2004**, 49, 787-794	2.8	20
12	Isobaric Vapor Liquid Equilibrium for 2,3-Dimethyl-2-butene + Methanol, + Ethanol, + 2-Propanol, or + 2-Butanol at Atmospheric Pressure. *Journal of Chemical & Engineering Data*, **2004**, 49, 251-255	2.8	10
11	Vapor–liquid Equilibrium for the trans-2-Butene + Methanol, + Ethanol, + 2-Propanol, + 2-Butanol, and + 2-Methyl-2-propanol Systems at 332 K. *Journal of Chemical & Engineering Data*, **2004**, 49, 1168-1174	2.8	15
10	Vapor–liquid Equilibrium for 1-Propanol + 1-Butene, + cis-2-Butene, + 2-Methyl-propene, + trans-2-Butene, + n-Butane, and + 2-Methyl-propane. *Journal of Chemical & Engineering Data*, **2004**, 49, 1628-1634	2.8	14
9	Vapour–liquid equilibrium for the 1-butene + methanol, + ethanol, + 2-propanol, + 2-butanol and + 2-methyl-2-propanol systems at 326 K. *Fluid Phase Equilibria*, **2003**, 206, 237-252	2.5	32
8	Vapour–liquid equilibrium for the cis-2-butene + methanol, + ethanol, + 2-propanol, + 2-butanol and + 2-methyl-2-propanol systems at 337 K. *Fluid Phase Equilibria*, **2003**, 212, 129-141	2.5	18
7	Vapor Liquid Equilibria for Ethanol + 2,4,4-Trimethyl-1-pentene and 2-Propanol + 2,4,4-Trimethyl-1-pentene at 101 kPa. *Journal of Chemical & Engineering Data*, **2003**, 48, 280-285	2.8	3
6	Vapor liquid equilibrium for the binary systems 2-methylpentane + 2-butanol at 329.2 K and n-hexane + 2-butanol at 329.2 and 363.2 K with a static apparatus. *Fluid Phase Equilibria*, **2002**, 201, 343-358	2.5	43
5	Vapor–liquid Equilibrium for the 2-Methylpentane + 2-Methyl-2-propanol and + 2-Butanol Systems at 329 K. *Journal of Chemical & Engineering Data*, **2002**, 47, 371-375	2.8	7
4	Vapor–liquid Equilibrium for the Binary Systems of Methanol + 2,4,4-Trimethyl-1-pentene at 331 K and 101 kPa and Methanol + 2-Methoxy-2,4,4-trimethylpentane at 333 K. *Journal of Chemical & Engineering Data*, **2001**, 46, 1244-1248	2.8	17

3	Vapor Liquid Equilibrium for the Binary Systems of 2-Methyl-2-propanol + 2,4,4-Trimethyl-1-pentene at 333 K and 348 K and 2-Butanol + 2,4,4-Trimethyl-1-pentene at 360 K. *Journal of Chemical & Engineering Data*, **2001**, 46, 686-691	2.8	11
2	Vapor Liquid Equilibrium for the Binary Systems of 3-Methylpentane + 2-Methyl-2-propanol at 331 K and + 2-Butanol at 331 K. *Journal of Chemical & Engineering Data*, **2001**, 46, 754-758	2.8	35
1	Vapor Liquid Equilibrium for the Binary Systems of 2-Methylpropane + Ethanenitrile and 2-Methylpropene + Ethanenitrile at 358 K. *Journal of Chemical & Engineering Data*, **2000**, 45, 116-119	2.8	4