Petri K Uusi-Kyyny

List of Publications by Year
in descending order

111	1,409	361045	500791
papers	citations	20 h-index	28 g-index

118	118	118	968
all docs	docs citations	times ranked	citing authors

#	Article	IF	Citations
1	The Henry's law constant of N2O and CO2 in aqueous binary and ternary amine solutions (MEA, DEA,) Tj ETQq1 1 0.784314 rgBT /Ov	1.4	62
2	Vaporâ˜'Liquid Equilibrium for Binary System of Thiophene +n-Hexane at (338.15 and 323.15) K and Thiophene + 1-Hexene at (333.15 and 323.15) K. Journal of Chemical & Engineering Data, 2006, 51, 2203-2208.	1.0	46
3	Vapor liquid equilibrium for the binary systems 2-methylpentane + 2-butanol at 329.2 K and n-hexane + 2-butanol at 329.2 and 363.2 K with a static apparatus. Fluid Phase Equilibria, 2002, 201, 343-358.	1.4	43
4	Novel micro-distillation column for process development. Chemical Engineering Research and Design, 2009, 87, 705-710.	2.7	42
5	Vaporâ˜'Liquid Equilibrium for the Binary Systems of 3-Methylpentane + 2-Methyl-2-propanol at 331 K and + 2-Butanol at 331 K. Journal of Chemical & Engineering Data, 2001, 46, 754-758.	1.0	36
6	Hydrogen solubility in heavy oil systems: Experiments and modeling. Fuel, 2014, 137, 393-404.	3.4	36
7	Experimental and Theoretical Thermodynamic Study of Distillable Ionic Liquid 1,5-Diazabicyclo[4.3.0]non-5-enium Acetate. Industrial & Engineering Chemistry Research, 2016, 55, 10445-10454.	1.8	35
8	Vapor Pressures, Densities, and PC-SAFT Parameters for 11 Bio-compounds. International Journal of Thermophysics, 2019, 40, 1.	1.0	34
9	Solubility of carbon dioxide in aqueous solutions of diisopropanolamine and methyldiethanolamine. Fluid Phase Equilibria, 2010, 293, 101-109.	1.4	33
10	Vapourâ€"liquid equilibrium for the 1-butene + methanol, + ethanol, + 2-propanol, + 2-butanol and + 2-methyl-2-propanol systems at 326 K. Fluid Phase Equilibria, 2003, 206, 237-252.	1.4	32
11	Measurements and modeling of CO2 solubility in 1,8-diazabicyclo-[5.4.0]-undec-7-eneâ€"Glycerol solutions. Fluid Phase Equilibria, 2014, 374, 25-36.	1.4	31
12	Vaporâ˜'Liquid Equilibrium for Binary System of 1-Propanethiol, Thiophene, and Diethyl Sulfide with Toluene at 90.03 kPa. Journal of Chemical & Engineering Data, 2006, 51, 1372-1376.	1.0	28
13	Chemical Recovery of Î³-Valerolactone/Water Biorefinery. Industrial & Engineering Chemistry Research, 2018, 57, 15147-15158.	1.8	28
14	Vaporâ€"liquid equilibrium for binary system of thiophene+2,2,4-trimethylpentane at 343.15 and 353.15K and thiophene+2-ethoxy-2-methylpropane at 333.15 and 343.15K. Fluid Phase Equilibria, 2007, 261, 115-121.	1.4	27
15	Development of a unique modular distillation column using 3D printing. Chemical Engineering and Processing: Process Intensification, 2016, 109, 136-148.	1.8	27
16	Isothermal Vapor Liquid Equilibrium for 2-Methylpropene + Methanol, + 1-Propanol, + 2-Propanol, + 2-Butanol, and + 2-Methyl-2-propanol Binary Systems at 364.5 K. Journal of Chemical & Engineering Data, 2006, 51, 562-568.	1.0	24
17	Feasibility of thermal separation in recycling of the distillable ionic liquid [DBNH][OAc] in cellulose fiber production. Chemical Engineering Research and Design, 2016, 114, 287-298.	2.7	23
18	Phase equilibria on four binary systems containing 3-methylthiophene. Fluid Phase Equilibria, 2009, 279, 81-86.	1.4	22

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19	Thermodynamics of aqueous solutions of methyldiethanolamine and diisopropanolamine. Fluid Phase Equilibria, 2010, 299, 51-59.	1.4	22
20	Hydrogen solubility in furfural and 2-propanol: Experiments and modeling. Journal of Chemical Thermodynamics, 2017, 112, 1-6.	1.0	21
21	Isothermal Vapor Liquid Equilibrium for Binary 2-Methylpropene + Methanol to Butanol Systems. Journal of Chemical & Engineering Data, 2004, 49, 787-794.	1.0	20
22	Vapourâ€“liquid equilibrium for the cis-2-butene + methanol, + ethanol, + 2-propanol, + 2-butanol and + 2-methyl-2-propanol systems at 337 K. Fluid Phase Equilibria, 2003, 212, 129-141.	1.4	18
23	Infinite dilution activity coefficient measurements by inert gas stripping method. Fluid Phase Equilibria, 2006, 243, 126-132.	1.4	18
24	Vapourâ€“liquid equilibrium for the systems butane+methanol, +2-propanol, +1-butanol, +2-butanol, +2-methyl-2-propanol at 364.5K. Fluid Phase Equilibria, 2007, 254, 49-59.	1.4	18
25	Vaporâ^'Liquid Equilibrium for the Binary Systems of Methanol + 2,4,4-Trimethyl-1-pentene at 331 K and 101 kPa and Methanol + 2-Methoxy-2,4,4-trimethylpentane at 333 K. Journal of Chemical & Engineering Data, 2001, 46, 1244-1248.	1.0	17
26	Isothermal vapourâ€“liquid equilibrium measurements for six binary systems of C4 hydrocarbons + 2-propanone. Fluid Phase Equilibria, 2004, 226, 173-181.	1.4	17
27	Vapourâ€“liquid equilibrium for the 2-methylpropane+methanol, +ethanol, +2-propanol, +2-butanol and +2-methyl-2-propanol systems at 313.15K. Fluid Phase Equilibria, 2005, 232, 90-99.	1.4	17
28	Measurements of H2S solubility in aqueous diisopropanolamine solutions and vapour pressure of diisopropanolamine. Fluid Phase Equilibria, 2013, 338, 164-171.	1.4	17
29	Vaporâ^'Liquid Equilibrium for 1-Propanol + 1-Butene, +cis-2-Butene, + 2-Methyl-propene, +trans-2-Butene, +n-Butane, and + 2-Methyl-propane. Journal of Chemical & Engineering Data, 2004, 49, 1628-1634.	1.0	16
30	Control of reflux and reboil flow rates for milli and micro distillation. Chemical Engineering Research and Design, 2013, 91, 753-760.	2.7	16
31	A comprehensive thermodynamic study of heat stable acetic acid salt of monoethanolamine. International Journal of Greenhouse Gas Control, 2014, 22, 313-324.	2.3	16
32	Solubility of hydrogen in bio-oil compounds. Journal of Chemical Thermodynamics, 2016, 102, 406-412.	1.0	16
33	Vaporâ^'Liquid Equilibrium for thetrans-2-Butene + Methanol, + Ethanol, + 2-Propanol, + 2-Butanol, and + 2-Methyl-2-propanol Systems at 332 K. Journal of Chemical & Engineering Data, 2004, 49, 1168-1174.	1.0	15
34	Vapor Liquid Equilibrium for Six Binary Systems of C4-Hydrocarbons + 2-Propanone. Journal of Chemical & Engineering Data, 2006, 51, 554-561.	1.0	15
35	Distillable Protic Ionic Liquid 2-(Hydroxy)ethylammonium Acetate (2-HEAA): Density, Vapor Pressure, Vaporâ€“Liquid Equilibrium, and Solidâ€“Liquid Equilibrium. Industrial & Engineering Chemistry Research, 2014, 53, 19322-19330.	1.8	15
36	Vaporâ€“Liquid Equilibrium for Butane + Methanol, + Ethanol, + 2-Propanol, + 2-Butanol, and + 2-Methyl-2-Propanol (TBA) at 323 K. Journal of Chemical & Engineering Data, 2008, 53, 83-88.	1.0	14

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37	Vaporâ€“Liquid Equilibrium, Excess Molar Enthalpies, and Excess Molar Volumes of Binary Mixtures Containing Methyl Isobutyl Ketone (MIBK) and 2-Butanol, tert-Pentanol, or 2-Ethyl-1-hexanol. Journal of Chemical & Engineering Data, 2012, 57, 3092-3101.	1.0	14
38	Vaporâ^'Liquid Equilibrium for Binary System of Diethyl Sulfide +n-Heptane and Diethyl Sulfide + 2,2,4-Trimethylpentane at (363.15 and 353.15) K. Journal of Chemical & Engineering Data, 2007, 52, 192-198.	1.0	13
39	Finding a suitable thermodynamic model and phase equilibria for hydrodeoxygenation reactions of methyl heptanoate. Fuel, 2011, 90, 3315-3322.	3.4	13
40	Vaporâ€“liquid equilibrium for binary system of diethyl sulfide+cyclohexane at 353.15 and 343.15K and diethyl sulfide+2-ethoxy-2-methylpropane at 343.15 and 333.15K. Fluid Phase Equilibria, 2007, 252, 130-136.	1.4	12
41	Isothermal binary vapourâ€“liquid equilibrium for butanes and butenes with dimethylsulphide. Fluid Phase Equilibria, 2008, 266, 143-153.	1.4	12
42	Phase equilibria of binary systems of 3-methylthiophene with four different hydrocarbons. Fluid Phase Equilibria, 2010, 288, 155-160.	1.4	12
43	Microscale distillation. Russian Journal of General Chemistry, 2012, 82, 2079-2087.	0.3	12
44	Measurements and modeling of LLE and HE for (methanol + 2,4,4-trimethyl-1-pentene), and LLE for (water + methanol + 2,4,4-trimethyl-1-pentene). Journal of Chemical Thermodynamics, 2015, 85, 120-128.	1.0	12
45	Hydrogen Solubility of Shale Oil Containing Polar Phenolic Compounds. Industrial & Engineering Chemistry Research, 2017, 56, 8738-8747.	1.8	12
46	Physical Properties of 7-Methyl-1,5,7-triazabicyclo[4.4.0]dec-5-ene (mTBD). International Journal of Thermophysics, 2019, 40, 1.	1.0	12
47	Vapor Liquid Equilibrium for the Binary Systems of 2-Methyl-2-propanol + 2,4,4-Trimethyl-1-pentene at 333 K and 348 K and 2-Butanol + 2,4,4-Trimethyl-1-pentene at 360 K. Journal of Chemical & Engineering Data, 2001, 46, 686-691.	1.0	11
48	Isobaric Vapor Liquid Equilibrium for 2,3-Dimethyl-2-butene + Methanol, + Ethanol, + 2-Propanol, or + 2-Butanol at Atmospheric Pressure. Journal of Chemical & Engineering Data, 2004, 49, 251-255.	1.0	11
49	Vaporâ^'Liquid Equilibrium for Methoxymethane + Methyl Formate, Methoxymethane + Hexane, and Methyl Formate + Methanol. Journal of Chemical & Engineering Data, 2011, 56, 2634-2640.	1.0	11
50	Vaporâ€“Liquid Equilibrium for Methoxymethane + Thiophene, + Diethylsulfide, + 2-Methyl-2-propanethiol and 1-Hexene, + 1-Propanethiol. Journal of Chemical & Engineering Data, 2013, 58, 956-963.	1.0	11
51	Isothermal vaporâ€“liquid equilibrium and excess molar enthalpies of the binary mixtures furfural+methyl isobutyl ketone, +2-butanol and +2-methyl-2-butanol. Fluid Phase Equilibria, 2014, 372, 85-99.	1.4	11
52	Vaporâ€“Liquid Equilibrium at 350 K, Excess Molar Enthalpies at 298 K, and Excess Molar Volumes at 298 K of Binary Mixtures Containing Ethyl Acetate, Butyl Acetate, and 2-Butanol. Journal of Chemical & Engineering Data, 2013, 58, 1011-1019.	1.0	10
53	A modified continuous flow apparatus for gas solubility measurements at high pressure and temperature with camera system. Fluid Phase Equilibria, 2014, 382, 150-157.	1.4	10
54	Dew points of pure DBN and DBU and vaporâ€“liquid equilibria of water+DBN and water+DBU systems for cellulose solvent recycling. Fluid Phase Equilibria, 2016, 408, 79-87.	1.4	10

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55	Application-Related Consideration of the Thermal Stability of [mTBDH][OAc] Compared to Amidine-Based Ionic Liquids in the Presence of Various Amounts of Water. Industrial & Engineering Chemistry Research, 2022, 61, 259-268.	1.8	10
56	Phase equilibria on five binary systems containing 1-butanethiol and 3-methylthiophene in hydrocarbons. Fluid Phase Equilibria, 2010, 293, 157-163.	1.4	9
57	Comparative study: Absorption enthalpy of carbon dioxide into aqueous diisopropanolamine and monoethanolamine solutions and densities of the carbonated amine solutions. Fluid Phase Equilibria, 2014, 376, 85-95.	1.4	9
58	Hydrogen solubility measurements of analyzed tall oil fractions and a solubility model. Journal of Chemical Thermodynamics, 2017, 105, 15-20.	1.0	9
59	Vaporâ^'Liquid Equilibrium for Dimethyl Disulfide + Butane, +trans-But-2-ene, + 2-Methylpropane, + 2-Methylpropene, + Ethanol, and 2-Ethoxy-2-methylpropane. Journal of Chemical & Engineering Data, 2011, 56, 2501-2510.	1.0	8
60	Isobaric vaporâ€"liquid equilibrium for binary systems containing benzothiophene. Fluid Phase Equilibria, 2011, 307, 180-184.	1.4	8
61	Phase equilibria on binary systems containing diethyl sulfide. Fluid Phase Equilibria, 2011, 301, 200-205.	1.4	8
62	Vaporâ€"Liquid Equilibria, Excess Enthalpy, and Excess Volume of Binary Mixtures Containing an Alcohol (1-Butanol, 2-Butanol, or 2-Methyl-2-butanol) and 2-Ethoxy-2-methylbutane. Journal of Chemical & Engineering Data, 2012, 57, 3502-3509.	1.0	8
63	Vaporâ€"Liquid Equilibrium of Ionic Liquid 7-Methyl-1,5,7-triazabicyclo[4.4.0]dec-5-enium Acetate and Its Mixtures with Water. Journal of Chemical & Engineering Data, 2020, 65, 2405-2421.	1.0	8
64	Vapor- liquid equilibrium for the n-dodecaneÂ+Âphenol and n-hexadecaneÂ+Âphenol systems at 523 K and 573 K. Fluid Phase Equilibria, 2021, 537, 112991.	1.4	8
65	Vaporâ^'Liquid Equilibrium for the 2-Methylpentane + 2-Methyl-2-propanol and + 2-Butanol Systems at 329 K. Journal of Chemical & Engineering Data, 2002, 47, 371-375.	1.0	7
66	Vapourâ€"liquid equilibrium for the ethyl ethanoate+1-butene, +cis-2-butene, +trans-2-butene, +2-methylpropene, +n-butane and +2-methylpropane. Fluid Phase Equilibria, 2005, 230, 21-28.	1.4	7
67	Vaporâ^'Liquid Equilibrium for 1-Butene + Methanol, + 1-Propanol, + 2-Propanol, + 2-Butanol, and 2-Methyl-2-propanol (TBA) at 364.5 K. Journal of Chemical & Engineering Data, 2008, 53, 1829-1835.	1.0	7
68	Vapourâ€"liquid equilibrium for the systems diethyl sulphide+1-butene, +cis-2-butene, +2-methylpropane, +2-methylpropene, +n-butane, +trans-2-butene. Fluid Phase Equilibria, 2010, 291, 180-187.	1.4	7
69	Isothermal Binary Vaporâ^'Liquid Equilibrium for 2-Methylpropane and n-Butane with 1,2-Ethanedithiol and 2-Methyl-2-propanethiol. Journal of Chemical & Engineering Data, 2010, 55, 291-296.	1.0	7
70	A novel continuous flow apparatus with a video camera system for high pressure phase equilibrium measurements. Fluid Phase Equilibria, 2013, 356, 291-300.	1.4	7
71	Vaporâ^'Liquid Equilibrium for Binary System of Diethyl Sulfide +n-Hexane at (338.15 and 323.15) K and Diethyl Sulfide + 1-Hexene at (333.15 and 323.15) K. Journal of Chemical & Engineering Data, 2007, 52, 571-576.	1.0	6
72	Vaporâ€"Liquid Equilibrium for the Systems trans-2-Butene + Methanol, + 1-Propanol, + 2-Propanol, + 2-Butanol, and + 2-Methyl-2-propanol at 364.5 K. Journal of Chemical & Engineering Data, 2008, 53, 607-612.	1.0	6

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73	Vaporâˆ'Liquid Equilibrium for Tetrahydrothiophene + n-Butane, + trans-2-Butene, + 2-Methylpropane, and + 2-Methylpropene. Journal of Chemical & Engineering Data, 2009, 54, 1311-1317.	1.0	6
74	Phase equilibrium measurements for systems containing propanenitrile with tert-butyl ethyl ether and C4-hydrocarbons. Fluid Phase Equilibria, 2010, 299, 148-160.	1.4	6
75	Phase equilibria for systems containing dimethyl disulfide and diethyl disulfide with hydrocarbons at 368.15K. Fluid Phase Equilibria, 2010, 293, 175-181.	1.4	6
76	Vaporâ€"Liquid Equilibrium, Excess Molar Enthalpies, and Excess Molar Volumes of Binary Mixtures Containing 2-Ethoxy-2-methylpropane or 2-Ethoxy-2-methylbutane and Acetonitrile or Propanenitrile. Journal of Chemical & Engineering Data, 2013, 58, 943-950.	1.0	6
77	Design of Equilibrium Cells for Phase Equilibria and PVT Measurements in Large Ranges of Temperatures and Pressures. I. Vaporâ€"Liquidâ€"Liquid Equilibria. Journal of Chemical & Engineering Data, 2016, 61, 2700-2711.	1.0	6
78	Isobaric Vaporâ€"Liquid Equilibrium of Furfural + Î³-Valerolactone at 30 kPa and Isothermal Liquidâ€"Liquid Equilibrium of Carbon Dioxide + Î³-Valerolactone + Water at 298 K. Journal of Chemical & Engineering Data, 0, , .	1.0	6
79	110th Anniversary: Critical Properties and High Temperature Vapor Pressures for Furan, 2-Methylfuran, 2-Methoxy-2-methylpropane, 2-Ethoxy-2-methylbutane, n-Hexane, and Ethanol and Bubble Points of Mixtures with a New Apparatus. Industrial & Engineering Chemistry Research, 2019, 58, 22350-22362.	1.8	6
80	Practical Methodology for Distillation Design using a Miniplant. Chemical Engineering and Technology, 2006, 29, 104-112.	0.9	5
81	Vaporâˆ'Liquid Equilibrium for the cis-2-Butene + Methanol, + 2-Propanol, + 2-Butanol, + 2-Methyl-2-propanol Systems at 364.5 K. Journal of Chemical & Engineering Data, 2008, 53, 1539-1544.	1.0	5
82	The use of microplants in process developmentâ€"Case study of etherification of 2-ethoxy-2-methylbutane. Chemical Engineering and Processing: Process Intensification, 2013, 74, 75-82.	1.8	5
83	Measurement of activity coefficient at infinite dilution for some bio-oil components in water and mass transfer study of bubbles in the dilutor. Fluid Phase Equilibria, 2015, 392, 1-11.	1.4	5
84	A comprehensive study of CO 2 solubility in aqueous 2-HEAA and MEA + 2-HEAA solutions â€" Measurements and modeling. International Journal of Greenhouse Gas Control, 2015, 42, 296-306.	2.3	5
85	Temperature and Pressure Dependence of Density of a Shale Oil and Derived Thermodynamic Properties. Industrial & Engineering Chemistry Research, 2018, 57, 5128-5135.	1.8	5
86	A Volumetric Pitzer Model for Aqueous Solutions of Zinc Sulfate up to Near-Saturation Concentrations at Temperatures from 293.15 to 393.15 K and Pressures up to 10 MPa. Journal of Chemical & Engineering Data, 2021, 66, 58-64.	1.0	5
87	Liquid â€" liquid equilibria in binary and ternary systems of phenolÂ+Âhydrocarbons (nâ€"dodecane or) Tj ETQq1 1 0.784314 rgBT /Ov between 298K and 353K. Fluid Phase Equilibria, 2022, 556, 113402.	1.4	5
88	Vapor Liquid Equilibrium for the Binary Systems of 2-Methylpropane + Ethanenitrile and 2-Methylpropene + Ethanenitrile at 358 K. Journal of Chemical & Engineering Data, 2000, 45, 116-119.	1.0	4
89	Vaporâˆ'Liquid Equilibrium for 1-Butanol + 1-Butene at (318.4 and 364.5) K and Vaporâˆ'Liquid Equilibrium of 1-Butanol + 2-Methylpropane, + n-Butane and 1-Butene + 2-Methylpropane at 318.4 K. Journal of Chemical & Engineering Data, 2008, 53, 2454-2461.	1.0	4
90	Vaporâ€"liquid equilibrium for the binary systems tetrahydrothiophene+toluene and tetrahydrothiophene+o-xylene at 368.15K and 383.15K. Fluid Phase Equilibria, 2010, 296, 4-8.	1.4	4

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91	Infinite dilution activity coefficient and vapour liquid equilibrium measurements for dimethylsulphide and tetrahydrothiophene with hydrocarbons. Fluid Phase Equilibria, 2010, 295, 17-25.	1.4	4
92	Vaporâ"Liquid Equilibrium for Thiophene + Butane, +trans-But-2-ene, + 2-Methylpropane, and + 2-Methylpropene. Journal of Chemical & Engineering Data, 2011, 56, 614-621.	1.0	4
93	Prototyping a calorimeter mixing cell with direct metal laser sintering. Chemical Engineering Research and Design, 2016, 108, 146-151.	2.7	4
94	Solubility of carbon monoxide in bio-oil compounds. Journal of Chemical Thermodynamics, 2017, 105, 296-311.	1.0	4
95	Densities, Viscosities, and Thermal Conductivities of the Ionic Liquid 7-Methyl-1,5,7-triazabicyclo[4.4.0]dec-5-enium Acetate and Its Mixtures with Water. International Journal of Thermophysics, 2020, 41, 1.	1.0	4
96	Volumetric Properties of Aqueous Solutions of Zinc Sulfate at Temperatures from 298.15 to 393.15 K and Pressures up to 10 MPa. Journal of Chemical & Engineering Data, 2021, 66, 45-57.	1.0	4
97	Vapor Liquid Equilibria for Ethanol + 2,4,4-Trimethyl-1-pentene and 2-Propanol + 2,4,4-Trimethyl-1-pentene at 101 kPa. Journal of Chemical & Engineering Data, 2003, 48, 280-285.	1.0	3
98	Vaporâ€"Liquid Equilibrium for the Systems 2-Methylpropane + Methanol, + 2-Propanol, + 2-Butanol, and + 2-Methyl-2-propanol at 364.5 K. Journal of Chemical & Engineering Data, 2008, 53, 913-918.	1.0	3
99	Application of Microreactors in the Dehydrogenation of Isobutane. Topics in Catalysis, 2011, 54, 1206-1212.	1.3	3
100	Study of CO₂ Absorption into Phase Change Solvents MAPA and DEEA. Journal of Chemical & Engineering Data, 2017, 62, 2261-2271.	1.0	3
101	Vaporâ€"liquid equilibrium measurements of dimethylsulfide, +ethanol, +dimethylether, +methylacetate with a static total pressure method. Fluid Phase Equilibria, 2013, 355, 34-39.	1.4	2
102	FEASIBILITY OF LASER MATERIAL PROCESSING IN THE DESIGN AND MANUFACTURE OF SMALL SCALE DEVICES. Mechanika, 2013, 19, .	0.3	2
103	Micro-scale piloting of a process for production of 2-methoxy-2,4,4-trimethylpentane. Chemical Engineering and Processing: Process Intensification, 2017, 122, 143-154.	1.8	2
104	Application of GaInSn Liquid Metal Alloy Replacing Mercury in a Phase Equilibrium Cell: Vapor Pressures of Toluene, Hexylbenzene, and 2-Ethylnaphthalene. Journal of Chemical & Engineering Data, 2020, 65, 3270-3276.	1.0	2
105	Hydrodeoxygenation Model Compounds Î³-Heptalactone and Î³-Nonalactone: Density from 293 to 473 K and H₂ Solubility from 479 to 582 K. Journal of Chemical & Engineering Data, 2020, 65, 2764-2773.	1.0	2
106	Measurements and modeling for the density of 2-methoxy-2,4,4-trimethylpentane, HE for (methanol +) Tj ETQq0 0 0 rgBT /Overlock 10 T (water + methanol + 2-methoxy-2,4,4-trimethylpentane). Journal of Chemical Thermodynamics, 2015, 91, 313-320.	1.0	1
107	Vaporâ€"liquid equilibrium for binary system of tetrahydrothiophene+2,2,4-trimethylpentane and tetrahydrothiophene+2,4,4-trimethyl-1-pentene at 358.15 and 368.15K. Fluid Phase Equilibria, 2010, 296, 159-163.	1.4	0
108	Reply to the letter to the editor by J. Gmehling and A. Jacob about the paper â€œPhase equilibria on four binary systems containing 3-methylthiopheneâ€•[Fluid Phase Equilib. 279 (2009) 81â€"86]. Fluid Phase Equilibria, 2010, 292, 117.	1.4	0

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109	6. Process intensification for microdistillation using the equipment miniaturization approach. , 2017, , 213-240.		0
110	Hydrodeoxygenation of Propylphenols on a Niobiaâ€Supported Platinum Catalyst: Ortho , Meta , Para Isomerism, Reaction Conditions, and Phase Equilibria. Advanced Sustainable Systems, 2020, 4, 1900140.	2.7	0
111	Laser welding of micro-VLE-measurement device and its practical application. , 2010, , .		0