

Estela Lladosa

List of Publications by Year in descending order

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48
papers

1,060
citations

393982

19
h-index

454577

30
g-index

50
all docs

50
docs citations

50
times ranked

761
citing authors

#	ARTICLE	IF	CITATIONS
1	Optimization of rice straw pretreatment with 1-ethyl-3-methylimidazolium acetate by the response surface method. <i>Biomass Conversion and Biorefinery</i> , 2023, 13, 12057-12072.	2.9	8
2	Thermophysical Properties of Mixtures of 1-Ethyl-3-methylimidazolium Methylsulfate or 1-Ethyl-3-methylimidazolium Thiocyanate with Alcohols. <i>Journal of Chemical & Engineering Data</i> , 2021, 66, 968-978.	1.0	12
3	Azeotropic distillation for 1-propanol dehydration with diisopropyl ether as entrainer: Equilibrium data and process simulation. <i>Separation and Purification Technology</i> , 2019, 212, 692-698.	3.9	48
4	Capability study of 1-butyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide and trihexyl(tetradecyl)phosphonium bis(2,4,4-trimethylpentyl)phosphinate as solvents in the separation of 1-propanol from water. <i>Fluid Phase Equilibria</i> , 2018, 469, 1-8.	1.4	13
5	Experimental Determination and Correlation of Liquid-Liquid Equilibria Data for a System of Water + Ethanol + 1-Butyl-3-methylimidazolium Hexafluorophosphate at Different Temperatures. <i>Journal of Chemical & Engineering Data</i> , 2017, 62, 773-779.	1.0	13
6	Proposal of Isobutyl Alcohol as Entrainer To Separate Mixtures Formed by Ethanol and Water and 1-Propanol and Water. <i>Journal of Chemical & Engineering Data</i> , 2017, 62, 2697-2707.	1.0	5
7	Evaluation of Diethyl Carbonate and Methyl Isobutyl Ketone as Entrainers for the Separation of 1-Hexene and <i>n</i> -Hexane. <i>Journal of Chemical & Engineering Data</i> , 2017, 62, 1355-1364.	1.0	4
8	Isobaric vapor-liquid equilibria for extractive distillation of 1-propanol + water mixture using thiocyanate-based ionic liquids. <i>Journal of Chemical Thermodynamics</i> , 2017, 113, 219-228.	1.0	17
9	Study of liquid-liquid equilibria at different temperatures of water+ethanol+1-butyl-1-methylpyrrolidinium bis(trifluoromethylsulfonyl)imide ternary system. <i>Fluid Phase Equilibria</i> , 2016, 426, 3-9.	1.4	30
10	Liquid-Liquid Equilibria of the Water + 1-Propanol + 1-Butyl-1-methylpyrrolidinium Bis(trifluoromethylsulfonyl)imide Ternary System: Study of the Ability of Ionic Liquid as a Solvent. <i>Journal of Chemical & Engineering Data</i> , 2016, 61, 4006-4012.	1.0	17
11	Density, Viscosity, and Sound Speed of Bis(trifluoromethylsulfonyl)imide-Based Ionic Liquids + 1-Propanol Mixtures. <i>Journal of Chemical & Engineering Data</i> , 2016, 61, 56-66.	1.0	19
12	Density, Speed of Sound, Viscosity, and Excess Properties of Binary Mixtures Formed by Ethanol and Bis(trifluorosulfonyl)imide-Based Ionic Liquids. <i>Journal of Chemical & Engineering Data</i> , 2015, 60, 525-540.	1.0	88
13	Approach to the 1-propanol dehydration using an extractive distillation process with ethylene glycol. <i>Chemical Engineering and Processing: Process Intensification</i> , 2015, 91, 121-129.	1.8	22
14	Liquid-Liquid Equilibria of Water + Ethanol + 1-Butyl-3-methylimidazolium Bis(trifluoromethanesulfonyl)imide Ternary System: Measurements and Correlation at Different Temperatures. <i>Journal of Chemical & Engineering Data</i> , 2015, 60, 2426-2433.	1.0	40
15	Answer to the Letter to the Editor by Dr. Sanjay Pralhad Shirsat concerning the article "Separation of isobutyl alcohol and isobutyl acetate by extractive distillation and pressure-swing distillation: Simulation and optimization". <i>Separation and Purification Technology</i> , 2015, 154, 367.	3.9	0
16	Thermodynamic Analysis and Process Simulation of Ethanol Dehydration via Heterogeneous Azeotropic Distillation. <i>Industrial & Engineering Chemistry Research</i> , 2014, 53, 6084-6093.	1.8	38
17	Isobaric Vapor-Liquid Equilibria for the Ternary Systems Ethanol + Water + Propyl Acetate and 1-Propanol + Water + Propyl acetate. <i>Journal of Chemical & Engineering Data</i> , 2014, 59, 2054-2064.	1.0	18
18	Measurements and correlation at different temperatures of liquid-liquid equilibria of 2-butanol or 2-methyl-2-butanol+1,2,3-propanetriol+water ternary systems. <i>Fluid Phase Equilibria</i> , 2014, 377, 38-44.	1.4	14

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19	Liquid-liquid equilibria of 4-methyl-2-pentanone+1-propanol or 2-propanol+water ternary systems: Measurements and correlation at different temperatures. <i>Fluid Phase Equilibria</i> , 2014, 361, 23-29.	1.4	40
20	Evaluation of the 2-Methoxyethanol as Entrainer in Ethanol-Water and 1-Propanol-Water Mixtures. <i>Journal of Chemical & Engineering Data</i> , 2013, 58, 3504-3512.	1.0	14
21	Phase equilibria for the ternary systems ethanol, water+ethylene glycol or+glycerol at 101.3kPa. <i>Fluid Phase Equilibria</i> , 2013, 341, 54-60.	1.4	28
22	Effect of Aqueous Two-Phase System Constituents in Different Poly(ethylene glycol)-Salt Phase Diagrams. <i>Journal of Chemical & Engineering Data</i> , 2012, 57, 1203-1208.	1.0	53
23	(Liquid+liquid) equilibria of polymer-salt aqueous two-phase systems for laccase partitioning: UCON 50-HB-5100 with potassium citrate and (sodium or potassium) formate at 23°C. <i>Journal of Chemical Thermodynamics</i> , 2012, 55, 166-171.	1.0	32
24	Measurements and correlation of liquid-liquid equilibria of 4-methyl-2-pentanone+ethanol+water and 4-methyl-2-pentanone+n-butanol+water ternary systems between 283.2 and 323.2K. <i>Fluid Phase Equilibria</i> , 2012, 317, 89-95.	1.4	30
25	Liquid-Liquid and Vapor-Liquid Equilibrium of the 4-Methyl-2-pentanone + 2-Butanol + Water System. <i>Journal of Chemical & Engineering Data</i> , 2011, 56, 1925-1932.	1.0	14
26	Liquid-Liquid and Vapor-Liquid Equilibrium of the 2-Butanone + 2-Butanol + Water System. <i>Journal of Chemical & Engineering Data</i> , 2011, 56, 1755-1761.	1.0	12
27	Phase Equilibria Involved in the Extractive Distillation of Cyclohexane + Cyclohexene Using Diethyl Carbonate as an Entrainer. <i>Journal of Chemical & Engineering Data</i> , 2011, 56, 4790-4796.	1.0	8
28	Separation of di-n-propyl ether and n-propyl alcohol by extractive distillation and pressure-swing distillation: Computer simulation and economic optimization. <i>Chemical Engineering and Processing: Process Intensification</i> , 2011, 50, 1266-1274.	1.8	60
29	Measurements and correlation of vapour-liquid equilibria of 2-butanone and hydrocarbons binary systems at two different pressures. <i>Fluid Phase Equilibria</i> , 2011, 307, 24-29.	1.4	6
30	Phase equilibrium for the systems diisopropyl ether, isopropyl alcohol+2,2,4-trimethylpentane and +n-heptane at 101.3kPa. <i>Fluid Phase Equilibria</i> , 2010, 289, 135-139.	1.4	7
31	Effect of the reference solution in the measurement of ion activity coefficients using cells with transference at T=298.15K. <i>Journal of Chemical Thermodynamics</i> , 2010, 42, 244-250.	1.0	14
32	Isobaric Vapor-Liquid Equilibria for Binary and Ternary Mixtures of Ethanol and 2-Propanol with 2-Butanone and Butyl Propionate at 101.3 kPa. <i>Journal of Chemical & Engineering Data</i> , 2010, 55, 798-803.	1.0	13
33	Liquid-Liquid Equilibria for the System 1-Methyl Propyl Ethanoate (1) + Acetic Acid (2) + Water (3) at (283.15 and 323.15) K. <i>Journal of Chemical & Engineering Data</i> , 2010, 55, 523-525.	1.0	10
34	Isobaric vapour-liquid equilibria for the binary systems 4-methyl-2-pentanone+1-butanol and+2-butanol at 20 and 101.3kPa. <i>Fluid Phase Equilibria</i> , 2009, 277, 49-54.	1.4	20
35	Isobaric Vapor-Liquid Equilibria for Binary and Ternary Mixtures of Diisopropyl Ether, 2-Propyl Alcohol, and n-Butyl Propionate at 101.3 kPa. <i>Journal of Chemical & Engineering Data</i> , 2009, 54, 2991-2995.	1.0	5
36	Liquid-liquid equilibria of the systems isobutyl acetate+isobutyl alcohol+water and isobutyl acetate+isobutyl alcohol+glycerol at different temperatures. <i>Fluid Phase Equilibria</i> , 2008, 265, 122-128.	1.4	11

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37	Isobaric (vapour+liquid+liquid) equilibrium data for (di-n-propyl ether+n-propyl alcohol+water) and (diisopropyl ether+isopropyl alcohol+water) systems at 100kPa. Journal of Chemical Thermodynamics, 2008, 40, 867-873.	1.0	24
38	Isobaric vapour-liquid equilibria for binary systems of 2-butanone with ethanol, 1-propanol, and 2-propanol at 20 and 101.3kPa. Fluid Phase Equilibria, 2008, 270, 62-68.	1.4	40
39	Study of liquid-liquid equilibrium of the systems isobutyl acetate+acetic acid+water and isobutyl alcohol+acetic acid+water at different temperatures. Fluid Phase Equilibria, 2008, 271, 76-81.	1.4	36
40	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa. Journal of Chemical & Engineering Data, 2008, 53, 108-115.	1.0	34
41	Isobaric Vapor-Liquid Equilibria for Binary and Ternary Mixtures of Diisopropyl Ether, 2-Propyl Alcohol, and 3-Methyl-1-Butanol. Journal of Chemical & Engineering Data, 2008, 53, 1897-1902.	1.0	13
42	Phase Equilibria Involved in Extractive Distillation of Dipropyl Ether + 1-Propyl Alcohol Using N,N-Dimethylformamide as Entrainer. Journal of Chemical & Engineering Data, 2007, 52, 532-537.	1.0	9
43	Phase equilibria involved in extractive distillation of dipropyl ether+1-propyl alcohol using 2-ethoxyethanol as entrainer. Fluid Phase Equilibria, 2007, 255, 62-69.	1.4	21
44	Liquid-liquid equilibria of the systems dipropyl ether+n-propanol+water and dipropyl ether+n-propanol+ethylene glycol at different temperatures. Fluid Phase Equilibria, 2007, 262, 76-81.	1.4	11
45	Effect of pressure and the capability of 2-methoxyethanol as a solvent in the behaviour of a diisopropyl ether-isopropyl alcohol azeotropic mixture. Fluid Phase Equilibria, 2007, 262, 271-279.	1.4	34
46	Isobaric Vapor-Liquid Equilibria for Binary and Ternary Mixtures of Dipropyl Ether, 1-Propyl Alcohol, and Butyl Propionate. Journal of Chemical & Engineering Data, 2006, 51, 2233-2238.	1.0	11
47	Isobaric vapor-liquid equilibria for the binary systems 1-propyl alcohol+dipropyl ether and 1-butyl alcohol+dibutyl ether at 20 and 101.3kPa. Fluid Phase Equilibria, 2006, 247, 47-53.	1.4	25
48	Vapor-liquid equilibria in the ternary system dipropyl ether+1-propanol+1-pentanol and the binary systems dipropyl ether+1-pentanol, 1-propanol+1-pentanol at 101.3kPa. Fluid Phase Equilibria, 2006, 247, 175-181.	1.4	16