

Sigurd Skogestad

List of Publications by Citations

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The third column is the impact factor (IF) of the journal, and the fourth column is the number of citations of the article.

263
papers

9,593
citations

48
h-index

91
g-index

282
ext. papers

10,898
ext. citations

3.2
avg. IF

6.72
L-index

#	Paper	IF	Citations
263	Simple analytic rules for model reduction and PID controller tuning. <i>Journal of Process Control</i> , 2003 , 13, 291-309	3.9	1151
262	Internal model control: PID controller design. <i>Industrial & Engineering Chemistry Process Design and Development</i> , 1986 , 25, 252-265		909
261	Plantwide control: the search for the self-optimizing control structure. <i>Journal of Process Control</i> , 2000 , 10, 487-507	3.9	406
260	Control structure design for complete chemical plants. <i>Computers and Chemical Engineering</i> , 2004 , 28, 219-234	4	288
259	Operation of Integrated Three-Product (Petlyuk) Distillation Columns. <i>Industrial & Engineering Chemistry Research</i> , 1995 , 34, 2094-2103	3.9	227
258	Implications of large RGA-elements on control performance. <i>Industrial & Engineering Chemistry Research</i> , 1987 , 26, 2323-2330	3.9	180
257	Understanding the dynamic behavior of distillation columns. <i>Industrial & Engineering Chemistry Research</i> , 1988 , 27, 1848-1862	3.9	175
256	Simple frequency-dependent tools for control system analysis, structure selection and design. <i>Automatica</i> , 1992 , 28, 989-996	5.7	162
255	Estimation of distillation compositions from multiple temperature measurements using partial-least-squares regression. <i>Industrial & Engineering Chemistry Research</i> , 1991 , 30, 2543-2555	3.9	154
254	Plantwide control - A review and a new design procedure. <i>Modeling, Identification and Control</i> , 2000 , 21, 209-240	1	152
253	Optimal Selection of Controlled Variables. <i>Industrial & Engineering Chemistry Research</i> , 2003 , 42, 3273-3284	3.9	144
252	Robust performance of decentralized control systems by independent designs. <i>Automatica</i> , 1989 , 25, 119-125	5.7	135
251	Sequential design of decentralized controllers. <i>Automatica</i> , 1994 , 30, 1601-1607	5.7	124
250	Minimum Energy Consumption in Multicomponent Distillation. 2. Three-Product Petlyuk Arrangements. <i>Industrial & Engineering Chemistry Research</i> , 2003 , 42, 605-615	3.9	117
249	Null Space Method for Selecting Optimal Measurement Combinations as Controlled Variables. <i>Industrial & Engineering Chemistry Research</i> , 2007 , 46, 846-853	3.9	116
248	Optimal measurement combinations as controlled variables. <i>Journal of Process Control</i> , 2009 , 19, 138-148	3.9	107
247	Self-Optimizing Control of a Large-Scale Plant: The Tennessee Eastman Process. <i>Industrial & Engineering Chemistry Research</i> , 2001 , 40, 4889-4901	3.9	99

246	LV-Control of a high-purity distillation column. <i>Chemical Engineering Science</i> , 1988 , 43, 33-48	4.4	97
245	Optimal operation of Petlyuk distillation: steady-state behavior. <i>Journal of Process Control</i> , 1999 , 9, 407-424	3.9	94
244	Multiple steady states in ideal two-product distillation. <i>AIChE Journal</i> , 1991 , 37, 499-511	3.6	94
243	Selecting the best distillation control configuration. <i>AIChE Journal</i> , 1990 , 36, 753-764	3.6	93
242	Effect of disturbance directions on closed-loop performance. <i>Industrial & Engineering Chemistry Research</i> , 1987 , 26, 2029-2035	3.9	89
241	The setpoint overshoot method: A simple and fast closed-loop approach for PID tuning. <i>Journal of Process Control</i> , 2010 , 20, 1220-1234	3.9	88
240	Minimum Energy Consumption in Multicomponent Distillation. 3. More Than Three Products and Generalized Petlyuk Arrangements. <i>Industrial & Engineering Chemistry Research</i> , 2003 , 42, 616-629	3.9	88
239	Complex distillation arrangements: Extending the petlyuk ideas. <i>Computers and Chemical Engineering</i> , 1997 , 21, S237-S242	4	84
238	Minimum Energy Consumption in Multicomponent Distillation. 1. VminDiagram for a Two-Product Column. <i>Industrial & Engineering Chemistry Research</i> , 2003 , 42, 596-604	3.9	84
237	Self-optimizing control: the missing link between steady-state optimization and control. <i>Computers and Chemical Engineering</i> , 2000 , 24, 569-575	4	83
236	Composition estimator in a pilot-plant distillation column using multiple temperatures. <i>Industrial & Engineering Chemistry Research</i> , 1991 , 30, 2555-2564	3.9	82
235	Analysis of instability in an industrial ammonia reactor. <i>AIChE Journal</i> , 1998 , 44, 888-895	3.6	81
234	Control configuration selection for distillation columns. <i>AIChE Journal</i> , 1987 , 33, 1620-1635	3.6	81
233	Dynamics and Control of Distillation Columns - A Critical Survey. <i>Modeling, Identification and Control</i> , 1997 , 18, 177-217	1	77
232	Economically efficient operation of CO ₂ capturing process part I: Self-optimizing procedure for selecting the best controlled variables. <i>Chemical Engineering and Processing: Process Intensification</i> , 2011 , 50, 247-253	3.7	76
231	Active Vapor Split Control for Dividing-Wall Columns. <i>Industrial & Engineering Chemistry Research</i> , 2012 , 51, 15176-15183	3.9	70
230	Control structure design for the ammonia synthesis process. <i>Computers and Chemical Engineering</i> , 2008 , 32, 2920-2932	4	68
229	Performance weight selection for H-infinity and E-control methods. <i>Transactions of the Institute of Measurement and Control</i> , 1991 , 13, 241-252	1.8	67

228	Energy efficient distillation. <i>Journal of Natural Gas Science and Engineering</i> , 2011 , 3, 571-580	4.6	66
227	Tuning for Smooth PID Control with Acceptable Disturbance Rejection. <i>Industrial & Engineering Chemistry Research</i> , 2006 , 45, 7817-7822	3.9	66
226	Economically efficient operation of CO ₂ capturing process. Part II. Design of control layer. <i>Chemical Engineering and Processing: Process Intensification</i> , 2012 , 52, 112-124	3.7	64
225	An industrial and academic perspective on plantwide control. <i>Annual Reviews in Control</i> , 2011 , 35, 99-110	4.3	61
224	Optimal operation of simple refrigeration cycles. <i>Computers and Chemical Engineering</i> , 2007 , 31, 712-724	4	61
223	Dividing wall columns for heterogeneous azeotropic distillation. <i>Chemical Engineering Research and Design</i> , 2015 , 99, 111-119	5.5	58
222	Application of plantwide control to the HDA process. Steady-state optimization and self-optimizing control. <i>Control Engineering Practice</i> , 2007 , 15, 1222-1237	3.9	57
221	Pairing Criteria for Decentralized Control of Unstable Plants. <i>Industrial & Engineering Chemistry Research</i> , 1994 , 33, 2134-2139	3.9	56
220	Optimal PI and PID control of first-order plus delay processes and evaluation of the original and improved SIMC rules. <i>Journal of Process Control</i> , 2018 , 70, 36-46	3.9	56
219	Design of resilient processing plants-IX. Effect of model uncertainty on dynamic resilience. <i>Chemical Engineering Science</i> , 1987 , 42, 1765-1780	4.4	55
218	Multivessel batch distillation. <i>AIChE Journal</i> , 1997 , 43, 971-978	3.6	54
217	Coordinator MPC for maximizing plant throughput. <i>Computers and Chemical Engineering</i> , 2008 , 32, 195-204	4	53
216	Control of fuel cell power output. <i>Journal of Process Control</i> , 2007 , 17, 333-347	3.9	52
215	NCO tracking and self-optimizing control in the context of real-time optimization. <i>Journal of Process Control</i> , 2011 , 21, 1407-1416	3.9	48
214	Shortcut Analysis of Optimal Operation of Petlyuk Distillation. <i>Industrial & Engineering Chemistry Research</i> , 2004 , 43, 3994-3999	3.9	48
213	Comparison of regular and inverted batch distillation. <i>Chemical Engineering Science</i> , 1996 , 51, 4949-4962	4.4	48
212	SVD controllers for H ₂ and optimal control. <i>Automatica</i> , 1997 , 33, 433-439	5.7	46
211	Controllability analysis of two-phase pipeline-riser systems at riser slugging conditions. <i>Control Engineering Practice</i> , 2007 , 15, 567-581	3.9	44

210	Dynamic behaviour of integrated plants. <i>Journal of Process Control</i> , 1996 , 6, 145-156	3.9	44
209	A Natural Gas to Liquids Process Model for Optimal Operation. <i>Industrial & Engineering Chemistry Research</i> , 2012 , 51, 425-433	3.9	42
208	Optimal operation of Kaibel distillation columns. <i>Chemical Engineering Research and Design</i> , 2011 , 89, 1382-1391	5.5	41
207	Representation of uncertain time delays in the H _∞ framework. Present address: Department of Electrical Engineering, Pennsylvania State University, U.S.A.. <i>International Journal of Control</i> , 1994 , 59, 627-638	1.5	41
206	Output estimation using multiple secondary measurements: High-purity distillation. <i>AIChE Journal</i> , 1993 , 39, 1641-1653	3.6	41
205	Optimizing control of Petlyuk distillation: Understanding the steady-state behavior. <i>Computers and Chemical Engineering</i> , 1997 , 21, S249-S254	4	40
204	Optimal operation of simple refrigeration cycles. <i>Computers and Chemical Engineering</i> , 2007 , 31, 1590-1601	4	40
203	Total reflux operation of multivessel batch distillation. <i>Computers and Chemical Engineering</i> , 1996 , 20, S1041-S1046	4	39
202	Effects of recycle on dynamics and control of chemical processing plants. <i>Computers and Chemical Engineering</i> , 1994 , 18, S529-S534	4	39
201	Comparison of Various Control Configurations for Continuous Bioreactors. <i>Industrial & Engineering Chemistry Research</i> , 1997 , 36, 697-705	3.9	38
200	Hydraulic design, technical challenges and comparison of alternative configurations of a four-product dividing wall column. <i>Chemical Engineering and Processing: Process Intensification</i> , 2014 , 84, 71-81	3.7	37
199	Inadequacy of steady-state analysis for feedback control: distillate-bottom control of distillation columns. <i>Industrial & Engineering Chemistry Research</i> , 1990 , 29, 2339-2346	3.9	37
198	Control structure selection for three-product Petlyuk (dividing-wall) column. <i>Chemical Engineering and Processing: Process Intensification</i> , 2013 , 64, 57-67	3.7	36
197	Application of Plantwide Control to the HDA Process. IIRegulatory Control. <i>Industrial & Engineering Chemistry Research</i> , 2007 , 46, 5159-5174	3.9	36
196	Multi-effect distillation applied to an industrial case study. <i>Chemical Engineering and Processing: Process Intensification</i> , 2005 , 44, 819-826	3.7	36
195	Improved independent design of robust decentralized controllers. <i>Journal of Process Control</i> , 1993 , 3, 43-51	3.9	35
194	Selection of Controlled Variables and Robust Setpoints. <i>Industrial & Engineering Chemistry Research</i> , 2005 , 44, 2207-2217	3.9	34
193	Near-optimal operation by self-optimizing control: from process control to marathon running and business systems. <i>Computers and Chemical Engineering</i> , 2004 , 29, 127-137	4	34

192	Integrating operations and control: A perspective and roadmap for future research. <i>Computers and Chemical Engineering</i> , 2018 , 115, 179-184	4	33
191	Steady State and Dynamic Operation of Four-Product Dividing-Wall (Kaibel) Columns: Experimental Verification. <i>Industrial & Engineering Chemistry Research</i> , 2012 , 51, 15696-15709	3.9	33
190	Steady-state real-time optimization using transient measurements. <i>Computers and Chemical Engineering</i> , 2018 , 115, 34-45	4	31
189	Consistent Inventory Control. <i>Industrial & Engineering Chemistry Research</i> , 2009 , 48, 10892-10902	3.9	30
188	Control structure design for optimal operation of heat exchanger networks. <i>AIChE Journal</i> , 2008 , 54, 150-162	3.6	30
187	Dynamic models for heat exchangers and heat exchanger networks. <i>Computers and Chemical Engineering</i> , 1994 , 18, S459-S463	4	30
186	Real-Time Optimization under Uncertainty Applied to a Gas Lifted Well Network. <i>Processes</i> , 2016 , 4, 52	2.9	30
185	Control structure selection for four-product Petlyuk column. <i>Chemical Engineering and Processing: Process Intensification</i> , 2013 , 67, 49-59	3.7	29
184	Control-oriented modelling and experimental study of the transient response of a high-temperature polymer fuel cell. <i>Journal of Power Sources</i> , 2006 , 162, 215-227	8.9	29
183	Inconsistencies in Dynamic Models for Ill-Conditioned Plants: Application to Low-Order Models of Distillation Columns. <i>Industrial & Engineering Chemistry Research</i> , 1994 , 33, 631-640	3.9	29
182	Convex formulations for optimal selection of controlled variables and measurements using Mixed Integer Quadratic Programming. <i>Journal of Process Control</i> , 2012 , 22, 995-1007	3.9	28
181	Buffer Tank Design for Acceptable Control Performance. <i>Industrial & Engineering Chemistry Research</i> , 2003 , 42, 2198-2208	3.9	28
180	Control structure selection for four-product Kaibel column. <i>Computers and Chemical Engineering</i> , 2016 , 93, 372-381	4	27
179	Model Predictive Control of Reactive Dividing Wall Column for the Selective Hydrogenation and Separation of a C3 Stream in an Ethylene Plant. <i>Industrial & Engineering Chemistry Research</i> , 2016 , 55, 9738-9748	3.9	26
178	Problems with Specifying τ_{\min} in the Design of Processes with Heat Exchangers. <i>Industrial & Engineering Chemistry Research</i> , 2008 , 47, 3071-3075	3.9	26
177	Data reconciliation and optimal operation of a catalytic naphtha reformer. <i>Journal of Process Control</i> , 2008 , 18, 320-331	3.9	26
176	Single-cycle mixed-fluid LNG process Part I: Optimal design 2009 , 211-218		25
175	Dynamic considerations in the synthesis of self-optimizing control structures. <i>AIChE Journal</i> , 2008 , 54, 1830-1841	3.6	24

174	Instability of distillation columns. <i>AICHE Journal</i> , 1994 , 40, 1466-1478	3.6	24
173	Model predictive control for the self-optimized operation in wastewater treatment plants: Analysis of dynamic issues. <i>Computers and Chemical Engineering</i> , 2015 , 82, 259-272	4	23
172	Control structure design and dynamic modeling for a solid oxide fuel cell with direct internal reforming of methane. <i>Chemical Engineering Research and Design</i> , 2015 , 98, 202-211	5.5	23
171	Self-optimizing control with active set changes. <i>Journal of Process Control</i> , 2012 , 22, 873-883	3.9	22
170	Steady-State Operational Degrees of Freedom with Application to Refrigeration Cycles. <i>Industrial & Engineering Chemistry Research</i> , 2009 , 48, 6652-6659	3.9	22
169	Selection of Controlled Variables: Maximum Gain Rule and Combination of Measurements. <i>Industrial & Engineering Chemistry Research</i> , 2008 , 47, 9465-9471	3.9	22
168	Optimal operation of heat exchanger networks with stream split: Only temperature measurements are required. <i>Computers and Chemical Engineering</i> , 2014 , 70, 35-49	4	21
167	Multiple Steady States and Instability in Distillation. Implications for Operation and Control. <i>Industrial & Engineering Chemistry Research</i> , 1995 , 34, 4395-4405	3.9	21
166	Temperature Cascade Control of Distillation Columns. <i>Industrial & Engineering Chemistry Research</i> , 1996 , 35, 475-484	3.9	21
165	Active constraint regions for a natural gas liquefaction process. <i>Journal of Natural Gas Science and Engineering</i> , 2013 , 10, 8-13	4.6	20
164	Control of the mass and energy dynamics of polybenzimidazole-membrane fuel cells. <i>Journal of Process Control</i> , 2009 , 19, 415-432	3.9	20
163	Perfect Steady-State Indirect Control. <i>Industrial & Engineering Chemistry Research</i> , 2005 , 44, 863-867	3.9	20
162	Relative Gain Array for Norm-Bounded Uncertain Systems. <i>Industrial & Engineering Chemistry Research</i> , 2006 , 45, 1751-1757	3.9	20
161	Minimum energy diagrams for multieffect distillation arrangements. <i>AICHE Journal</i> , 2005 , 51, 1714-1725	3.6	20
160	Control strategies for reactive batch distillation. <i>Journal of Process Control</i> , 1994 , 4, 205-217	3.9	20
159	Plantwide Control for Economic Optimum Operation of a Recycle Process with Side Reaction. <i>Industrial & Engineering Chemistry Research</i> , 2011 , 50, 8571-8584	3.9	19
158	Optimal operation and stabilising control of the concentric heat-integrated distillation column (HIDiC). <i>Computers and Chemical Engineering</i> , 2017 , 96, 196-211	4	18
157	Bypass selection for control of heat exchanger networks. <i>Computers and Chemical Engineering</i> , 1992 , 16, S263-S272	4	18

156	Economic Plantwide Control of the Cumene Process. <i>Industrial & Engineering Chemistry Research</i> , 2013 , 52, 830-846	3.9	17
155	pH-neutralization: integrated process and control design. <i>Computers and Chemical Engineering</i> , 2004 , 28, 1475-1487	4	17
154	Active Constraint Regions for Optimal Operation of Chemical Processes. <i>Industrial & Engineering Chemistry Research</i> , 2011 , 50, 11226-11236	3.9	16
153	A sensory-motor control model of animal flight explains why bats fly differently in light versus dark. <i>PLoS Biology</i> , 2015 , 13, e1002046	9.7	15
152	Small-scale experiments on stabilizing riser slug flow. <i>Chemical Engineering Research and Design</i> , 2010 , 88, 213-228	5.5	15
151	Effect of RHP zeros and poles on the sensitivity functions in multivariable systems. <i>Journal of Process Control</i> , 1998 , 8, 155-164	3.9	15
150	Opportunities and difficulties with 5 B distillation control. <i>Journal of Process Control</i> , 1995 , 5, 249-261	3.9	15
149	Robust control of time-delay systems using the Smith predictor. <i>International Journal of Control</i> , 1993 , 57, 1405-1420	1.5	15
148	Optimal controlled variables for polynomial systems. <i>Journal of Process Control</i> , 2012 , 22, 167-179	3.9	14
147	Sensitivity Analysis of Optimal Operation of an Activated Sludge Process Model for Economic Controlled Variable Selection. <i>Industrial & Engineering Chemistry Research</i> , 2013 , 52, 9908-9921	3.9	14
146	Economic Plantwide Control Over a Wide Throughput Range: A Systematic Design Procedure. <i>AIChE Journal</i> , 2013 , 59, 2407-2426	3.6	14
145	Computational performance of aggregated distillation models. <i>Computers and Chemical Engineering</i> , 2009 , 33, 296-308	4	14
144	Offset-Free Tracking of Model Predictive Control with Model Mismatch: Experimental Results. <i>Industrial & Engineering Chemistry Research</i> , 2005 , 44, 3966-3972	3.9	14
143	Consistency of steady-state models using insight about extensive variables. <i>Industrial & Engineering Chemistry Research</i> , 1991 , 30, 654-661	3.9	14
142	Evaluation of Dynamic Models of Distillation Columns with Emphasis on the Initial Response. <i>Modeling, Identification and Control</i> , 2000 , 21, 83-103	1	14
141	Simple Rules for Economic Plantwide Control. <i>Computer Aided Chemical Engineering</i> , 2015 , 37, 101-108	0.6	13
140	Feedforward Control under the Presence of Uncertainty*. <i>European Journal of Control</i> , 2004 , 10, 30-46	2.5	13
139	Closed operation of multivessel batch distillation: Experimental verification. <i>AIChE Journal</i> , 2000 , 46, 1209-1217	3.6	13

138	Chemical and Energy Process Engineering		13
137	Identification and analysis of possible splits for azeotropic mixtures. Method for column sections. <i>Chemical Engineering Science</i> , 2011 , 66, 2512-2522	4.4	12
136	Reactor/separator processes with recycles-2. Design for composition control. <i>Computers and Chemical Engineering</i> , 2003 , 27, 401-421	4	12
135	Selection of Controlled Variables for a Natural Gas to Liquids Process. <i>Industrial & Engineering Chemistry Research</i> , 2012 , 51, 10179-10190	3.9	11
134	Scaled steady state models for effective on-line applications. <i>Computers and Chemical Engineering</i> , 2008 , 32, 990-999	4	11
133	Plantwide control: Towards a systematic procedure. <i>Computer Aided Chemical Engineering</i> , 2002 , 10, 57-69	0.6	11
132	Robust control of homogeneous azeotropic distillation columns. <i>AIChE Journal</i> , 1991 , 37, 1810-1824	3.6	11
131	Anti-slug control based on a virtual flow measurement. <i>Flow Measurement and Instrumentation</i> , 2017 , 53, 299-307	2.2	10
130	Improving Scenario Decomposition for Multistage MPC Using a Sensitivity-Based Path-Following Algorithm 2018 , 2, 581-586		10
129	Simultaneous design of proportionalIntegralDerivative controller and measurement filter by optimisation. <i>IET Control Theory and Applications</i> , 2017 , 11, 341-348	2.5	10
128	Medium-Scale Experiments on Stabilizing Riser-Slug Flow. <i>SPE Projects, Facilities and Construction</i> , 2009 , 4, 156-170		10
127	Feedback Real-Time Optimization Strategy Using a Novel Steady-state Gradient Estimate and Transient Measurements. <i>Industrial & Engineering Chemistry Research</i> , 2019 , 58, 207-216	3.9	10
126	Control structure comparison for three-product Petlyuk column. <i>Chinese Journal of Chemical Engineering</i> , 2018 , 26, 1621-1630	3.2	10
125	On combining self-optimizing control and extremum-seeking control Applied to an ammonia reactor case study. <i>Journal of Process Control</i> , 2019 , 78, 78-87	3.9	9
124	Manipulation of vapour split in Kaibel distillation arrangements. <i>Chemical Engineering and Processing: Process Intensification</i> , 2013 , 72, 10-23	3.7	9
123	A simple dynamic gravity separator model for separation efficiency evaluation incorporating level and pressure control 2017 ,		9
122	Reduced distillation models via stage aggregation. <i>Chemical Engineering Science</i> , 2010 , 65, 3439-3456	4.4	9
121	Experience in Norsk Hydro with cubic equations of state. <i>Fluid Phase Equilibria</i> , 1983 , 13, 179-188	2.5	9

120	Systematic Design of Active Constraint Switching Using Classical Advanced Control Structures. <i>Industrial & Engineering Chemistry Research</i> , 2020 , 59, 2229-2241	3.9	9
119	Dividing-Wall Column for Fractionation of Natural Gas Liquids in Floating Liquefied Natural Gas Plants. <i>Chemical Engineering and Technology</i> , 2016 , 39, 2348-2354	2	9
118	Optimal Operation with Changing Active Constraint Regions using Classical Advanced Control. <i>IFAC-PapersOnLine</i> , 2018 , 51, 440-445	0.7	9
117	Online Process Optimization with Active Constraint Set Changes using Simple Control Structures. <i>Industrial & Engineering Chemistry Research</i> , 2019 , 58, 13555-13567	3.9	8
116	Anti-slug control solutions based on identified model. <i>Journal of Process Control</i> , 2015 , 30, 58-68	3.9	8
115	Optimal operation of oil and gas production using simple feedback control structures. <i>Control Engineering Practice</i> , 2019 , 91, 104107	3.9	8
114	Profitable and dynamically feasible operating point selection for constrained processes. <i>Journal of Process Control</i> , 2014 , 24, 531-541	3.9	8
113	Economic Plantwide Control 2012 , 229-251		8
112	A systematic approach to the design of buffer tanks. <i>Computers and Chemical Engineering</i> , 2000 , 24, 1395-14018		8
111	Comparison of stabilizing control structures for dividing wall columns. <i>IFAC-PapersOnLine</i> , 2016 , 49, 729-734	3.9	8
110	A Distributed Algorithm for Scenario-based Model Predictive Control using Primal Decomposition. <i>IFAC-PapersOnLine</i> , 2018 , 51, 351-356	0.7	8
109	Optimization of fixed-order controllers using exact gradients. <i>Journal of Process Control</i> , 2018 , 71, 130-138	3.9	8
108	Gas Lift Optimization under Uncertainty. <i>Computer Aided Chemical Engineering</i> , 2017 , 40, 1753-1758	0.6	7
107	Surrogate model generation using self-optimizing variables. <i>Computers and Chemical Engineering</i> , 2018 , 119, 143-151	4	7
106	Identification and analysis of possible splits for azeotropic mixtures. 2. Method for simple columns. <i>Chemical Engineering Science</i> , 2012 , 69, 159-169	4.4	7
105	Controller design for serial processes. <i>Journal of Process Control</i> , 2005 , 15, 259-271	3.9	7
104	Multiple-Input Single-Output Control for Extending the Steady-State Operating Range Use of Controllers with Different Setpoints. <i>Processes</i> , 2019 , 7, 941	2.9	7
103	A new termination criterion for sampling for surrogate model generation using partial least squares regression. <i>Computers and Chemical Engineering</i> , 2019 , 121, 75-85	4	7

102	Dynamic self-optimizing control for unconstrained batch processes. <i>Computers and Chemical Engineering</i> , 2018 , 117, 451-468	4	6
101	A Primal decomposition algorithm for distributed multistage scenario model predictive control. <i>Journal of Process Control</i> , 2019 , 81, 162-171	3.9	6
100	Systematic Design of Split Range Controllers. <i>IFAC-PapersOnLine</i> , 2019 , 52, 898-903	0.7	6
99	A New Class of Model-Based Static Estimators. <i>Industrial & Engineering Chemistry Research</i> , 2013 , 52, 12451-12462	3.9	6
98	L1/Q Approach for efficient computation of disturbance rejection measures for feedback control. <i>Journal of Process Control</i> , 2007 , 17, 501-508	3.9	6
97	Branch and bound methods for control structure design. <i>Computer Aided Chemical Engineering</i> , 2006 , 21, 1371-1376	0.6	6
96	Design and control of azeotropic dividing wall column for separating furfural-water mixture. <i>Computer Aided Chemical Engineering</i> , 2016 , 38, 409-414	0.6	6
95	Self-Optimizing Control in Chemical Recycle Processes. <i>IFAC-PapersOnLine</i> , 2018 , 51, 536-541	0.7	6
94	Virtual inflow monitoring for a three phase gravity separator 2017 ,		5
93	Systematic design of active constraint switching using selectors. <i>Computers and Chemical Engineering</i> , 2020 , 143, 107106	4	5
92	A Control- and Estimation-Oriented Gravity Separator Model for Oil and Gas Applications Based upon First-Principles. <i>Industrial & Engineering Chemistry Research</i> , 2018 , 57, 7201-7217	3.9	5
91	Optimal operation of energy storage in buildings: Use of the hot water system. <i>Journal of Energy Storage</i> , 2016 , 5, 102-112	7.8	5
90	Global Self-Optimizing Control for Uncertain Constrained Process Systems. <i>IFAC-PapersOnLine</i> , 2017 , 50, 4672-4677	0.7	5
89	Control-oriented modelling of gas-liquid cylindrical cyclones 2017 ,		5
88	Plantwide Control of a Cumene Manufacture Process. <i>Computer Aided Chemical Engineering</i> , 2011 , 29, 522-526	0.6	5
87	Experimental and Theoretical Studies on the Start-Up Operation of a Multivessel Batch Distillation Column. <i>Industrial & Engineering Chemistry Research</i> , 2009 , 48, 5336-5343	3.9	5
86	Controllability analysis of severe slugging in well-pipeline-riser systems. <i>IFAC Postprint Volumes IPPV / International Federation of Automatic Control</i> , 2012 , 45, 101-108		5
85	Optimal output selection for control of batch processes 2008 ,		5

84	Loopshaping for robust performance. <i>International Journal of Robust and Nonlinear Control</i> , 1996 , 6, 805-823	3.2	5
83	Control of Unstable Distillation Columns 1991 ,		5
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