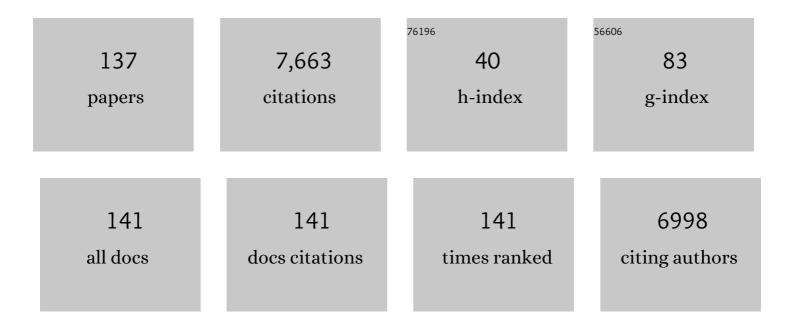
List of Publications by Year in descending order

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| # | Article | IF | CITATIONS |
|----|--|-----|-----------|
| 1 | Modulating redox metabolism to improve isobutanol production in Shimwellia blattae. Biotechnology for Biofuels, 2021, 14, 8. | 6.2 | 15 |
| 2 | Effect of additives on the enzymatic hydrolysis of pre-treated wheat straw. Brazilian Journal of Chemical Engineering, 2021, 38, 241. | 0.7 | 7 |
| 3 | Multi-feedstock lignocellulosic biorefineries based on biological processes: An overview. Industrial Crops and Products, 2021, 172, 114062. | 2.5 | 20 |
| 4 | Fluid dynamic conditions and oxygen availability effects on microbial cultures in STBR: An overview. Biochemical Engineering Journal, 2020, 164, 107803. | 1.8 | 16 |
| 5 | Enzymatic hydrolysis of several pretreated lignocellulosic biomasses: Fractal kinetic modelling. Bioresource Technology, 2020, 318, 124050. | 4.8 | 16 |
| 6 | Production of MCM-41 Nanoparticles with Control of Particle Size and Structural Properties: Optimizing Operational Conditions during Scale-Up. International Journal of Molecular Sciences, 2020, 21, 7899. | 1.8 | 26 |
| 7 | Kinetic Modeling of Dihydroxyacetone Production from Glycerol by Gluconobacter oxydans ATCC 621 Resting Cells: Effect of Fluid Dynamics Conditions. Catalysts, 2020, 10, 101. | 1.6 | 11 |
| 8 | Synthesis of Ibuprofen Monoglyceride in Solventless Medium with Novozym®435: Kinetic Analysis. Catalysts, 2020, 10, 76. | 1.6 | 7 |
| 9 | Thermal and operational deactivation of Aspergillus fumigatus β-glucosidase in ethanol/water pretreated wheat straw enzymatic hydrolysis. Journal of Biotechnology, 2019, 292, 32-38. | 1.9 | 6 |
| 10 | Effects of fluid-dynamic conditions in Shimwellia blattae (p424lbPSO) cultures in stirred tank bioreactors: Hydrodynamic stress and change of metabolic routes by oxygen availability. Biochemical Engineering Journal, 2019, 149, 107238. | 1.8 | 9 |
| 11 | Influence of oxygen transfer and uptake rates on dihydroxyacetone production from glycerol by Cluconobacter oxydans in resting cells operation. Biochemical Engineering Journal, 2019, 147, 20-28. | 1.8 | 14 |
| 12 | Orange peel waste upstream integrated processing to terpenes, phenolics, pectin and monosaccharides: Optimization approaches. Industrial Crops and Products, 2019, 134, 370-381. | 2.5 | 49 |
| 13 | Dihydroxyacetone production from glycerol using Gluconobacter oxydans : Study of medium composition and operational conditions in shaken flasks. Biotechnology Progress, 2019, 35, e2803. | 1.3 | 11 |
| 14 | Liquor re-use strategy in lignocellulosic biomass fractionation with ethanol-water mixtures. Bioresource Technology, 2019, 280, 396-403. | 4.8 | 13 |
| 15 | Kinetic Modeling of the Isobutanol Production from Glucose Using <i>Shimwellia blattae</i> (p424lbPSO) Strain: Effect of Initial Substrate Concentration. Industrial & Engineering Chemistry Research, 2019, 58, 1502-1512. | 1.8 | 4 |
| 16 | Carbon flux distribution in the metabolism of <i>Shimwellia blattae</i> (p424lbPSO) for isobutanol production from glucose as function of oxygen availability. Journal of Chemical Technology and Biotechnology, 2019, 94, 850-858. | 1.6 | 6 |
| 17 | Behavior of several <i>pseudomonas putida</i> strains growth under different agitation and oxygen supply conditions. Biotechnology Progress, 2018, 34, 900-909. | 1.3 | 8 |
| 18 | Wheat straw fractionation by ethanol-water mixture: Optimization of operating conditions and comparison with diluted sulfuric acid pre-treatment. Bioresource Technology, 2018, 256, 178-186. | 4.8 | 25 |

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| 19 | Isobutanol production by a recombinant biocatalyst Shimwellia blattae (p424lbPSO): Study of the operational conditions. Biochemical Engineering Journal, 2018, 133, 21-27. | 1.8 | 11 |
| 20 | Valorization of Cynara Cardunculus crops by ethanol-water treatment: Optimization of operating conditions. Industrial Crops and Products, 2018, 124, 856-862. | 2.5 | 20 |
| 21 | Resting cells isobutanol production byShimwellia blattae(p424lbPSO): Influence of growth culture conditions. Biotechnology Progress, 2018, 34, 1073-1080. | 1.3 | 8 |
| 22 | Pre-treatment of corn stover, Cynara cardunculus L. stems and wheat straw by ethanol-water and diluted sulfuric acid: Comparison under different energy input conditions. Bioresource Technology, 2018, 270, 449-456. | 4.8 | 21 |
| 23 | Kinetic modeling of cellobiose by a β-glucosidase from Aspergillus fumigatus. Chemical Engineering Research and Design, 2018, 136, 502-512. | 2.7 | 13 |
| 24 | Physico-chemical kinetic modelling of hydrolysis of a steam-explosion pre-treated corn stover: A two-step approach. Bioresource Technology, 2018, 268, 592-598. | 4.8 | 11 |
| 25 | Influence of fluid dynamic conditions on 1,3â€propanediol production from glycerol by <i>Shimwellia blattae</i> : carbon flux and cell response. Journal of Chemical Technology and Biotechnology, 2017, 92, 2050-2059. | 1.6 | 5 |
| 26 | Study of the enzymatic activity inhibition on the saccharification of acid pretreated corn stover. Biomass and Bioenergy, 2017, 98, 1-7. | 2.9 | 20 |
| 27 | Solventless synthesis of solketal with commercially available sulfonic acid based ion exchange resins and their catalytic performance. Green Processing and Synthesis, 2017, 6, 79-89. | 1.3 | 15 |
| 28 | Metabolic kinetic model for dibenzothiophene desulfurization through 4S pathway using intracellular compound concentrations. Biochemical Engineering Journal, 2017, 117, 89-96. | 1.8 | 12 |
| 29 | Kinetic modeling of 1,3-propanediol production from raw glycerol by Shimwellia blattae : Influence of the initial substrate concentration. Biochemical Engineering Journal, 2017, 117, 57-65. | 1.8 | 22 |
| 30 | Effect of fluid dynamic conditions on 2,3â€butanediol production by <i>Raoultella terrigena</i> in <scp>SBTR</scp> : oxygen transfer and uptake rates. Journal of Chemical Technology and Biotechnology, 2017, 92, 1266-1275. | 1.6 | 16 |
| 31 | Influence of fluid dynamic conditions on enzymatic hydrolysis of lignocellulosic biomass: Effect of mass transfer rate. Bioresource Technology, 2016, 216, 28-35. | 4.8 | 26 |
| 32 | Experimental and modelling approach to the catalytic coproduction of glycerol carbonate and ethylene glycol as a means to valorise glycerol. Journal of the Taiwan Institute of Chemical Engineers, 2016, 63, 89-100. | 2.7 | 22 |
| 33 | Enzymatic saccharification of acid pretreated corn stover: Empirical and fractal kinetic modelling. Bioresource Technology, 2016, 220, 110-116. | 4.8 | 19 |
| 34 | Enzymatic synthesis of ibuprofen monoglycerides catalyzed by free Candida antarctica lipase B in a toluene–glycerol biphasic medium. RSC Advances, 2016, 6, 69658-69669. | 1.7 | 14 |
| 35 | Influence of oxygen transfer on Pseudomonas putida effects on growth rate and biodesulfurization capacity. Bioprocess and Biosystems Engineering, 2016, 39, 545-554. | 1.7 | 21 |
| 36 | Biodesulfurization of dibenzothiophene by resting cells of <i>Pseudomonas putida</i> <scp>CECT5279</scp> : influence of the oxygen transfer rate in the scaleâ€up from shaken flask to stirred tank reactor. Journal of Chemical Technology and Biotechnology, 2016, 91, 184-189. | 1.6 | 24 |

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| 37 | 1,3-Propanediol production from glycerol with a novel biocatalyst Shimwellia blattae ATCC 33430: Operational conditions and kinetics in batch cultivations. Bioresource Technology, 2016, 200, 830-837. | 4.8 | 33 |
| 38 | Kinetics of the production of glycerol carbonate by transesterification of glycerol with dimethyl and ethylene carbonate using potassium methoxide, a highly active catalyst. Fuel Processing Technology, 2015, 138, 243-251. | 3.7 | 66 |
| 39 | Kinetic modelling of the solventless synthesis of solketal with a sulphonic ion exchange resin. Chemical Engineering Journal, 2015, 269, 194-202. | 6.6 | 66 |
| 40 | 1,3-Propanediol production by Klebsiella oxytoca NRRL-B199 from glycerol. Medium composition and operational conditions. Biotechnology Reports (Amsterdam, Netherlands), 2015, 6, 100-107. | 2.1 | 17 |
| 41 | Effect of fluiddynamic conditions on growth rate and biodesulfurization capacity of Rhodococcus erythropolis IGTS8. Biochemical Engineering Journal, 2015, 99, 138-146. | 1.8 | 18 |
| 42 | Enhancement of the biodesulfurization capacity of Pseudomonas putida CECT5279 by co-substrate addition. Process Biochemistry, 2015, 50, 119-124. | 1.8 | 42 |
| 43 | Specific oxygen uptake rate as indicator of cell response of Rhodococcus erythropolis cultures to shear effects. Chemical Engineering Science, 2015, 122, 491-499. | 1.9 | 23 |
| 44 | Phenomenological kinetic model of the synthesis of glycerol carbonate assisted by focused beam reflectance measurements. Chemical Engineering Journal, 2015, 260, 434-443. | 6.6 | 52 |
| 45 | Liquid–liquid equilibria for the systems ethylene carbonate + ethylene glycol + glycerol; ethylene carbonate + glycerol carbonate + glycerol and ethylene carbonate + ethylene glycol + glycerol carbonate + glycerol at catalytic reacting temperatures. Chemical Engineering Research and Design, 2015. 94. 440-448. | 2.7 | 13 |
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| 47 | Homogeneous catalytic esterification of glycerol with cinnamic and methoxycinnamic acids to cinnamate glycerides in solventless medium: Kinetic modeling. Chemical Engineering Journal, 2014, 247, 174-182. | 6.6 | 27 |
| 48 | Liquid–Liquid Equilibria for the System Acetone + Solketal + Glycerol at (303.2, 313.2, and 323.2) K. Journal of Chemical & Engineering Data, 2014, 59, 2850-2855. | 1.0 | 26 |
| 49 | Liquid–liquid equilibria for the ternary systems DMC–methanol–glycerol, DMC–glycerol carbonate–glycerol and the quaternary system DMC–methanol–glycerol carbonate–glycerol at catalytic reacting temperatures. Chemical Engineering Research and Design, 2014, 92, 2797-2805. | 2.7 | 29 |
| 50 | Thermal esterification of cinnamic and p-methoxycinnamic acids with glycerol to cinnamate glycerides in solventless media: A kinetic model. Chemical Engineering Journal, 2013, 225, 710-719. | 6.6 | 16 |
| 51 | The effect of hydrodynamic stress on the growth of Xanthomonas campestris cultures in a stirred and sparged tank bioreactor. Bioprocess and Biosystems Engineering, 2013, 36, 911-925. | 1.7 | 39 |
| 52 | Phenomenological kinetic modelling of the esterification of rosin and polyols. Chemical Engineering Journal, 2012, 197, 387-397. | 6.6 | 23 |
| 53 | Extended kinetic model for DBT desulfurization using Pseudomonas Putida CECT5279 in resting cells. Biochemical Engineering Journal, 2012, 66, 52-60. | 1.8 | 14 |
| 54 | Esterification of benzoic acid and glycerol to α-monobenzoate glycerol in solventless media using an industrial free Candida antarctica lipase B. Process Biochemistry, 2012, 47, 243-250. | 1.8 | 32 |

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| 55 | Kinetic modelling of the esterification of rosin and glycerol: Application to industrial operation. Chemical Engineering Journal, 2011, 169, 319-328. | 6.6 | 35 |
| 56 | Disproportionation of rosin on an industrial Pd/C catalyst: Reaction pathway and kinetic model discrimination. Bioresource Technology, 2011, 102, 3504-3511. | 4.8 | 21 |
| 57 | Mixtures of Pseudomonas putida CECT 5279 cells of different ages: Optimization as biodesulfurization catalyst. Process Biochemistry, 2011, 46, 1323-1328. | 1.8 | 25 |
| 58 | Oxygen uptake rate in microbial processes: An overview. Biochemical Engineering Journal, 2010, 49, 289-307. | 1.8 | 344 |
| 59 | Analysis of Dibenzothiophene Desulfurization in a Recombinant Pseudomonas putida Strain. Applied and Environmental Microbiology, 2009, 75, 875-877. | 1.4 | 34 |
| 60 | Bioreactor scale-up and oxygen transfer rate in microbial processes: An overview. Biotechnology Advances, 2009, 27, 153-176. | 6.0 | 1,085 |
| 61 | Biodesulfurization of Dibenzothiophene (DBT) Using Pseudomonas putida CECT 5279: A Biocatalyst Formulation Comparison. Energy & Fuels, 2009, 23, 5491-5495. | 2.5 | 32 |
| 62 | Kinetic model for DBT desulphurization by resting whole cells of Pseudomonas putida CECT5279. Biochemical Engineering Journal, 2008, 39, 486-495. | 1.8 | 17 |
| 63 | Activated carbon as catalyst in wet oxidation of phenol: Effect of the oxidation reaction on the catalyst properties and stability. Applied Catalysis B: Environmental, 2008, 81, 122-131. | 10.8 | 38 |
| 64 | Desulfurization of dibenzothiophene using the 4S enzymatic route: Influence of operational conditions on initial reaction rates. Biocatalysis and Biotransformation, 2007, 25, 286-294. | 1.1 | 6 |
| 65 | Oxidation and mineralisation of substituted phenols by Fenton's reagent and catalytic wet oxidation. Water Science and Technology, 2007, 55, 37-45. | 1.2 | 25 |
| 66 | Decolorization of Textile Dyes by Wet Oxidation Using Activated Carbon as Catalyst. Industrial & Engineering Chemistry Research, 2007, 46, 2423-2427. | 1.8 | 37 |
| 67 | Abatement of phenolic mixtures by catalytic wet oxidation enhanced by Fenton's pretreatment: Effect of H2O2 dosage and temperature. Journal of Hazardous Materials, 2007, 146, 595-601. | 6.5 | 45 |
| 68 | Hindered diffusion of proteins and polymethacrylates in controlled-pore glass: An experimental approach. Chemical Engineering Science, 2007, 62, 666-678. | 1.9 | 10 |
| 69 | Oxygen-Uptake and Mass-Transfer Rates on the Growth ofPseudomonasputidaCECT5279:  Influence on Biodesulfurization (BDS) Capability. Energy & Fuels, 2006, 20, 1565-1571. | 2.5 | 47 |
| 70 | Kinetic modelling of the thermal inactivation of an industrial β-galactosidase from Kluyveromyces fragilis. Enzyme and Microbial Technology, 2006, 38, 1-9. | 1.6 | 40 |
| 71 | Oxygen transport rate on Rhodococcus erythropolis cultures: Effect on growth and BDS capability. Chemical Engineering Science, 2006, 61, 4595-4604. | 1.9 | 33 |
| 72 | Thermal and pH inactivation of an immobilized thermostable β-galactosidase from Thermus sp. strain T2: Comparison to the free enzyme. Biochemical Engineering Journal, 2006, 31, 14-24. | 1.8 | 50 |

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| 74 | Reaction network and kinetic modeling of wet oxidation of phenol catalyzed by activated carbon. Chemical Engineering Science, 2006, 61, 2457-2467. | 1.9 | 55 |
| 75 | Wet oxidation of phenol, cresols and nitrophenols catalyzed by activated carbon in acid and basic media. Applied Catalysis B: Environmental, 2006, 65, 269-281. | 10.8 | 75 |
| 76 | Phenotypic Characterization of <i>DFNA24</i> : Prelingual Progressive Sensorineural Hearing Impairment. Audiology and Neuro-Otology, 2006, 11, 269-275. | 0.6 | 3 |
| 77 | Modeling the production of a Rhodococcus erythropolis IGTS8 biocatalyst for DBT biodesulfurization: Influence of media composition. Enzyme and Microbial Technology, 2005, 37, 157-166. | 1.6 | 55 |
| 78 | Kinetic modelling of the thermal and pH inactivation of a thermostable β-galactosidase from Thermus sp. strain T2. Enzyme and Microbial Technology, 2005, 37, 505-513. | 1.6 | 26 |
| 79 | Catalytic wet oxidation of phenol on active carbon: stability, phenol conversion and mineralization. Catalysis Today, 2005, 102-103, 213-218. | 2.2 | 55 |
| 80 | Kinetic model of wet oxidation of phenol at basic pH using a copper catalyst. Chemical Engineering Science, 2005, 60, 4866-4878. | 1.9 | 27 |
| 81 | Production of a Rhodococcus erythropolis IGTS8 biocatalyst for DBT biodesulfurization: influence of operational conditions. Biochemical Engineering Journal, 2005, 22, 229-237. | 1.8 | 67 |
| 82 | Biodesulfurisation of DBT with Pseudomonas putida CECT5279 by resting cells: Influence of cell growth time on reducing equivalent concentration and HpaC activity. Biochemical Engineering Journal, 2005, 26, 168-175. | 1.8 | 40 |
| 83 | Study of the copper leaching in the wet oxidation of phenol with CuO-based catalysts: Causes and effects. Applied Catalysis B: Environmental, 2005, 61, 323-333. | 10.8 | 139 |
| 84 | Prediction of gas-liquid mass transfer coefficient in sparged stirred tank bioreactors. Biotechnology and Bioengineering, 2005, 92, 761-772. | 1.7 | 79 |
| 85 | Influence of pH on the wet oxidation of phenol with copper catalyst. Topics in Catalysis, 2005, 33, 181-192. | 1.3 | 38 |
| 86 | Generalized Kinetic Model for the Catalytic Wet Oxidation of Phenol Using Activated Carbon as the Catalyst. Industrial & Engineering Chemistry Research, 2005, 44, 3869-3878. | 1.8 | 23 |
| 87 | Production of a Biocatalyst ofPseudomonas putidaCECT5279 for DBT Biodesulfurization:  Influence of the Operational Conditions. Energy & Fuels, 2005, 19, 775-782. | 2.5 | 52 |
| 88 | Lower toxicity route in catalytic wet oxidation of phenol at basic pH by using bicarbonate media. Applied Catalysis B: Environmental, 2004, 53, 181-194. | 10.8 | 37 |
| 89 | Theoretical prediction of gas–liquid mass transfer coefficient, specific area and hold-up in sparged stirred tanks. Chemical Engineering Science, 2004, 59, 2489-2501. | 1.9 | 150 |
| 90 | Structured kinetic model for Xanthomonas campestris growth. Enzyme and Microbial Technology, 2004, 34, 583-594. | 1.6 | 10 |

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| 91 | Use of flow cytometry for growth structured kinetic model development. Enzyme and Microbial Technology, 2004, 34, 399-406. | 1.6 | 16 |
| 92 | Chemical structured kinetic model for xanthan production. Enzyme and Microbial Technology, 2004, 35, 284-292. | 1.6 | 27 |
| 93 | Production of a Biocatalyst of Pseudomonas putida CECT5279 for Dibenzothiophene (DBT) Biodesulfurization for Different Media Compositions. Energy & Fuels, 2004, 18, 851-857. | 2.5 | 55 |
| 94 | Evolution of Toxicity upon Wet Catalytic Oxidation of Phenol. Environmental Science & Technology, 2004, 38, 133-138. | 4.6 | 148 |
| 95 | Hydrolysis of lactose by free and immobilized ?-galactosidase from Thermus sp. strain T2. Biotechnology and Bioengineering, 2003, 81, 241-252. | 1.7 | 41 |
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| 97 | Studies on the activity and the stability of β-galactosidases from Thermus sp strain T2 and from Kluyveromyces fragilis. Enzyme and Microbial Technology, 2002, 30, 392-405. | 1.6 | 61 |
| 98 | Catalytic Wet Oxidation of Phenol:Â Kinetics of Phenol Uptake. Environmental Science & Technology, 2001, 35, 2828-2835. | 4.6 | 32 |
| 99 | Catalytic Wet Oxidation of Phenol:Â Kinetics of the Mineralization Rate. Industrial & Engineering Chemistry Research, 2001, 40, 2773-2781. | 1.8 | 36 |
| 100 | Oxidation of hardwood kraft-lignin to phenolic derivatives with oxygen as oxidant. Wood Science and Technology, 2001, 35, 245-255. | 1.4 | 168 |
| 101 | Estimation of oxygen mass transfer coefficient in stirred tank reactors using artificial neural networks. Enzyme and Microbial Technology, 2001, 28, 560-569. | 1.6 | 39 |
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| 103 | Oxidation of phenol in aqueous solution with copper catalysts. Catalysis Today, 2001, 66, 511-517. | 2.2 | 28 |
| 104 | Viscosity of guar gum and xanthan/guar gum mixture solutions. Journal of the Science of Food and Agriculture, 2000, 80, 1722-1727. | 1.7 | 163 |
| 105 | Kinetic modeling of lactose hydrolysis with an immobilized β-galactosidase from Kluyveromyces fragilis. Enzyme and Microbial Technology, 2000, 27, 583-592. | 1.6 | 83 |
| 106 | Oxygen transfer and uptake rates during xanthan gum production. Enzyme and Microbial Technology, 2000, 27, 680-690. | 1.6 | 151 |
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| 108 | Xanthan gum: production, recovery, and properties. Biotechnology Advances, 2000, 18, 549-579. | 6.0 | 1,166 |

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| 111 | Unstructured kinetic model for sophorolipid production by Candida bombicola. Enzyme and Microbial Technology, 1999, 25, 613-621. | 1.6 | 41 |
| 112 | Overall rate of aqueous-phase catalytic oxidation of phenol: pH and catalyst loading influences. Catalysis Today, 1999, 48, 109-117. | 2.2 | 34 |
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| 114 | Sophorolipid production by Candida bombicola: Medium composition and culture methods. Journal of Bioscience and Bioengineering, 1999, 88, 488-494. | 1.1 | 131 |
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| 116 | Kinetics ofEucalyptus globulusDelignification in a Methanolâ^'Water Medium. Industrial & Engineering Chemistry Research, 1999, 38, 3324-3332. | 1.8 | 26 |
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| 118 | Intracellular compounds quantification by means of flow cytometry in bacteria: Application to xanthan production byXanthomonas campestris. , 1998, 57, 87-94. | | 13 |
| 119 | Kinetic Modeling of Lactose Hydrolysis by a β-Galactosidase from Kluyveromices Fragilis. Enzyme and Microbial Technology, 1998, 22, 558-567. | 1.6 | 101 |
| 120 | Metabolic structured kinetic model for xanthan production. Enzyme and Microbial Technology, 1998, 23, 75-82. | 1.6 | 37 |
| 121 | Mass transfer coefficient in stirred tank reactors for xanthan gum solutions. Biochemical Engineering Journal, 1998, 1, 1-10. | 1.8 | 104 |
| 122 | Oxidation of Hardwood Kraft-Lignin to Phenolic Derivatives. Nitrobenzene and Copper Oxide as Oxidants. Journal of Wood Chemistry and Technology, 1997, 17, 259-285. | 0.9 | 62 |
| 123 | Kinetic Modeling of Kraft Delignification ofEucalyptus globulus. Industrial & Engineering Chemistry Research, 1997, 36, 4114-4125. | 1.8 | 40 |
| 124 | Optimization of a synthetic medium for Candida bombicola growth using factorial design of experiments. Enzyme and Microbial Technology, 1997, 21, 221-229. | 1.6 | 42 |
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| 127 | Effective diffusivity under inert and reaction conditions. Chemical Engineering Science, 1994, 49, 3091-3102. | 1.9 | 22 |
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| 131 | Modeling of the liquid-phase n-octane oxidation catalyzed by cobalt. Industrial & Engineering Chemistry Research, 1990, 29, 1989-1994. | 1.8 | 11 |
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| 137 | Analysis of the impurities in industrial É≻-caprolactam. Hypothesis of formation. Journal of Applied Polymer Science, 1981, 26, 3271-3282. | 1.3 | 23 |