

Jietae Lee

List of Publications by Year in descending order

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86
papers

944
citations

516215

16
h-index

500791

28
g-index

87
all docs

87
docs citations

87
times ranked

407
citing authors

#	ARTICLE	IF	CITATIONS
1	Real-time optimization for nonlinear processes including output saturation. Asia-Pacific Journal of Chemical Engineering, 2021, 16, e2603.	0.8	0
2	Analytic Pade-like approximations of $\exp(\sqrt{s})$ for simulations of diffusion processes in the semi-infinite geometry. Chemical Engineering Communications, 2020, 207, 194-202.	1.5	0
3	Shape factor for the relay feedback autotuning. Indian Chemical Engineer, 2020, , 1-15.	0.9	0
4	Real-Time Optimization of a CO Preferential Oxidation Reactor Temperature with Extremum Seeking Control Techniques. ACS Omega, 2020, 5, 13822-13828.	1.6	2
5	Minimized Test Times for Step and Pulse Responses of Slow Linear Processes. Industrial & Engineering Chemistry Research, 2019, 58, 12116-12123.	1.8	0
6	Full Closed-Loop Tests for the Relay Feedback Autotuning of Stable, Integrating, and Unstable Processes. ACS Omega, 2019, 4, 18760-18770.	1.6	8
7	Simple Proportional Integral Controller Tuning Rules for FOPTD and HOPTD Models Based on Matching Two Asymptotes. Industrial & Engineering Chemistry Research, 2018, 57, 2905-2916.	1.8	6
8	Three-Parameter Models for Conservative Relay Feedback Autotuning. , 2018, , .		1
9	Half order plus time delay (HOPTD) models to tune PI controllers. AIChE Journal, 2017, 63, 601-609.	1.8	9
10	Double First-Order Plus Time Delay Models To Tune Proportional-Integral Controllers. Industrial & Engineering Chemistry Research, 2016, 55, 10328-10335.	1.8	1
11	Extremum seeking control using a partial sum of input-output product. Korean Journal of Chemical Engineering, 2016, 33, 3079-3084.	1.2	1
12	Globally stable control systems for processes with input multiplicities. Korean Journal of Chemical Engineering, 2016, 33, 416-422.	1.2	4
13	An improved linear formula for cyclic adsorption, diffusion and reaction in a catalyst. Korean Journal of Chemical Engineering, 2016, 33, 1186-1191.	1.2	1
14	Stability Margin Interpretation of the SIMC Tuning Rule for PI Controllers and its Applications. IFAC-PapersOnLine, 2015, 48, 1186-1191.	0.5	4
15	n-Propanol aqueous solution shows nonlinearity in liquid level depending on water proportion. , 2015, , .		0
16	Wiener Model and Extremum Seeking Control for a CO Preferential Oxidation Reactor with the CuO-CeO ₂ catalyst. IFAC-PapersOnLine, 2015, 48, 574-579.	0.5	4
17	Nonlinear PI controllers with output transformations. AIChE Journal, 2015, 61, 4264-4269.	1.8	0
18	The control of pH neutralization process in the large scale reactor. , 2015, , .		3

#	ARTICLE	IF	CITATIONS
19	Optimization of hysteresis on the liquid level system and hysteresis process implemented with siphon in the liquid level system. , 2015, , .		0
20	A frequency response identification method for discrete-time processes with cyclic steady state conditions. Automatica, 2014, 50, 3260-3267.	3.0	8
21	Simple Analytic PID Controller Tuning Rules Revisited. Industrial & Engineering Chemistry Research, 2014, 53, 5038-5047.	1.8	67
22	Simple Analytic Proportional-Integral-Derivative (PID) Controller Tuning Rules for Unstable Processes. Industrial & Engineering Chemistry Research, 2014, 53, 5048-5054.	1.8	46
23	In-line mixer pH system for the identification of titration curve. International Journal of Control, Automation and Systems, 2013, 11, 442-449.	1.6	2
24	Slow drift modeling and compensation in the glass electrode dynamics for the fast measurement of pH. Korean Journal of Chemical Engineering, 2013, 30, 1008-1012.	1.2	2
25	Temperature oscillations in methanol partial oxidation reactor for the production of hydrogen. Korean Journal of Chemical Engineering, 2013, 30, 790-795.	1.2	7
26	Global approximations of unsteady-state adsorption, diffusion, and reaction in a porous catalyst. AIChE Journal, 2013, 59, 2540-2548.	1.8	9
27	Web cam for easy-monitoring of the growth of organisms. , 2013, , .		1
28	Preferential CO oxidation over CuO/CeO ₂ in excess hydrogen: Effectiveness factors of catalyst particles and temperature window for CO removal. International Journal of Hydrogen Energy, 2013, 38, 4429-4436.	3.8	14
29	Multiple switching relays for the estimation of ultimate data. International Journal of Control, Automation and Systems, 2011, 9, 294-300.	1.6	3
30	Third quadrant Nyquist point for the relay feedback autotuning of PI controllers. Korean Journal of Chemical Engineering, 2011, 28, 342-347.	1.2	6
31	Process identification method using relay feedback and backward integrals. Korean Journal of Chemical Engineering, 2011, 28, 2116-2121.	1.2	3
32	Fractional order integrator for the relay feedback identification of a process Nyquist point in the third quadrant. Korean Journal of Chemical Engineering, 2011, 28, 2227-2229.	1.2	4
33	Relay feedback identification for processes under drift and noisy environments. AIChE Journal, 2011, 57, 1809-1816.	1.8	12
34	A half-order approximation for the adsorption dynamics in a porous particle. AIChE Journal, 2011, 57, 2282-2286.	1.8	1
35	Improved frequency response model identification method for processes with initial cyclic steady-state. AIChE Journal, 2011, 57, 3429-3435.	1.8	12
36	10.2478/s11814-009-0155-1. , 2011, 26, 925.		0

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37	Relay feedback method for processes under noisy environments. <i>AIChE Journal</i> , 2010, 56, 560-562.	1.8	4
38	Dynamics study for oscillatory temperature in methanol partial oxidation. , 2010, , .		1
39	Improved Fourier transform for processes with initial cyclicâ€steadyâ€state. <i>AIChE Journal</i> , 2010, 56, 1536-1544.	1.8	7
40	Area Method for a Biased Relay Feedback System. <i>Industrial & Engineering Chemistry Research</i> , 2010, 49, 8016-8020.	1.8	2
41	Area Methods for Relay Feedback Tests. <i>Industrial & Engineering Chemistry Research</i> , 2010, 49, 7807-7813.	1.8	8
42	Iterative identification of temperature dynamics in single wafer rapid thermal processing. <i>Korean Journal of Chemical Engineering</i> , 2009, 26, 307-312.	1.2	2
43	Process systems engineering approaches to speed-up the auto-titrator operations. <i>Korean Journal of Chemical Engineering</i> , 2009, 26, 636-640.	1.2	9
44	Improved fourier transform to estimate frequency responses. <i>Korean Journal of Chemical Engineering</i> , 2009, 26, 925-929.	1.2	4
45	An upper bound of structured singular value. <i>International Journal of Control, Automation and Systems</i> , 2009, 7, 848-851.	1.6	3
46	Sequential relay autotuning method for the temperature control of multizone heated rollers. <i>International Journal of Control, Automation and Systems</i> , 2009, 7, 918-921.	1.6	0
47	Improving Dynamics of Glass pH Electrodes. <i>IEEE Sensors Journal</i> , 2009, 9, 1793-1796.	2.4	3
48	Improved system identification method for Hammerstein-Wiener processes. <i>Korean Journal of Chemical Engineering</i> , 2008, 25, 631-636.	1.2	12
49	Enhanced frequency response estimator to guarantee pre-specified phase angle and static disturbance rejection with all harmonics removed. <i>Korean Journal of Chemical Engineering</i> , 2008, 25, 1273-1278.	1.2	3
50	Temperature control of multizone heated rollers. , 2008, , .		3
51	Speed-up of the auto-titrator operation. , 2008, , .		0
52	Nonlinear Model Identification for Temperature Control in Single Wafer Rapid Thermal Processing. <i>Industrial & Engineering Chemistry Research</i> , 2008, 47, 4791-4796.	1.8	13
53	Iterative identification of temperature dynamics in single wafer rapid thermal processing. , 2007, , .		0
54	Integrals of relay feedback responses for extracting process information. <i>AIChE Journal</i> , 2007, 53, 2329-2338.	1.8	45

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55	Computation of multiloop controllers having desired closed-loop responses. Korean Journal of Chemical Engineering, 2007, 24, 562-566.	1.2	1
56	Two-Channel Relay Feedback Method under Static Disturbances. Industrial & Engineering Chemistry Research, 2006, 45, 4071-4074.	1.8	21
57	Modeling of Hammerstein~Wiener Processes with Special Input Test Signals. Industrial & Engineering Chemistry Research, 2006, 45, 1029-1038.	1.8	39
58	Step and pulse response methods for identification of wiener processes. AIChE Journal, 2006, 52, 668-677.	1.8	14
59	A simple formula for estimation of the effectiveness factor in porous catalysts. AIChE Journal, 2006, 52, 3631-3635.	1.8	5
60	Integrals of Relay Feedback Responses. , 2006, , .		0
61	Static decouplers for control of multivariable processes. AIChE Journal, 2005, 51, 2712-2720.	1.8	53
62	Continuation Method for the Modified Ziegler~Nichols Tuning of Multiloop Control Systems. Industrial & Engineering Chemistry Research, 2005, 44, 7428-7434.	1.8	8
63	Analytic Expressions of Ultimate Gains and Ultimate Periods with Phase~Optimal Approximations of Time Delays. Canadian Journal of Chemical Engineering, 2005, 83, 990-995.	0.9	6
64	Analytical design of multiloop PID controllers for desired closed-loop responses. AIChE Journal, 2004, 50, 1631-1635.	1.8	58
65	Relay Feedback Approaches for the Identification of Hammerstein-Type Nonlinear Processes. Industrial & Engineering Chemistry Research, 2004, 43, 735-740.	1.8	15
66	Dynamic Interaction Measures for Decentralized Control of Multivariable Processes. Industrial & Engineering Chemistry Research, 2004, 43, 283-287.	1.8	23
67	Two-Step IMC~PID Method for Multiloop Control System Design. Industrial & Engineering Chemistry Research, 2002, 41, 3037-3041.	1.8	16
68	Subspace identification method for simulation of closed-loop systems with time delays. AIChE Journal, 2002, 48, 417-420.	1.8	5
69	Improved PI controller with delayed or filtered integral mode. AIChE Journal, 2002, 48, 2844-2850.	1.8	14
70	Adaptive Slow/Fast Control Systems for Some Interacting Multivariable Processes. Industrial & Engineering Chemistry Research, 2001, 40, 5929-5934.	1.8	0
71	Approximation of the optimal minimum-phase output for control of nonlinear nonminimum-phase processes. Korean Journal of Chemical Engineering, 2000, 17, 559-563.	1.2	0
72	High-order approximations for noncyclic and cyclic adsorption in a biporous adsorbent. Korean Journal of Chemical Engineering, 1999, 16, 69-74.	1.2	21

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73	One-Parameter Method for a Multiloop Control System Design. Industrial & Engineering Chemistry Research, 1999, 38, 1580-1588.	1.8	31
74	Parallel Compensation with a Secondary Measurement. Industrial & Engineering Chemistry Research, 1999, 38, 1575-1579.	1.8	3
75	Effects of Diagonal Input Uncertainties and Element Uncertainties in Ill-Conditioned Processes. Industrial & Engineering Chemistry Research, 1998, 37, 1009-1017.	1.8	5
76	Iterative Identification Methods for Ill-Conditioned Processes. Industrial & Engineering Chemistry Research, 1998, 37, 1018-1023.	1.8	9
77	Steady State Structural Analysis and Interaction Characterization for Multivariable Control Systems. Industrial & Engineering Chemistry Research, 1997, 36, 3718-3726.	1.8	12
78	Automatic Tuning of PID Controller Using Second-Order Plus Time Delay Model.. Journal of Chemical Engineering of Japan, 1996, 29, 990-999.	0.3	59
79	Comparison of two identification methods for PID controller tuning. AIChE Journal, 1993, 39, 695-697.	1.8	27
80	Relay feedback method for tuning of nonlinear pH control systems. AIChE Journal, 1993, 39, 1093-1096.	1.8	23
81	Cheap control for a class of non-linear systems. International Journal of Control, 1990, 51, 289-300.	1.2	0
82	An improved technique for PID controller tuning from closed-loop tests. AIChE Journal, 1990, 36, 1891-1895.	1.8	43
83	On-line PID controller tuning from a single, closed-loop test. AIChE Journal, 1989, 35, 329-331.	1.8	54
84	A computational method for infinite-time optimal regulation problems. IEEE Transactions on Automatic Control, 1986, 31, 1146-1149.	3.6	0
85	A note on a computer-aided root-locus method. IEEE Transactions on Automatic Control, 1986, 31, 246-247.	3.6	5
86	Interaction measure for decentralized control of multivariable processes. , 0, , .		14