List of Publications by Year in descending order

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#	Article	IF	CITATIONS
1	Fluid phase equilibria for the CO2 +Â2,3-dimethylbutane binary system from 291.9ÂK to 373.1ÂK. Journal of Supercritical Fluids, 2022, 179, 105387.	1.6	6
2	Use of 300,000 pseudoâ€experimental data over 1800 pure fluids to assess the performance of four cubic equations of state: <scp>SRK</scp> , <scp>R</scp> , <scp><i>tc</i>â€RK</scp> , and <scp><i>tc</i>â€PR</scp> . AICHE Journal, 2022, 68, e17518.	1.8	16
3	The impressive impact of including enthalpy and heat capacity of mixing data when parameterising equations of state. Application to the development of the E-PPR78 (Enhanced-Predictive-Peng-Robinson-78) model Fluid Phase Equilibria, 2022, 560, 113456.	1.4	9
4	Assessing the performance of nonâ€associating <scp>SAFT</scp> â€type equations of state to reproduce vapor pressure, liquid density, enthalpy of vaporization, and liquid heat capacity data of 1800 pure fluids. AICHE Journal, 2022, 68, .	1.8	13
5	High-Pressure Phase Equilibria Measurements of the Carbon Dioxide + Cycloheptane Binary System. Journal of Chemical & Engineering Data, 2022, 67, 176-181.	1.0	2
6	A comparative study of COSMO-based and equation-of-state approaches for the prediction of solvation energies based on the compsol databank. Fluid Phase Equilibria, 2022, 561, 113540.	1.4	2
7	Development and characterization of electrospun curcumin-loaded antimicrobial nanofibrous membranes. Textile Reseach Journal, 2021, 91, 1478-1485.	1.1	6
8	Good reporting practice for thermophysical and thermochemical property measurements (IUPAC) Tj ETQq0 0 0 r	gBT /Overl	ock 10 Tf 50 24
9	Thermo-chemical engines: Unexploited high-potential energy converters. Energy Conversion and Management, 2021, 229, 113685.	4.4	10
10	SAFT and cubic EoS: Type of deviation from ideality naturally predicted in the absence of BIPs. Application to the modelling of athermal mixtures. Fluid Phase Equilibria, 2021, 533, 112924.	1.4	10
11	Development of a Detailed Kinetic Model for the Oxidation of <i>n</i> -Butane in the Liquid Phase. Journal of Physical Chemistry B, 2021, 125, 6955-6967.	1.2	8
12	Assessment of the Perturbed Chain-Statistical Associating Fluid Theory Equation of State against a Benchmark Database of High-Quality Binary-System Data. Industrial & Engineering Chemistry Research, 2021, 60, 8935-8946.	1.8	20
	Experimental determination and modelling of high-pressure phase behavior for the high-system CO2		

13	Experimental determination and modelling of high-pressure phase behavior for the binary system CO2 +Âcyclooctane. Journal of Supercritical Fluids, 2021, 174, 105249.	1.6	2
14	Design of Promising Working Fluids for Emergent Combined Cooling, Heating, and Power (CCHP) Systems. ACS Sustainable Chemistry and Engineering, 2021, 9, 11807-11824.	3.2	6
15	Assessment of organic Rankine cycle configurations for solar polygeneration orientated to electricity production and desalination. Applied Thermal Engineering, 2021, 195, 116983.	3.0	13
16	Revisiting the Entropy-Scaling Concept for Shear-Viscosity Estimation from Cubic and SAFT Equations of State: Application to Pure Fluids in Gas, Liquid and Supercritical States. Industrial & Engineering Chemistry Research, 2021, 60, 12719-12739.	1.8	26
17	Phase equilibria of mixtures involving fatty acid ethyl esters and fat alcohols between 4 and 27ÅkPa for bioproduct production. Fuel, 2021, 306, 121304.	3.4	2
18	What Is the Optimal Activity Coefficient Model To Be Combined with the <i>translated</i> – <i>consistent</i> Peng–Robinson Equation of State through Advanced Mixing Rules? Cross-Comparison and Grading of the Wilson, UNIQUAC, and NRTL <i>a</i> ^E Models against a Benchmark Database Involving 200 Binary Systems. Industrial & Engineering Chemistry Research, 2021, 60, 17228-17247.	1.8	12

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19	Note on the inconsistent definition assigned in the literature to the heat capacity of the so-called "equilibrium hydrogen―mixture. Fluid Phase Equilibria, 2020, 504, 112325.	1.4	4
20	4-Chloro-2-nitroaniline Solubility in Several Pure Solvents: Determination, Modeling, and Solvent Effect Analysis. Journal of Chemical & Engineering Data, 2020, 65, 222-232.	1.0	18
21	Benchmark Database Containing Binary-System-High-Quality-Certified Data for Cross-Comparing Thermodynamic Models and Assessing Their Accuracy. Industrial & Engineering Chemistry Research, 2020, 59, 14981-15027.	1.8	32
22	Parameterization of SAFT Models: Analysis of Different Parameter Estimation Strategies and Application to the Development of a Comprehensive Database of PC-SAFT Molecular Parameters. Journal of Chemical & Engineering Data, 2020, 65, 5920-5932.	1.0	20
23	Search for the optimal expression of the volumetric dependence of the attractive contribution in cubic equations of state. Fluid Phase Equilibria, 2020, 522, 112750.	1.4	16
24	A Predictive Equation of State to Perform an Extending Screening of Working Fluids for Power and Refrigeration Cycles. , 2020, , .		0
25	Accurate quantum-corrected cubic equations of state for helium, neon, hydrogen, deuterium and their mixtures. Fluid Phase Equilibria, 2020, 524, 112790.	1.4	14
26	A new technique for the synthesis of lanthanum substituted nickel cobaltite nanocomposites for the photo catalytic degradation of organic dyes in wastewater. Arabian Journal of Chemistry, 2020, 13, 6341-6347.	2.3	6
27	Vapor–Liquid Equilibria of the CH ₄ + CO ₂ + H ₂ S Ternary System with Two Different Global Compositions: Experiments and Modeling. Journal of Chemical & Engineering Data, 2020, 65, 1802-1813.	1.0	8
28	Thermophysical properties of switchable-hydrophilicity solvent systems: N,N-Dipropyl-1-propanamine, water and carbon dioxide. Journal of Chemical Thermodynamics, 2020, 143, 106049.	1.0	1
29	Stationary gas turbines: an exergetic approach to part load operation. Oil and Gas Science and Technology, 2020, 75, 10.	1.4	0
30	Modelling of multi-component droplet evaporation under cryogenic conditions. Oil and Gas Science and Technology, 2020, 75, 81.	1.4	3
31	Taking Another Look at the van der Waals Equation of State–Almost 150 Years Later. Journal of Chemical & Engineering Data, 2019, 64, 4619-4637.	1.0	48
32	<i>I</i> -PC-SAFT: An Industrialized Version of the Volume-Translated PC-SAFT Equation of State for Pure Components, Resulting from Experience Acquired All through the Years on the Parameterization of SAFT-Type and Cubic Models. Industrial & Engineering Chemistry Research, 2019, 58, 20815-20827.	1.8	44
33	Exergetic analysis of an LPG production plant using HYSYS software. Energy Procedia, 2019, 157, 1385-1390.	1.8	9
34	From ethyl biodiesel to biolubricants: Options for an Indian mustard integrated biorefinery toward a green and circular economy. Industrial Crops and Products, 2019, 137, 597-614.	2.5	30
35	Application of the Corresponding-State Law to the Parametrization of Statistical Associating Fluid Theory (SAFT)-Type Models: Generation and Use of "Generalized Charts― Industrial & Engineering Chemistry Research, 2019, 58, 9127-9139.	1.8	13
36	Can we safely predict solvation Gibbs energies of pure and mixed solutes with a cubic equation of state?. Pure and Applied Chemistry, 2019, 91, 1295-1307.	0.9	7

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37	Updated versions of the generalized Soave α-function suitable for the Redlich-Kwong and Peng-Robinson equations of state. Fluid Phase Equilibria, 2019, 485, 264-269.	1.4	58
38	A thermal and thermodynamic code for the computation of Boil-Off Gas – Industrial applications of LNG carrier. Cryogenics, 2019, 99, 105-113.	0.9	30
39	Sizing and operating units for the purification and compression of CO2-based streams: The impact of thermodynamic model accuracy. Journal of Supercritical Fluids, 2018, 140, 336-347.	1.6	7
40	Thermodynamic study of binary systems containing sulphur dioxide and nitric oxide: Measurements and modelling. Fluid Phase Equilibria, 2018, 461, 84-100.	1.4	7
41	Modelling the thermodynamics of air-component mixtures (N2, O2 and Ar): Comparison and performance analysis of available models. Fluid Phase Equilibria, 2018, 458, 278-287.	1.4	5
42	Densities, Apparent Molar Volume, Expansivities, Hepler's Constant, and Isobaric Thermal Expansion Coefficients of the Binary Mixtures of Piperazine with Water, Methanol, and Acetone at <i>T</i> = 293.15 to 328.15 K. International Journal of Chemical Engineering, 2018, 2018, 1-10.	1.4	15
43	Inert and Reactive Working Fluids for Closed Power Cycles: Present Knowledge, Applications and Open Researches. , 2018, , .		1
44	Analysis of the Combinations of Property Data That Are Suitable for a Safe Estimation of Consistent Twu α-Function Parameters: Updated Parameter Values for the Translated-Consistent <i>tc</i> -PR and <i>tc</i> -RK Cubic Equations of State. Journal of Chemical & Engineering Data, 2018, 63, 3980-3988.	1.0	32
45	Superstructure optimization (MINLP) within ProSimPlus Simulator. Computer Aided Chemical Engineering, 2018, , 767-772.	0.3	1
46	Measurement and prediction of multi-property data of CO2-N2-O2-CH4 mixtures with the "Peng-RobinsonÂ+Âresidual Helmholtz energy-based―model. Fluid Phase Equilibria, 2017, 437, 166-180.	1.4	16
47	Optimizing Thermodynamic Models: The Relevance of Molar Fraction Uncertainties. Journal of Chemical & Engineering Data, 2017, 62, 825-832.	1.0	9
48	Modeling the Thermodynamics of Fluids Treated by CO ₂ Capture Processes with Peng–Robinson + Residual Helmholtz Energy-Based Mixing Rules. Industrial & Engineering Chemistry Research, 2017, 56, 2259-2276.	1.8	17
49	Phase equilibrium data and modeling of ethylic biodiesel, with application to a non-edible vegetable oil. Fuel, 2017, 203, 633-641.	3.4	9
50	On the imperative need to use a consistent \hat{I}_{\pm} -function for the prediction of pure-compound supercritical properties with a cubic equation of state. Fluid Phase Equilibria, 2017, 445, 45-53.	1.4	70
51	Selection of a Proper Equation of State for the Modeling of a Supercritical CO ₂ Brayton Cycle: Consequences on the Process Design. Industrial & Engineering Chemistry Research, 2017, 56, 6841-6853.	1.8	24
52	E -PPR78: A proper cubic EoS for modelling fluids involved in the design and operation of carbon dioxide capture and storage (CCS) processes. International Journal of Greenhouse Gas Control, 2017, 56, 126-154.	2.3	44
53	Estimation of Solvation Quantities from Experimental Thermodynamic Data: Development of the Comprehensive CompSol Databank for Pure and Mixed Solutes. Journal of Physical and Chemical Reference Data, 2017, 46, .	1.9	39
54	Simulations of the Impact of Co-injected Gases on CO2 Storage, the SIGARRR Project: Processes and Geochemical Approaches for Gas-water-Salt Interactions Modeling. Energy Procedia, 2017, 114, 3322-3334.	1.8	5

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55	The design of CO 2 -based working fluids for high-temperature heat source power cycles. Energy Procedia, 2017, 129, 947-954.	1.8	8
56	Solubility and freezing point depression (FPD) measurements of Na-1-ethanethiolate, Na-1-propanethiolate, Na-2-propanethiolate, Na-1-butanethiolate, and Na-2-methyl-2-propanethiolate salts in pure water. Chemical Engineering Communications, 2017, 204, 1225-1236.	1.5	0
57	Prediction of Thermodynamic Properties of Alkyne-Containing Mixtures with the <i>E</i> -PPR78 Model. Industrial & Engineering Chemistry Research, 2017, 56, 8143-8157.	1.8	28
58	Phase equilibrium of CCS mixtures: Equation of state modeling and Monte Carlo simulation. Journal of Supercritical Fluids, 2017, 119, 169-202.	1.6	26
59	Fluid-phase-equilibrium prediction of fluorocompound-containing binary systems with the predictive E -PPR78 model. International Journal of Refrigeration, 2017, 73, 65-90.	1.8	36
60	Teaching the Concept of Gibbs Energy Minimization through Its Application to Phase-Equilibrium Calculation. Journal of Chemical Education, 2016, 93, 1569-1577.	1.1	10
61	Editor's Preface for the Special Issue Dedicated to the 2015 JETC. International Journal of Thermophysics, 2016, 37, 1.	1.0	0
62	Incorporation of a volume translation in an equation of state for fluid mixtures: which combining rule? which effect on properties of mixing?. Fluid Phase Equilibria, 2016, 427, 414-420.	1.4	63
63	A consistency test for α-functions of cubic equations of state. Fluid Phase Equilibria, 2016, 427, 513-538.	1.4	116
64	Development of the translated-consistent tc-PR and tc-RK cubic equations of state for a safe and accurate prediction of volumetric, energetic and saturation properties of pure compounds in the sub- and super-critical domains. Fluid Phase Equilibria, 2016, 429, 301-312.	1.4	107
65	Application of PPR78 Thermodynamic Framework as a Fill Method with a Semiempirical Mixing Rule for Mixtures Involved in Gas Processing. Journal of Chemical & Engineering Data, 2016, 61, 4164-4171.	1.0	3
66	Improving Students' Understanding of the Connections between the Concepts of Real-Gas Mixtures, Gas Ideal-Solutions, and Perfect-Gas Mixtures. Journal of Chemical Education, 2016, 93, 2040-2045.	1.1	6
67	VLE properties of CO2 – Based binary systems containing N2, O2 and Ar: Experimental measurements and modelling results with advanced cubic equations of state. Fluid Phase Equilibria, 2016, 428, 18-31.	1.4	47
68	Integrating support vector regression with genetic algorithm for CO2-oil minimum miscibility pressure (MMP) in pure and impure CO2 streams. Fuel, 2016, 182, 550-557.	3.4	62
69	Design of Hybrid Fuels Using a Modeling Study of the Miscibility of Ethanol–Biodiesel–Hydrocarbon Systems. International Journal of Thermophysics, 2016, 37, 1.	1.0	1
70	A five-parameter empirical model for correlating the solubility of solid compounds in supercritical carbon dioxide. Fluid Phase Equilibria, 2016, 411, 74-80.	1.4	66
71	Note on the properties altered by application of a Péneloux–type volume translation to an equation of state. Fluid Phase Equilibria, 2016, 419, 88-95.	1.4	101
72	Analysis and prediction of the alpha-function parameters used in cubic equations of state. Chemical Engineering Science, 2015, 126, 584-603.	1.9	30

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73	Predicting Binary-Interaction Parameters of Cubic Equations of State for Petroleum Fluids Containing Pseudo-components. Industrial & Engineering Chemistry Research, 2015, 54, 2816-2824.	1.8	38
74	Extension of the E-PPR78 equation of state to predict fluid phase equilibria of natural gases containing carbon monoxide, helium-4 and argon. Journal of Petroleum Science and Engineering, 2015, 133, 744-770.	2.1	29
75	Addition of the Sulfur Dioxide Group (SO ₂), the Oxygen Group (O ₂), and the Nitric Oxide Group (NO) to the <i>E</i> -PPR78 Model. Industrial & Engineering Chemistry Research, 2015, 54, 9494-9504.	1.8	23
76	Simulations of the Impact of Co-injected Gases on CO2 Storage, the SIGARRR Project: First Results on Water-gas Interactions Modeling. Energy Procedia, 2014, 63, 3160-3171.	1.8	10
77	Experimental measurements and correlation of vapor–liquid equilibrium and critical data for the CO 2 Å+ÂR1234yf and CO 2 Â+ÂR1234ze(E) binary mixtures. International Journal of Refrigeration, 2014, 47, 141-152.	1.8	72
78	Solubility of carbon dioxide, nitrous oxide and methane in ionic liquids at pressures close to atmospheric. Fluid Phase Equilibria, 2014, 372, 26-33.	1.4	45
79	General reflection on critical negative azeotropy and upgrade of the Bancroft's rule with application to the acetone+chloroform binary system. Journal of Supercritical Fluids, 2014, 94, 17-29.	1.6	14
80	Editor's preface for the special issue "Romanian International Conference on Chemistry and Chemical Engineering― Open Chemistry, 2014, 12, 747-748.	1.0	0
81	Development of a Predictive Equation of State for CO ₂ + Ethyl Ester Mixtures Based on Critical Points Measurements. Journal of Chemical & Engineering Data, 2014, 59, 3205-3219.	1.0	28
82	Experimental Measurement and Modeling of Phase Diagrams of Binary Systems Encountered in the Gasoline Desulfurization Process Using Ionic Liquids. Journal of Chemical & Engineering Data, 2014, 59, 603-612.	1.0	26
83	Comments on "Computational procedure for thermodynamic minimum miscibility pressure of reservoir oil― Fuel, 2013, 107, 882-883.	3.4	1
84	Novel Methodology for Analysis and Evaluation of SAFT-Type Equations of State. Industrial & Engineering Chemistry Research, 2013, 52, 13875-13885.	1.8	51
85	Classification of global fluid-phase equilibrium behaviors in binary systems. Chemical Engineering Research and Design, 2013, 91, 1807-1839.	2.7	141
86	Solubility of CO2 in 1-butyl-3-methylimidazolium diethylene-glycolmonomethylethersulfate and trihexyl(tetradecyl)phosphonium dodecyl-benzenesulfonate. Fluid Phase Equilibria, 2013, 354, 191-198.	1.4	18
87	Predicting the Phase Equilibria, Critical Phenomena, and Mixing Enthalpies of Binary Aqueous Systems Containing Alkanes, Cycloalkanes, Aromatics, Alkenes, and Gases (N ₂ , CO ₂ ,) Tj ETQq1	1 0,78431 1.8	l4 _g gBT /Ove
88	Enthalpy and Heat Capacity Changes on Mixing: Fundamental Aspects and Prediction by Means of the PPR78 Cubic Equation of State. Energy & amp; Fuels, 2013, 27, 7150-7178.	2.5	57
89	A simple and unified algorithm to solve fluid phase equilibria using either the gamma–phi or the phi–phi approach for binary and ternary mixtures. Computers and Chemical Engineering, 2013, 50, 139-151.	2.0	22
90	Reliability of the correlation allowing the kij to switch from an alpha function to another one in hydrogen-containing systems. Fluid Phase Equilibria, 2013, 338, 23-29.	1.4	19

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91	Role of Impurities on CO2 Injection: Experimental and Numerical Simulations of Thermodynamic Properties of Water-salt-gas Mixtures (CO2 + Co-injected Gases) Under Geological Storage Conditions. Energy Procedia, 2013, 37, 3638-3645.	1.8	21
92	Prediction of the phase behavior of alkene-containing binary systems with the PPR78 model. Fluid Phase Equilibria, 2013, 354, 212-235.	1.4	43
93	Quest for an efficient binary working mixture for an absorption-demixing heat transformer. Energy, 2013, 55, 594-609.	4.5	9
94	Validation of a New Apparatus Using the Dynamic Method for Determining the Critical Properties of Binary Gas/Gas Mixtures. Journal of Chemical & Engineering Data, 2013, 58, 671-676.	1.0	33
95	Phase equilibria in hydrogen-containing binary systems modeled with the Peng–Robinson equation of state and temperature-dependent binary interaction parameters calculated through a group-contribution method. Journal of Supercritical Fluids, 2013, 75, 58-71.	1.6	73
96	Modeling phase diagrams of systems containing ionic liquids used in different applications. MATEC Web of Conferences, 2013, 3, 01014.	0.1	0
97	The thermodynamics of alcohols-hydrocarbons mixtures. MATEC Web of Conferences, 2013, 3, 01018.	0.1	Ο
98	Experimental determination of the critical locus of binary systems containing CO2and an ethyl ester. MATEC Web of Conferences, 2013, 3, 01020.	0.1	0
99	Ethanol and Distillate Blends: A Thermodynamic Approach to Miscibility Issues: Part 3 — Generalization to Other Alcohols (Methanol, Isopropanol and 1-Butanol). , 2012, , .		Ο
100	Discussion around the paradigm of ideal mixtures with emphasis on the definition of the property changes on mixing. Chemical Engineering Science, 2012, 82, 319-333.	1.9	27
101	Addition of the sulfhydryl group (SH) to the PPR78 model: Estimation of missing group-interaction parameters for systems containing mercaptans and carbon dioxide or nitrogen or methane, from newly published data. Fluid Phase Equilibria, 2012, 334, 197-203.	1.4	30
102	Fluid Phase Equilibria Correlation for Carbon Dioxide +1-Heptanol System with Cubic Equations of State. Industrial & Engineering Chemistry Research, 2012, 51, 11284-11293.	1.8	16
103	Testing the ability of various equations of state to reproduce high-pressure isotherm crossings in the (α, P) plane. Fluid Phase Equilibria, 2012, 327, 45-57.	1.4	8
104	Modeling the Solubility of Carbon Dioxide in Imidazolium-Based Ionic Liquids with the PC-SAFT Equation of State. Journal of Physical Chemistry B, 2012, 116, 14375-14388.	1.2	112
105	Thermodynamic Models for the Prediction of Petroleum-Fluid Phase Behaviour. , 2012, , .		4
106	Are safe results obtained when SAFT equations are applied to ordinary chemicals? Part 2: Study of solid–liquid equilibria in binary systems. Fluid Phase Equilibria, 2012, 318, 61-76.	1.4	39
107	Validation of a new apparatus using the dynamic method for determining the critical properties of binary mixtures containing CO2 and a n-alkane. Fluid Phase Equilibria, 2012, 325, 66-70.	1.4	19
108	Comments on "PVTxy properties of CO2 mixtures relevant for CO2 capture, transport and storage: Review of available experimental data and theoretical models― Applied Energy, 2012, 93, 750-752.	5.1	1

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109	An improved crude oil atmospheric distillation process for energy integration: Part I: Energy and exergy analyses of the process when a flash is installed in the preheating train. Applied Thermal Engineering, 2012, 32, 125-131.	3.0	32
110	An improved crude oil atmospheric distillation process for energy integration: Part II: New approach for energy saving by use of residual heat. Applied Thermal Engineering, 2012, 40, 132-144.	3.0	16
111	Validation of a new apparatus using the dynamic and static methods for determining the critical properties of pure components and mixtures. Journal of Supercritical Fluids, 2012, 68, 25-30.	1.6	17
112	Deep Fuels Desulfurization and Denitrogenation Using 1-Butyl-3-methylimidazolium Trifluoromethanesulfonate. Energy & Fuels, 2011, 25, 1559-1565.	2.5	82
113	Prediction of Partition Coefficients of Organic Compounds in Ionic Liquids Using a Temperature-Dependent Linear Solvation Energy Relationship with Parameters Calculated through a Group Contribution Method. Journal of Chemical & Engineering Data, 2011, 56, 3598-3606.	1.0	32
114	Extraction of Thiophene or Pyridine from n-Heptane Using Ionic Liquids. Gasoline and Diesel Desulfurization. Industrial & Engineering Chemistry Research, 2011, 50, 2296-2306.	1.8	198
115	Extraction of <i>n</i> -Alcohols from <i>n</i> -Heptane Using Ionic Liquids Journal of Chemical & Engineering Data, 2011, 56, 3873-3880.	1.0	38
116	Péneloux's mixing rules: 25 years ago and now. Fluid Phase Equilibria, 2011, 308, 164-167.	1.4	10
117	Activity Coefficients at Infinite Dilution of Organic Compounds in Four New Imidazolium-Based Ionic Liquids. Journal of Chemical & Engineering Data, 2011, 56, 3106-3114.	1.0	81
118	Ethanol-Hydrocarbon Blend Vapor Prediction. Journal of Engineering for Gas Turbines and Power, 2010, 132, .	0.5	5
119	Ethanol and Distillate Blends: A Thermodynamic Approach to Miscibility Issues. , 2010, , .		0
120	Partition Coefficients of Organic Compounds in New Imidazolium and Tetralkylammonium Based Ionic Liquids Using Inverse Gas Chromatography. Journal of Chemical & Engineering Data, 2010, 55, 234-242.	1.0	148
121	Relationship between the binary interaction parameters (kij) of the Peng–Robinson and those of the Soave–Redlich–Kwong equations of state: Application to the definition of the PR2SRK model. Fluid Phase Equilibria, 2010, 295, 26-37.	1.4	138
122	Are safe results obtained when the PC-SAFT equation of state is applied to ordinary pure chemicals?. Fluid Phase Equilibria, 2010, 295, 76-92.	1.4	126
123	Predicting the phase equilibria of synthetic petroleum fluids with the PPR78 approach. AICHE Journal, 2010, 56, 3225-3235.	1.8	160
124	Estimation of the environmental impact of a petrochemical process using coupled LCA and exergy analysis. Resources, Conservation and Recycling, 2010, 54, 291-298.	5.3	44
125	(Vapor+liquid) equilibria of binary mixtures containing light alcohols and ionic liquids. Journal of Chemical Thermodynamics, 2010, 42, 177-181.	1.0	26
126	Comments on "Application of predictive equations of state in calculating natural gas phase envelopes and critical points― Journal of Natural Gas Science and Engineering, 2010, 2, 150-151.	2.1	8

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127	Life Cycle Assessment Applied to Naphtha Catalytic Reforming. Oil and Gas Science and Technology, 2010, 65, 793-805.	1.4	17
128	Study of Ether-, Alcohol-, or Cyano-Functionalized Ionic Liquids Using Inverse Gas Chromatography. Journal of Chemical & Engineering Data, 2010, 55, 2434-2443.	1.0	88
129	Prediction of Partition Coefficients of Organic Compounds in Ionic Liquids: Use of a Linear Solvation Energy Relationship with Parameters Calculated through a Group Contribution Method. Industrial & Engineering Chemistry Research, 2010, 49, 3883-3892.	1.8	67
130	Reducing of Nitrous Oxide Emissions Using Ionic Liquids. Journal of Physical Chemistry B, 2010, 114, 8199-8206.	1.2	47
131	Extraction of Benzene or Thiophene from <i>n</i> -Heptane Using Ionic Liquids. NMR and Thermodynamic Study. Journal of Physical Chemistry B, 2010, 114, 4600-4608.	1.2	141
132	High Carbon Dioxide Solubilities in Imidazolium-Based Ionic Liquids and in Poly(ethylene glycol) Dimethyl Ether. Journal of Physical Chemistry B, 2010, 114, 12908-12913.	1.2	122
133	Partition coefficients of organic compounds in new imidazolium based ionic liquids using inverse gas chromatography. Journal of Chromatography A, 2009, 1216, 4775-4786.	1.8	75
134	Can cubic equations of state be recast in the virial form?. Fluid Phase Equilibria, 2009, 282, 38-50.	1.4	14
135	Activity Coefficients at Infinite Dilution of Organic Compounds in 1-Butyl-3-methylimidazolium Tetrafluoroborate Using Inverse Gas Chromatography. Journal of Chemical & Engineering Data, 2009, 54, 90-101.	1.0	86
136	Ethanol-Hydrocarbon Blend Vapor Prediction. , 2009, , .		1
137	High-pressure phase behaviour of the binary system {CO2+cis-decalin} from (292.75 to 373.75)K. Journal of Chemical Thermodynamics, 2008, 40, 1358-1363.	1.0	15
138	Addition of the sulfhydryl group (–SH) to the PPR78 model (predictive 1978, Peng–Robinson EOS with) Tj ET Thermodynamics, 2008, 40, 1331-1341.	Qq0 0 0 r 1.0	gBT /Overloo 59
139	Phase equilibria measurements of CO2+methyl cyclopentane and CO2+isopropyl cyclohexane binary mixtures at elevated pressures. Journal of Supercritical Fluids, 2008, 44, 155-163.	1.6	38
140	Predicting the phase equilibria of CO2+hydrocarbon systems with the PPR78 model (PR EOS and kij) Tj ETQq0 0 (O rgBT /Ov	erlock 10 Tf
141	Addition of the Hydrogen Sulfide Group to the PPR78 Model (Predictive 1978, Peng–Robinson Equation) Tj ETC	Qq1 1 0.78 1.8	34314 rgBT 77
142	Activity Coefficients at Infinite Dilution of Organic Compounds in 1-(Meth)acryloyloxyalkyl-3-methylimidazolium Bromide Using Inverse Gas Chromatography. Journal of Physical Chemistry B, 2008, 112, 3773-3785.	1.2	79
143	Use of the PPR78 Model To Predict New Equilibrium Data of Binary Systems Involving Hydrocarbons and Nitrogen. Comparison with Other GCEOS. Industrial & Engineering Chemistry Research, 2008, 47, 7483-7489.	1.8	66
144	Comments on "Solubility of CO2, N2, and CO2 + N2 Gas Mixtures in Isooctane―(Zhang, J. S.; Lee, S.; Lee, J.) 2001-2001.	Tj ETQq0 1.0	0 0 rgBT /Ov 2

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145	Addition of the Nitrogen Group to the PPR78 Model (Predictive 1978, Peng Robinson EOS with) Tj ETQq1 1 0.784	314 rgBT 1.8	/Overlock 10 82
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