

Jean Nol Jaubert

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182
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46
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188
ext. papers

6,706
ext. citations

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L-index

#	Paper	IF	Citations
182	VLE predictions with the Peng-Robinson equation of state and temperature dependent kij calculated through a group contribution method. <i>Fluid Phase Equilibria</i> , 2004 , 224, 285-304	2.5	289
181	Extraction of Thiophene or Pyridine from n-Heptane Using Ionic Liquids. Gasoline and Diesel Desulfurization. <i>Industrial & Engineering Chemistry Research</i> , 2011 , 50, 2296-2306	3.9	177
180	Predicting the phase equilibria of CO ₂ + hydrocarbon systems with the PPR78 model (PR EOS and kij calculated through a group contribution method). <i>Journal of Supercritical Fluids</i> , 2008 , 45, 1-26	4.2	173
179	Predicting the phase equilibria of synthetic petroleum fluids with the PPR78 approach. <i>AIChE Journal</i> , 2010 , 56, 3225-3235	3.6	144
178	Partition Coefficients of Organic Compounds in New Imidazolium and Tetralkylammonium Based Ionic Liquids Using Inverse Gas Chromatography. <i>Journal of Chemical & Engineering Data</i> , 2010 , 55, 234-242	2.8	136
177	Accurate measurements of thermodynamic properties of solutes in ionic liquids using inverse gas chromatography. <i>Journal of Chromatography A</i> , 2006 , 1102, 256-67	4.5	124
176	Relationship between the binary interaction parameters (kij) of the Peng-Robinson and those of the Soave-Redlich-Kwong equations of state: Application to the definition of the PR2SRK model. <i>Fluid Phase Equilibria</i> , 2010 , 295, 26-37	2.5	121
175	Extraction of benzene or thiophene from n-heptane using ionic liquids. NMR and thermodynamic study. <i>Journal of Physical Chemistry B</i> , 2010 , 114, 4600-8	3.4	120
174	Classification of global fluid-phase equilibrium behaviors in binary systems. <i>Chemical Engineering Research and Design</i> , 2013 , 91, 1807-1839	5.5	111
173	Extension of the PPR78 model (predictive 1978, Peng-Robinson EOS with temperature dependent kij calculated through a group contribution method) to systems containing aromatic compounds. <i>Fluid Phase Equilibria</i> , 2005 , 237, 193-211	2.5	110
172	Are safe results obtained when the PC-SAFT equation of state is applied to ordinary pure chemicals?. <i>Fluid Phase Equilibria</i> , 2010 , 295, 76-92	2.5	109
171	High carbon dioxide solubilities in imidazolium-based ionic liquids and in poly(ethylene glycol) dimethyl ether. <i>Journal of Physical Chemistry B</i> , 2010 , 114, 12908-13	3.4	107
170	Application of Inverse Gas Chromatography and Regular Solution Theory for Characterization of Ionic Liquids. <i>Industrial & Engineering Chemistry Research</i> , 2005 , 44, 4120-4127	3.9	106
169	A consistency test for Φ -functions of cubic equations of state. <i>Fluid Phase Equilibria</i> , 2016 , 427, 513-538	2.5	98
168	A crude oil data bank containing more than 5000 PVT and gas injection data. <i>Journal of Petroleum Science and Engineering</i> , 2002 , 34, 65-107	4.4	94
167	Modeling the solubility of carbon dioxide in imidazolium-based ionic liquids with the PC-SAFT equation of state. <i>Journal of Physical Chemistry B</i> , 2012 , 116, 14375-88	3.4	92
166	Measurement of activity coefficients at infinite dilution in 1-hexadecyl-3-methylimidazolium tetrafluoroborate ionic liquid. <i>Journal of Chemical Thermodynamics</i> , 2007 , 39, 1144-1150	2.9	88

165	Development of the translated-consistent tc-PR and tc-RK cubic equations of state for a safe and accurate prediction of volumetric, energetic and saturation properties of pure compounds in the sub- and super-critical domains. <i>Fluid Phase Equilibria</i> , 2016 , 429, 301-312	2.5	85
164	A Very Simple Multiple Mixing Cell Calculation To Compute the Minimum Miscibility Pressure Whatever the Displacement Mechanism. <i>Industrial & Engineering Chemistry Research</i> , 1998 , 37, 4854-4859	3.0	85
163	Extension of the PPR78 model (Predictive 1978, Peng-Robinson EOS with temperature dependent kij calculated through a group contribution method) to systems containing naphtenic compounds. <i>Fluid Phase Equilibria</i> , 2006 , 243, 9-28	2.5	84
162	Note on the properties altered by application of a PélouxB-type volume translation to an equation of state. <i>Fluid Phase Equilibria</i> , 2016 , 419, 88-95	2.5	79
161	Deep Fuels Desulfurization and Denitrogenation Using 1-Butyl-3-methylimidazolium Trifluoromethanesulfonate. <i>Energy & Fuels</i> , 2011 , 25, 1559-1565	4.1	77
160	Predicting the Phase Equilibria, Critical Phenomena, and Mixing Enthalpies of Binary Aqueous Systems Containing Alkanes, Cycloalkanes, Aromatics, Alkenes, and Gases (N ₂ , CO ₂ , H ₂ S, H ₂) with the PPR78 Equation of State. <i>Industrial & Engineering Chemistry Research</i> , 2013 , 52, 16457-16490	3.9	76
159	Activity Coefficients at Infinite Dilution of Organic Compounds in 1-Butyl-3-methylimidazolium Tetrafluoroborate Using Inverse Gas Chromatography. <i>Journal of Chemical & Engineering Data</i> , 2009 , 54, 90-101	2.8	76
158	Activity coefficients at infinite dilution of organic compounds in 1-(meth)acryloyloxyalkyl-3-methylimidazolium bromide using inverse gas chromatography. <i>Journal of Physical Chemistry B</i> , 2008 , 112, 3773-85	3.4	76
157	Study of Ether-, Alcohol-, or Cyano-Functionalized Ionic Liquids Using Inverse Gas Chromatography. <i>Journal of Chemical & Engineering Data</i> , 2010 , 55, 2434-2443	2.8	75
156	Is It Still Necessary to Measure the Minimum Miscibility Pressure?. <i>Industrial & Engineering Chemistry Research</i> , 2002 , 41, 303-310	3.9	74
155	Partition coefficients of organic compounds in new imidazolium based ionic liquids using inverse gas chromatography. <i>Journal of Chromatography A</i> , 2009 , 1216, 4775-86	4.5	73
154	Enantioseparation through Supercritical Fluid Simulated Moving Bed (SF-SMB) Chromatography. <i>Industrial & Engineering Chemistry Research</i> , 2001 , 40, 4603-4609	3.9	73
153	Activity Coefficients at Infinite Dilution of Organic Compounds in Four New Imidazolium-Based Ionic Liquids. <i>Journal of Chemical & Engineering Data</i> , 2011 , 56, 3106-3114	2.8	72
152	Addition of the Nitrogen Group to the PPR78 Model (Predictive 1978, Peng Robinson EOS with Temperature-Dependent kij Calculated through a Group Contribution Method). <i>Industrial & Engineering Chemistry Research</i> , 2008 , 47, 2033-2048	3.9	71
151	Solubility of CO ₂ in branched alkanes in order to extend the PPR78 model (predictive 1978, Peng-Robinson EOS with temperature-dependent kij calculated through a group contribution method) to such systems. <i>Fluid Phase Equilibria</i> , 2005 , 238, 157-168	2.5	70
150	Addition of the Hydrogen Sulfide Group to the PPR78 Model (Predictive 1978, Peng-Robinson Equation of State with Temperature Dependent kij Calculated through a Group Contribution Method). <i>Industrial & Engineering Chemistry Research</i> , 2008 , 47, 10041-10052	3.9	66
149	On the imperative need to use a consistent β -function for the prediction of pure-compound supercritical properties with a cubic equation of state. <i>Fluid Phase Equilibria</i> , 2017 , 445, 45-53	2.5	59
148	Prediction of Partition Coefficients of Organic Compounds in Ionic Liquids: Use of a Linear Solvation Energy Relationship with Parameters Calculated through a Group Contribution Method. <i>Industrial & Engineering Chemistry Research</i> , 2010 , 49, 3883-3892	3.9	59

147	Use of the PPR78 Model To Predict New Equilibrium Data of Binary Systems Involving Hydrocarbons and Nitrogen. Comparison with Other GCEOS. <i>Industrial & Engineering Chemistry Research</i> , 2008 , 47, 7483-7489	3.9	59
146	Thermodynamic Properties of Mixtures Containing Ionic Liquids: Activity Coefficients at Infinite Dilution of Organic Compounds in 1-Propyl Boronic Acid-3-Alkylimidazolium Bromide and 1-Propenyl-3-alkylimidazolium Bromide Using Inverse Gas Chromatography. <i>Journal of Chemical Engineering Data</i> , 2001 , 51, 1271-1278	2.8	57
145	Phase equilibria in hydrogen-containing binary systems modeled with the Peng-Robinson equation of state and temperature-dependent binary interaction parameters calculated through a group-contribution method. <i>Journal of Supercritical Fluids</i> , 2013 , 75, 58-71	4.2	56
144	Experimental and Modeled Results Describing the Adsorption of Toluene onto Activated Carbon. <i>Journal of Chemical & Engineering Data</i> , 2000 , 45, 650-653	2.8	56
143	Addition of the sulfhydryl group (SH) to the PPR78 model (predictive 1978, Peng-Robinson EOS with temperature dependent kij calculated through a group contribution method). <i>Journal of Chemical Thermodynamics</i> , 2008 , 40, 1331-1341	2.9	55
142	Incorporation of a volume translation in an equation of state for fluid mixtures: which combining rule? which effect on properties of mixing?. <i>Fluid Phase Equilibria</i> , 2016 , 427, 414-420	2.5	50
141	Phase equilibria measurements and modeling of EPA and DHA ethyl esters in supercritical carbon dioxide. <i>Journal of Supercritical Fluids</i> , 2001 , 20, 145-155	4.2	50
140	The Group Contribution Concept: A Useful Tool To Correlate Binary Systems and To Predict the Phase Behavior of Multicomponent Systems Involving Supercritical CO ₂ and Fatty Acids. <i>Industrial & Engineering Chemistry Research</i> , 1999 , 38, 5011-5018	3.9	50
139	From the Correlation of Binary Systems Involving Supercritical CO ₂ and Fatty Acid Esters to the Prediction of (CO ₂ -rich Oils) Phase Behavior. <i>Industrial & Engineering Chemistry Research</i> , 1999 , 38, 3162-3171	3.9	49
138	Thermodynamic modeling for petroleum fluids I. Equation of state and group contribution for the estimation of thermodynamic parameters of heavy hydrocarbons. <i>Fluid Phase Equilibria</i> , 1997 , 139, 155-170	2.5	48
137	Integrating support vector regression with genetic algorithm for CO ₂ -oil minimum miscibility pressure (MMP) in pure and impure CO ₂ streams. <i>Fuel</i> , 2016 , 182, 550-557	7.1	47
136	A five-parameter empirical model for correlating the solubility of solid compounds in supercritical carbon dioxide. <i>Fluid Phase Equilibria</i> , 2016 , 411, 74-80	2.5	46
135	Experimental measurements and correlation of vapor-liquid equilibrium and critical data for the CO ₂ + R1234yf and CO ₂ + R1234ze(E) binary mixtures. <i>International Journal of Refrigeration</i> , 2014 , 47, 141-152	3.8	46
134	Characterization of heavy oils. <i>Industrial & Engineering Chemistry Research</i> , 1993 , 32, 1196-1203	3.9	46
133	Enthalpy and Heat Capacity Changes on Mixing: Fundamental Aspects and Prediction by Means of the PPR78 Cubic Equation of State. <i>Energy & Fuels</i> , 2013 , 27, 7150-7178	4.1	45
132	Novel Methodology for Analysis and Evaluation of SAFT-Type Equations of State. <i>Industrial & Engineering Chemistry Research</i> , 2013 , 52, 13875-13885	3.9	43
131	Reducing of nitrous oxide emissions using ionic liquids. <i>Journal of Physical Chemistry B</i> , 2010 , 114, 8199-206	3.4	43
130	Enantiomeric enrichment of non-racemic mixtures of binaphthol with non-chiral packings. <i>Chirality</i> , 1996 , 8, 234-243	2.1	40

129	Updated versions of the generalized Soave α -function suitable for the Redlich-Kwong and Peng-Robinson equations of state. <i>Fluid Phase Equilibria</i> , 2019 , 485, 264-269	2.5	40
128	Estimation of the environmental impact of a petrochemical process using coupled LCA and exergy analysis. <i>Resources, Conservation and Recycling</i> , 2010 , 54, 291-298	11.9	36
127	E-PPR78: A proper cubic EoS for modelling fluids involved in the design and operation of carbon dioxide capture and storage (CCS) processes. <i>International Journal of Greenhouse Gas Control</i> , 2017 , 56, 126-154	4.2	35
126	Prediction of the phase behavior of alkene-containing binary systems with the PPR78 model. <i>Fluid Phase Equilibria</i> , 2013 , 354, 212-235	2.5	35
125	Solubility of carbon dioxide, nitrous oxide and methane in ionic liquids at pressures close to atmospheric. <i>Fluid Phase Equilibria</i> , 2014 , 372, 26-33	2.5	35
124	Are safe results obtained when SAFT equations are applied to ordinary chemicals? Part 2: Study of solid-liquid equilibria in binary systems. <i>Fluid Phase Equilibria</i> , 2012 , 318, 61-76	2.5	35
123	Extraction of n-Alcohols from n-Heptane Using Ionic Liquids.. <i>Journal of Chemical & Engineering Data</i> , 2011 , 56, 3873-3880	2.8	35
122	Phase equilibria measurements of CO ₂ +methyl cyclopentane and CO ₂ +isopropyl cyclohexane binary mixtures at elevated pressures. <i>Journal of Supercritical Fluids</i> , 2008 , 44, 155-163	4.2	35
121	VLE properties of CO ₂ based binary systems containing N ₂ , O ₂ and Ar: Experimental measurements and modelling results with advanced cubic equations of state. <i>Fluid Phase Equilibria</i> , 2016 , 428, 18-31	2.5	33
120	Predicting Binary-Interaction Parameters of Cubic Equations of State for Petroleum Fluids Containing Pseudo-components. <i>Industrial & Engineering Chemistry Research</i> , 2015 , 54, 2816-2824	3.9	32
119	Properly Defining the Classical Vaporizing and Condensing Mechanisms When a Gas Is Injected into a Crude Oil. <i>Industrial & Engineering Chemistry Research</i> , 1998 , 37, 4860-4869	3.9	31
118	A new algorithm for enhanced oil recovery calculations. <i>Fluid Phase Equilibria</i> , 1996 , 117, 265-272	2.5	30
117	Prediction of Partition Coefficients of Organic Compounds in Ionic Liquids Using a Temperature-Dependent Linear Solvation Energy Relationship with Parameters Calculated through a Group Contribution Method. <i>Journal of Chemical & Engineering Data</i> , 2011 , 56, 3598-3606	2.8	29
116	Adsorption isotherms of m-xylene on activated carbon: measurements and correlation with different models. <i>Journal of Chemical Thermodynamics</i> , 2000 , 32, 401-411	2.9	29
115	Analysis of the Combinations of Property Data That Are Suitable for a Safe Estimation of Consistent Two-Function Parameters: Updated Parameter Values for the Translated-Consistent tc-PR and tc-RK Cubic Equations of State. <i>Journal of Chemical & Engineering Data</i> , 2018 , 63, 3980-3988	2.8	29
114	Determining Volatile Organic Compounds' Adsorption Isotherms on Dealuminated Y Zeolite and Correlation with Different Models. <i>Journal of Chemical & Engineering Data</i> , 2002 , 47, 1553-1557	2.8	28
113	Addition of the sulfhydryl group (SH) to the PPR78 model: Estimation of missing group-interaction parameters for systems containing mercaptans and carbon dioxide or nitrogen or methane, from newly published data. <i>Fluid Phase Equilibria</i> , 2012 , 334, 197-203	2.5	27
112	ADSORPTION AND DESORPTION OF M-XYLENE FROM SUPERCRITICAL CARBON DIOXIDE ON ACTIVATED CARBON. <i>Separation Science and Technology</i> , 2001 , 36, 2197-2211	2.5	27

111	An improved crude oil atmospheric distillation process for energy integration: Part I: Energy and exergy analyses of the process when a flash is installed in the preheating train. <i>Applied Thermal Engineering</i> , 2012 , 32, 125-131	5.8	26
110	I-PC-SAFT: An Industrialized Version of the Volume-Translated PC-SAFT Equation of State for Pure Components, Resulting from Experience Acquired All through the Years on the Parameterization of SAFT-Type and Cubic Models. <i>Industrial & Engineering Chemistry Research</i> , 2019 , 58, 20815-20827	3.9	25
109	Characterization of Heavy Oils. 3. Prediction of Gas Injection Behavior: Swelling Test, Multicontact Test, Multiple-Contact Minimum Miscibility Pressure, and Multiple-Contact Minimum Miscibility Enrichment. <i>Industrial & Engineering Chemistry Research</i> , 1995 , 34, 4016-4032	3.9	25
108	Discussion around the paradigm of ideal mixtures with emphasis on the definition of the property changes on mixing. <i>Chemical Engineering Science</i> , 2012 , 82, 319-333	4.4	24
107	Taking Another Look at the van der Waals Equation of State Almost 150 Years Later. <i>Journal of Chemical & Engineering Data</i> , 2019 , 64, 4619-4637	2.8	23
106	Development of a Predictive Equation of State for CO ₂ + Ethyl Ester Mixtures Based on Critical Points Measurements. <i>Journal of Chemical & Engineering Data</i> , 2014 , 59, 3205-3219	2.8	23
105	Phase equilibrium of CCS mixtures: Equation of state modeling and Monte Carlo simulation. <i>Journal of Supercritical Fluids</i> , 2017 , 119, 169-202	4.2	23
104	Bubble and Dew Points of Carbon Dioxide + a Five-Component Synthetic Mixture: Experimental Data and Modeling with the PPR78 Model. <i>Journal of Chemical & Engineering Data</i> , 2007 , 52, 1851-1855	2.8	23
103	Experimental Measurement and Modeling of Phase Diagrams of Binary Systems Encountered in the Gasoline Desulfurization Process Using Ionic Liquids. <i>Journal of Chemical & Engineering Data</i> , 2014 , 59, 603-612	2.8	22
102	Fluid-phase-equilibrium prediction of fluorocompound-containing binary systems with the predictive E-PPR78 model. <i>International Journal of Refrigeration</i> , 2017 , 73, 65-90	3.8	22
101	Analysis and prediction of the alpha-function parameters used in cubic equations of state. <i>Chemical Engineering Science</i> , 2015 , 126, 584-603	4.4	22
100	Pressure, Volume, and Temperature Calculations on an Indonesian Crude Oil Using Detailed NMR Analysis or a Predictive Method To Assess the Properties of the Heavy Fractions. <i>Industrial & Engineering Chemistry Research</i> , 1995 , 34, 640-655	3.9	22
99	Validation of a New Apparatus Using the Dynamic Method for Determining the Critical Properties of Binary Gas/Gas Mixtures. <i>Journal of Chemical & Engineering Data</i> , 2013 , 58, 671-676	2.8	21
98	Estimation of Solvation Quantities from Experimental Thermodynamic Data: Development of the Comprehensive CompSol Databank for Pure and Mixed Solutes. <i>Journal of Physical and Chemical Reference Data</i> , 2017 , 46, 033102	4.3	20
97	Extension of the E-PPR78 equation of state to predict fluid phase equilibria of natural gases containing carbon monoxide, helium-4 and argon. <i>Journal of Petroleum Science and Engineering</i> , 2015 , 133, 744-770	4.4	20
96	(Vapor + liquid) equilibria of binary mixtures containing light alcohols and ionic liquids. <i>Journal of Chemical Thermodynamics</i> , 2010 , 42, 177-181	2.9	20
95	Thermodynamic modeling for petroleum fluid III. Reservoir fluid saturation pressures. A complete PVT property estimation. Application to swelling test. <i>Fluid Phase Equilibria</i> , 1997 , 141, 87-104	2.5	19
94	A thermal and thermodynamic code for the computation of Boil-Off Gas [Industrial applications of LNG carrier. <i>Cryogenics</i> , 2019 , 99, 105-113	1.8	19

93	A simple and unified algorithm to solve fluid phase equilibria using either the gamma ϕ or the phi ϕ approach for binary and ternary mixtures. <i>Computers and Chemical Engineering</i> , 2013 , 50, 139-151	4	18
92	Modeling the Thermodynamics of Fluids Treated by CO ₂ Capture Processes with Peng-Robinson + Residual Helmholtz Energy-Based Mixing Rules. <i>Industrial & Engineering Chemistry Research</i> , 2017 , 56, 2259-2276	3.9	17
91	Addition of the Sulfur Dioxide Group (SO ₂), the Oxygen Group (O ₂), and the Nitric Oxide Group (NO) to the E-PPR78 Model. <i>Industrial & Engineering Chemistry Research</i> , 2015 , 54, 9494-9504	3.9	17
90	Thermodynamic modeling for petroleum fluids II. Prediction of PVT properties of oils and gases by fitting one or two parameters to the saturation pressures of reservoir fluids. <i>Fluid Phase Equilibria</i> , 1997 , 139, 171-203	2.5	17
89	Benchmark Database Containing Binary-System-High-Quality-Certified Data for Cross-Comparing Thermodynamic Models and Assessing Their Accuracy. <i>Industrial & Engineering Chemistry Research</i> , 2020 , 59, 14981-15027	3.9	17
88	From ethyl biodiesel to biolubricants: Options for an Indian mustard integrated biorefinery toward a green and circular economy. <i>Industrial Crops and Products</i> , 2019 , 137, 597-614	5.9	16
87	Prediction of Thermodynamic Properties of Alkyne-Containing Mixtures with the E-PPR78 Model. <i>Industrial & Engineering Chemistry Research</i> , 2017 , 56, 8143-8157	3.9	16
86	A new approach in correlating the oil thermodynamic properties. <i>Journal of Petroleum Science and Engineering</i> , 2001 , 30, 43-65	4.4	16
85	Validation of a new apparatus using the dynamic and static methods for determining the critical properties of pure components and mixtures. <i>Journal of Supercritical Fluids</i> , 2012 , 68, 25-30	4.2	15
84	Solubility of CO ₂ in 1-butyl-3-methylimidazolium diethylene-glycolmonomethylethersulfate and trihexyl(tetradecyl)phosphonium dodecyl-benzenesulfonate. <i>Fluid Phase Equilibria</i> , 2013 , 354, 191-198	2.5	15
83	Reliability of the correlation allowing the kij to switch from an alpha function to another one in hydrogen-containing systems. <i>Fluid Phase Equilibria</i> , 2013 , 338, 23-29	2.5	15
82	Validation of a new apparatus using the dynamic method for determining the critical properties of binary mixtures containing CO ₂ and a n-alkane. <i>Fluid Phase Equilibria</i> , 2012 , 325, 66-70	2.5	15
81	An improved crude oil atmospheric distillation process for energy integration: Part II: New approach for energy saving by use of residual heat. <i>Applied Thermal Engineering</i> , 2012 , 40, 132-144	5.8	15
80	Role of Impurities on CO ₂ Injection: Experimental and Numerical Simulations of Thermodynamic Properties of Water-salt-gas Mixtures (CO ₂ + Co-injected Gases) Under Geological Storage Conditions. <i>Energy Procedia</i> , 2013 , 37, 3638-3645	2.3	14
79	Fluid Phase Equilibria Correlation for Carbon Dioxide +1-Heptanol System with Cubic Equations of State. <i>Industrial & Engineering Chemistry Research</i> , 2012 , 51, 11284-11293	3.9	14
78	High-pressure phase behaviour of the binary system {CO ₂ + cis-decalin} from (292.75 to 373.75) K. <i>Journal of Chemical Thermodynamics</i> , 2008 , 40, 1358-1363	2.9	14
77	Good Reporting Practice for Thermophysical and Thermochemical Property Measurements (IUPAC Technical Report).. <i>Pure and Applied Chemistry</i> , 2021 , 93,	2.1	14
76	Selection of a Proper Equation of State for the Modeling of a Supercritical CO ₂ Brayton Cycle: Consequences on the Process Design. <i>Industrial & Engineering Chemistry Research</i> , 2017 , 56, 6841-6853	3.9	13

75	Life Cycle Assessment Applied to Naphtha Catalytic Reforming. <i>Oil and Gas Science and Technology</i> , 2010 , 65, 793-805	1.9	13
74	Characterization of Heavy Oils. 2. Definition of a Significant Characterizing Parameter To Ensure the Reliability of Predictive Methods for PVT Calculations. <i>Industrial & Engineering Chemistry Research</i> , 1995 , 34, 1873-1881	3.9	13
73	Can cubic equations of state be recast in the virial form?. <i>Fluid Phase Equilibria</i> , 2009 , 282, 38-50	2.5	12
72	Measurement and prediction of multi-property data of CO ₂ -N ₂ -O ₂ -CH ₄ mixtures with the Peng-Robinson + residual Helmholtz energy-based model. <i>Fluid Phase Equilibria</i> , 2017 , 437, 166-180	2.5	11
71	General reflection on critical negative azeotropy and upgrade of the Bancroft's rule with application to the acetone + chloroform binary system. <i>Journal of Supercritical Fluids</i> , 2014 , 94, 17-29	4.2	11
70	Possible Existence of a Negative (Positive) Homogeneous Azeotrope When the Binary Mixture Exhibits Positive (Negative) Deviations from Ideal Solution Behavior (That is, When g ^E is Positive (Negative)). <i>Industrial & Engineering Chemistry Research</i> , 2006 , 45, 8217-8222	3.9	10
69	Solubility of CO ₂ in some heavy alcohols and correlation of fluid phase equilibrium. <i>Fluid Phase Equilibria</i> , 2003 , 213, 153-162	2.5	10
68	4-Chloro-2-nitroaniline Solubility in Several Pure Solvents: Determination, Modeling, and Solvent Effect Analysis. <i>Journal of Chemical & Engineering Data</i> , 2020 , 65, 222-232	2.8	10
67	Search for the optimal expression of the volumetric dependence of the attractive contribution in cubic equations of state. <i>Fluid Phase Equilibria</i> , 2020 , 522, 112750	2.5	10
66	Simulations of the Impact of Co-injected Gases on CO ₂ Storage, the SIGARRR Project: First Results on Water-gas Interactions Modeling. <i>Energy Procedia</i> , 2014 , 63, 3160-3171	2.3	9
65	Use of a Predictive Cubic Equation of State To Model New Equilibrium Data of Binary Systems Involving Fatty Acid Esters and Supercritical Carbon Dioxide. <i>Industrial & Engineering Chemistry Research</i> , 2000 , 39, 2623-2626	3.9	9
64	Optimizing Thermodynamic Models: The Relevance of Molar Fraction Uncertainties. <i>Journal of Chemical & Engineering Data</i> , 2017 , 62, 825-832	2.8	8
63	Application of the Corresponding-State Law to the Parametrization of Statistical Associating Fluid Theory (SAFT)-Type Models: Generation and Use of Generalized Charts. <i>Industrial & Engineering Chemistry Research</i> , 2019 , 58, 9127-9139	3.9	8
62	Pfabeloux's mixing rules: 25 years ago and now. <i>Fluid Phase Equilibria</i> , 2011 , 308, 164-167	2.5	8
61	Comments on Application of predictive equations of state in calculating natural gas phase envelopes and critical points. <i>Journal of Natural Gas Science and Engineering</i> , 2010 , 2, 150-151	4.6	8
60	Sizing and operating units for the purification and compression of CO ₂ -based streams: The impact of thermodynamic model accuracy. <i>Journal of Supercritical Fluids</i> , 2018 , 140, 336-347	4.2	7
59	Quest for an efficient binary working mixture for an absorption-demixing heat transformer. <i>Energy</i> , 2013 , 55, 594-609	7.9	7
58	Testing the ability of various equations of state to reproduce high-pressure isotherm crossings in the (P, T) plane. <i>Fluid Phase Equilibria</i> , 2012 , 327, 45-57	2.5	7

57	Densities, Apparent Molar Volume, Expansivities, Hepler's Constant, and Isobaric Thermal Expansion Coefficients of the Binary Mixtures of Piperazine with Water, Methanol, and Acetone at T = 293.15 to 328.15 K. <i>International Journal of Chemical Engineering</i> , 2018 , 2018, 1-10	2.2	7
56	Phase equilibrium data and modeling of ethylic biodiesel, with application to a non-edible vegetable oil. <i>Fuel</i> , 2017 , 203, 633-641	7.1	6
55	The design of CO ₂ -based working fluids for high-temperature heat source power cycles. <i>Energy Procedia</i> , 2017 , 129, 947-954	2.3	6
54	VOCs isotherms on dry zeolite by static and dynamic methods: experiments and modelling. <i>Environmental Technology (United Kingdom)</i> , 2003 , 24, 1201-10	2.6	6
53	Solubility of Hexanol in pure carbon dioxide and in a mixed solvent formed by ethanol and carbon dioxide. <i>Fluid Phase Equilibria</i> , 2001 , 191, 59-69	2.5	6
52	Parameterization of SAFT Models: Analysis of Different Parameter Estimation Strategies and Application to the Development of a Comprehensive Database of PC-SAFT Molecular Parameters. <i>Journal of Chemical & Engineering Data</i> , 2020 , 65, 5920-5932	2.8	6
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